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Application of Flow Reactors within Drug Discovery

Elizabeth M. Doherty, Ph.D., Group Leader

Medicinal Chemistry Research Technologies Amgen, Inc. Thousand Oaks, California

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Drug Discovery Accelerating Technologies at Amgen

- The function of the Medicinal Chemistry Research Technologies (MCRT) group at Amgen is to evaluate and advance tools for accelerated drug discovery, including:
 - In silico target design tools
 - Parallel and high-throughput synthesis tools
 - High-throughput purification
 - High-throughput characterization
 - Reaction screening platforms

These tools must be:

- Effective
- Robust
- User-friendly (open access)



Flow Chemistry as an Accelerating Technology

Potential for:

- Accelerated reaction rates
- Accessing supercritical temperature/pressure
- Increased safety (reactives, gases, pyrophoric catalyst handling)
- Precise control of conditions (screening, optimization)
- Ease of use through automation

However:

- Translating batch to flow is not "intuitive"
- Few user-friendly commercial tools available directed toward Med Chem scale (25-50 mg for in vitro studies, up to 100 g for intermediates or in vivo studies)



ThalesNano[©] H-Cube[™]

Flow hydrogenation is advantageous due to relatively limited throughput, safety, and efficiency of batch processes.

Advertised features of H-Cube[™]:

- In situ H₂ production
- Adjustable parameters
 - Liquid flow rate
 - Temperature
 - "Full" H₂ flow mode (1 bar)
 - Controlled mode (metered H₂)
- User friendly interface
- Safe catalyst handling (CatCart[™])





Images courtesy of Thalesnano Technology



H-Cube™ with Autosampler

Gilson[©] liquid handler and ThalesNano[©] automation software:

- Permits walk-away use
- Experiments can be queued to facilitate screening



Image courtesy of Thalesnano Technology

See: Ladlow and Ley, Adv. Synth. Catal. 2007, 349, 535-538.

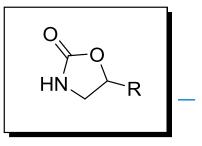


ThalesNano[©] H-Cube[™] at Amgen

Users have successfully performed:

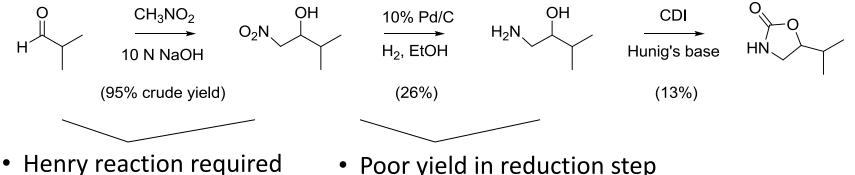
- Aromatic nitro reductions
- Aliphatic nitro reductions
- Heteroaromatic ring saturation
- ✓ CBZ-hydrogenolysis
- ✓ N-Debenzylation
- Olefin reductions
- ✓ Azide reduction
- Case studies
- ➤ H-Cube[™] characterization





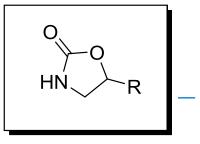
- Project team needed a series of 5-substituted oxazolidinones
- Limited commercial availability

Original unoptimized Med Chem route:



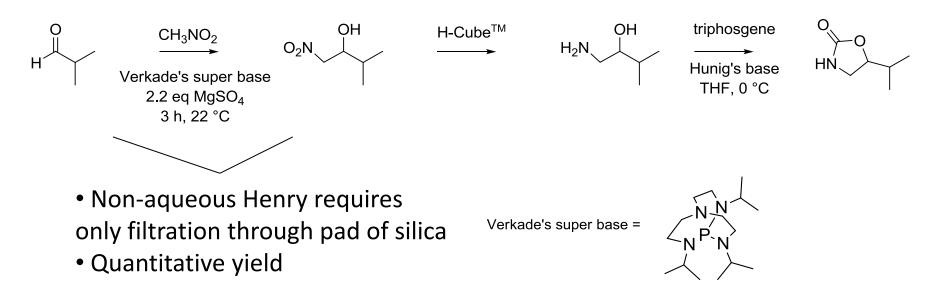
- Henry reaction required tedious extractive workup
- Poor yield in reduction step due to impurities
- Chromatography required





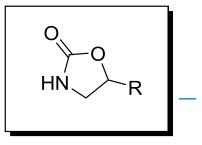
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Parallel amenable route:



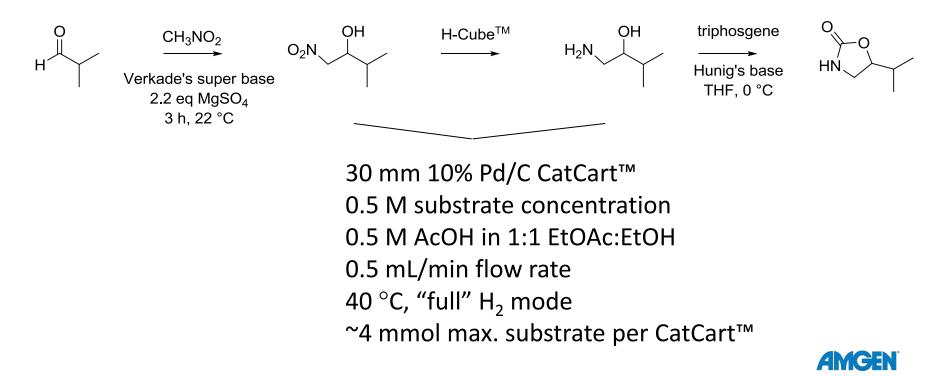
See: Verkade, J. G. J. Org. Chem. 1999, 64(12), 4298-4303.

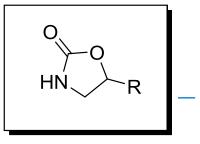




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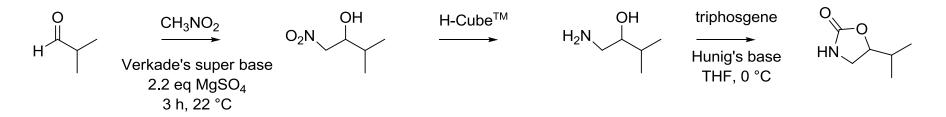
Parallel amenable route:





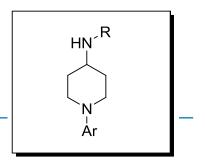
- Project team needed a series of 5-substituted oxazolidinones
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Parallel amenable route:

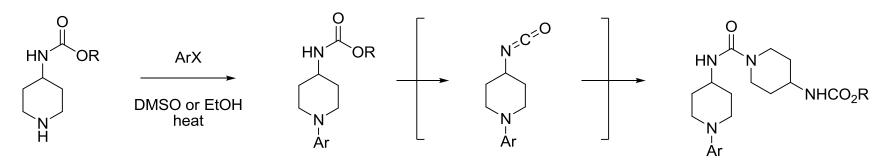


- ✓ Quantitative yields for first two steps
- ✓ No aqueous work-up required until the last step (overall >85% yield)
- ✓ Route was applied to a series of aldehydes to complete project



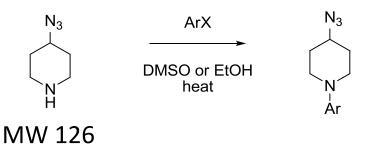


- Target-directed library of aminopiperidines
- CBZ- and Boc- protecting groups proved labile in SnAr

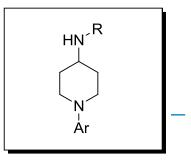


MW 200-234

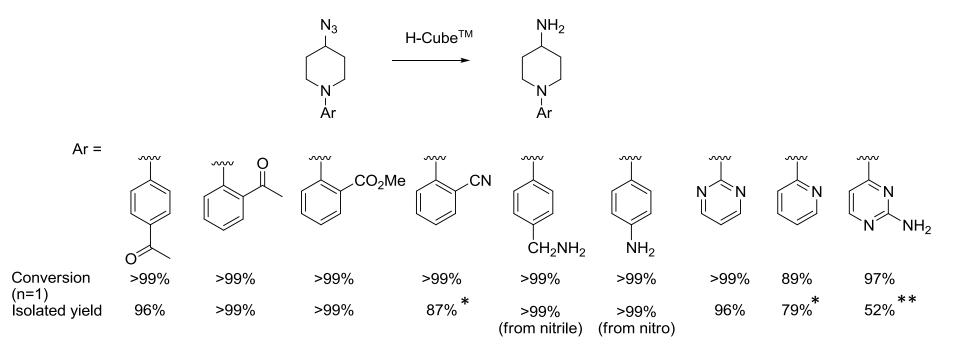
- > Azide afforded cleaner product
- Increased atom efficiency





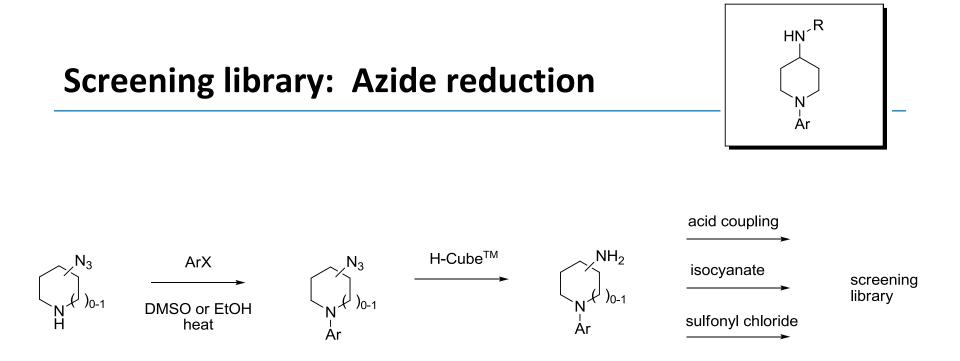


- CatCarts[™] screened : Pd/C, Pt/C, Ir/C, Pd(OH)₂/C, Pt/C (S), Pd-Cu/Al₂O₃
- Solvents screened: THF and MeOH
- Conditions used: 0.04 M THF, 10% Pt/C, "full" H_2 mode, 1.0 mL/min, 30 °C



*over-reduction by-products contributed to low yield **poor recovery from catalyst



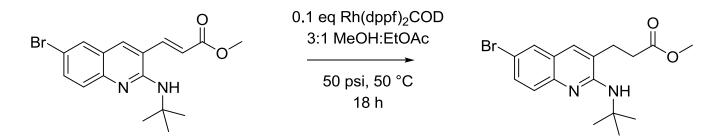


- > Azide route is more atom efficient (lower mass starting material)
- ➤ H-cube[™] reduction facilitates library synthesis
- Scale affords 120 library members per piperidine/pyrrolidine core
- > Final libraries rapidly produced in 24 well plate format



Selective reduction: Intermediate scale-up

Original batch route:



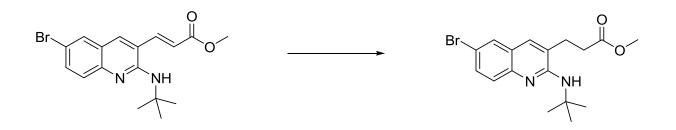
- Several days screening to identify best conditions
- Multiple batches run due to low solubility
- 88% yield after chromatography (5 g scale)

H-Cube[™] continuous flow route?



Selective reduction: Intermediate scale-up

H-Cube[™] route:



- Screened 12 conditions, ~2 h using autosampler
- 5% Rh/C, THF, 80 bar, 30 °C, 2.0 mL/min gave best conversion/selectivity
- 85% yield, @ 0.275 M in THF, 50 mg scale
- 60% yield, @ 0.275 M in THF, 1.0 g scale
- Re-subjecting product mixture to reaction conditions increased side products due to over-reduction, decreased yield

What went wrong?...



...and why is the H-Cube[™] not getting greater use in Amgen Drug Discovery?

Amgen users have experienced:

- Incomplete reductions
- Over-reductions
- Poor reproducibility
- Poor recoveries

Problems may arise from:

- Fluid mechanics issues
- Insufficient hydrogen
- Catalyst deactivation
- Adsorption effects

Can we get a better understanding of these issues and achieve better success with the H-Cube^m?



Characterization of the H-Cube[™]

Using a simple model system (styrene reduction) examine:

- Run to run variability
- Hydrogen flow variability
- Dispersion effects

Develop a screening to scale-up (100 mg -10 g) workflow.

- Conserve material during screening
- Conserve time/volume during scale-up

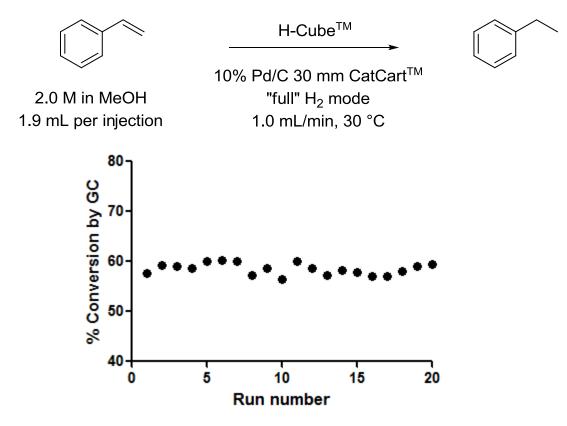
Demonstrate workflow on a relatively "complex" model.

- 1 g scale hydrogenation of methyl 3-bromocinnamate
- Limit undesired side products, maximize yield



Run to run variability

- High concentration of substrate gives incomplete reduction
- CatCart[™] was pre-conditioned (MeOH wash, 10 mL, in H₂ "full" mode)

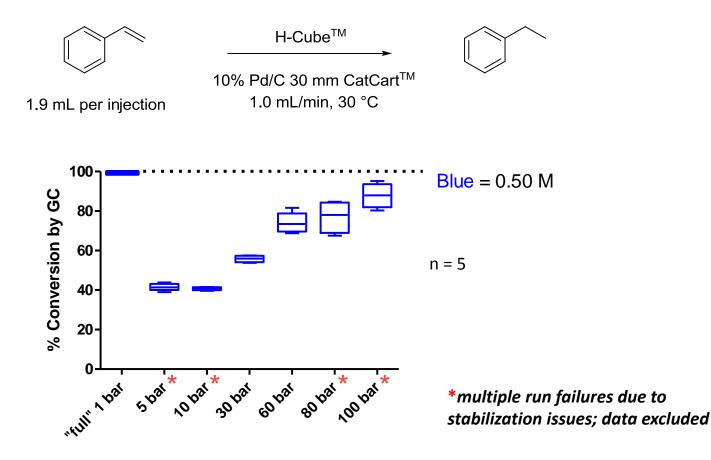


High reproducibility (56.4 – 60.2% conversion) over 20 sequential runs



Variability Associated with Pressure Settings

• Styrene reduction was repeated @ 0.5 M in MeOH, varying pressures



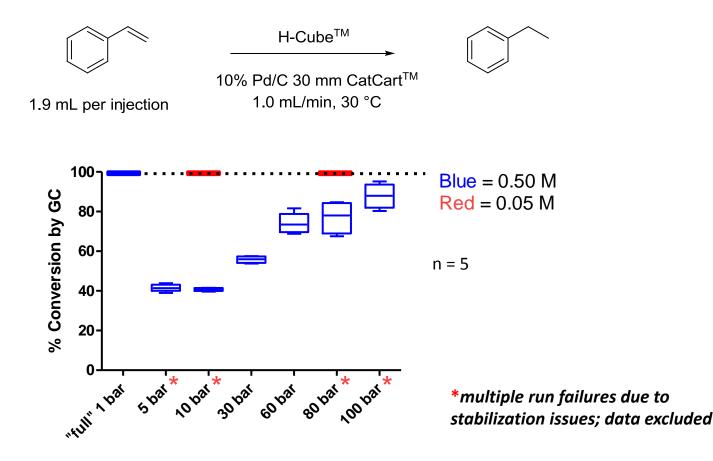
Stabilization issues were more frequent below 30 bar and above 60 bar

Variability increased with increasing pressure



Variability Associated with Pressure Settings

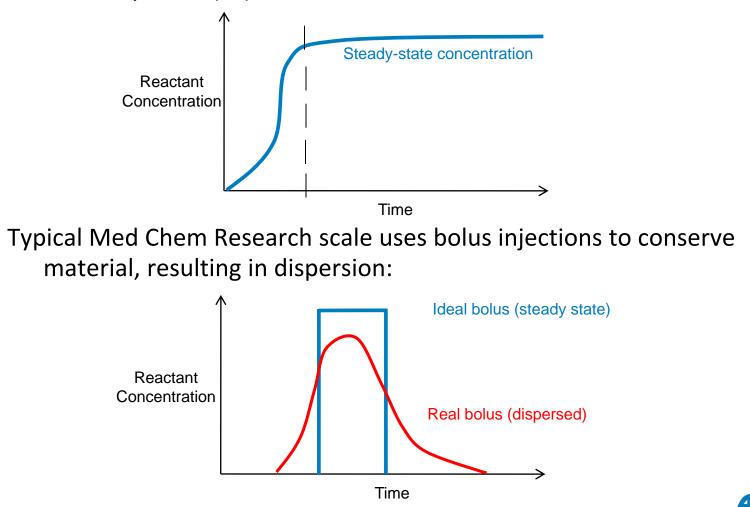
• The reduction was repeated @ 0.05 M, 10 bar and 80 bar only



At lower concentrations (recommended by ThalesNano[©]) variability is not observed.

Dispersion effects

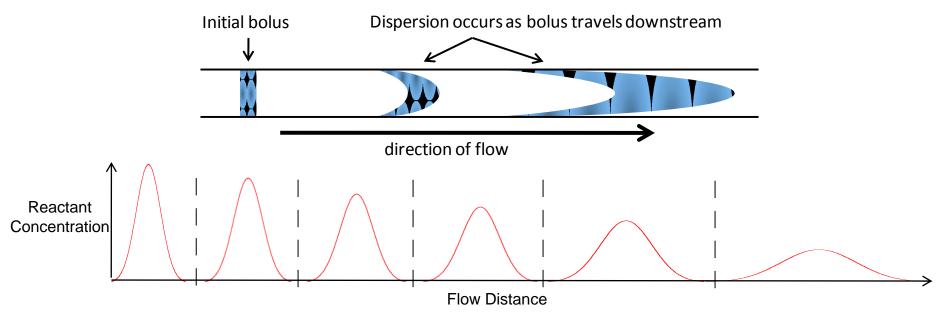
Typical Process Research scale optimization examines parameters at steady-state (SS) concentrations:



Dispersion effects

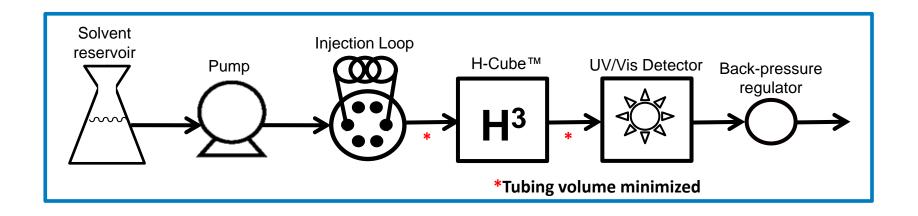
Factors that contribute to dispersion in a packed bed reactor:

- Flow rate
- Diffusion
- Channeling (effected by quality of the packed bed, frits, size/shape of cartridge)
- Particle size (large particle size contributes to dispersion, small size results in increased back pressure)
- Adsorption kinetics





Characterization of dispersion in the H-Cube[™]

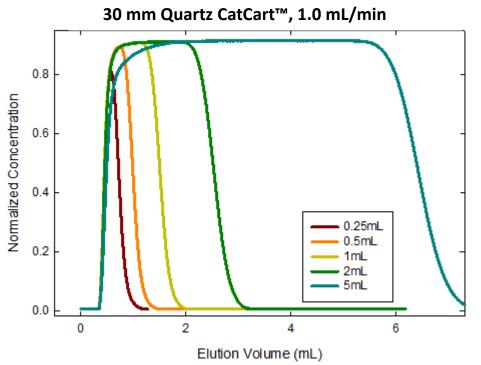


- For the characterization, a UV detector was added in-line
- Manual injections were performed using a sample loop
- Sample loop size was varied to accommodate different injection volumes



Dispersion by UV in the H-Cube™ Reactor

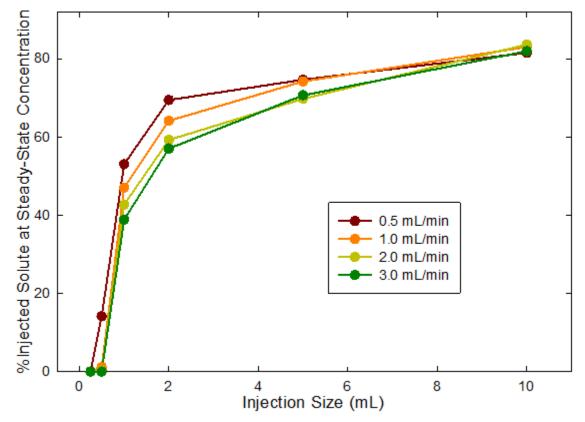
- Bolus injections of caffeine solution made through a 30 mm quartz CatCart[™]
- Injection volumes varied, constant flow rate, no H₂



- The H-Cube[™] introduces dispersion.
- A steady-state concentration equal to that injected can be reached.
- <u>></u>2 mL injection is needed to achieve significant steady-state.



Mass percent at Steady State (SS)



- 2 mL bolus gives ~60-70% mass at SS (flow rate dependent), in a 30 mm quartz CatCart[™] (150 uL void volume)
- >2 mL bolus does not significantly increase mass percent at SS, relative to total volume injected



Design of Experiment (DoE) Optimization of Model Styrene Reduction

Will optimization using 2 mL bolus injections translate to a SS continuous flow scale-up?

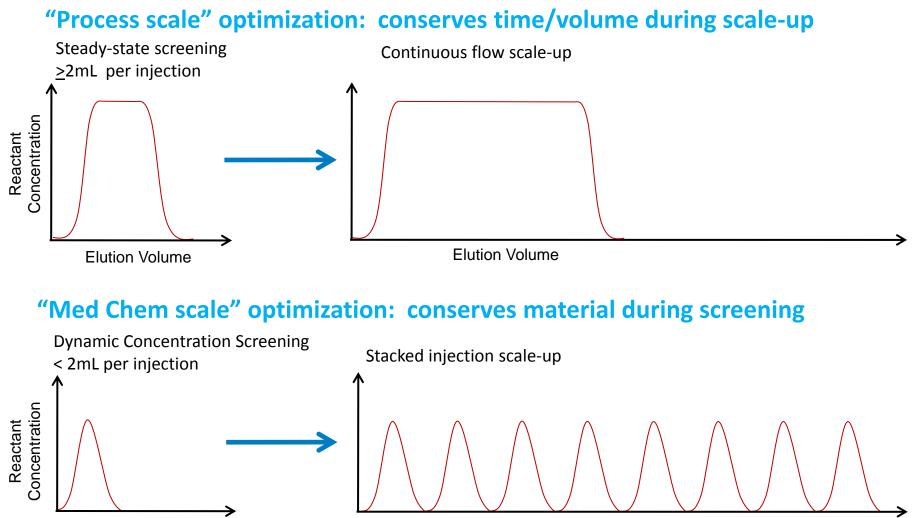
 DoE factors, 2 levels, n=2: Initial Concentration: 0.4 and 0.6 M Pressure setting: 40 and 80 bar Flow Rate: 0.4 and 1.0 mL/min Temperature: 20 and 35 °C Catalyst (10% Pd/C) Loading: 50 mg (micro) and 150 mg

Initial concentration and pressure settings were the most critical factors*

- At 0.4 M and 80 bar: flow rate, cartridge loading, and temperature did not have significant effects
- Using the DoE optimized conditions >90% conversion was achieved upon scale-up (>1 g) in continuous mode
- However, >3 g starting material was consumed during optimization



Scale-up in Continuous Mode vs. Stacked Injections

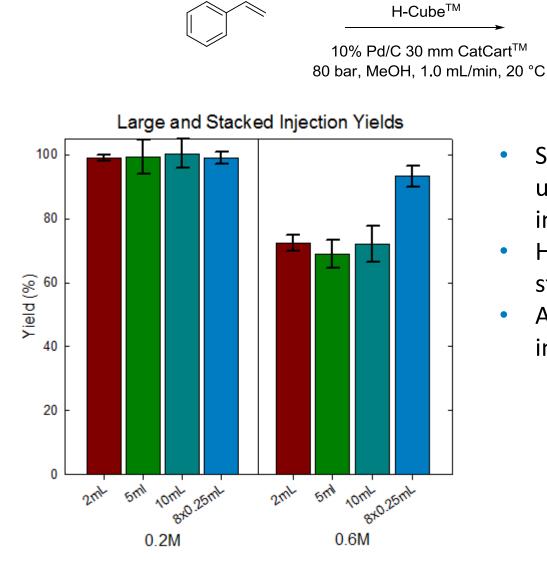


Elution Volume

Elution Volume



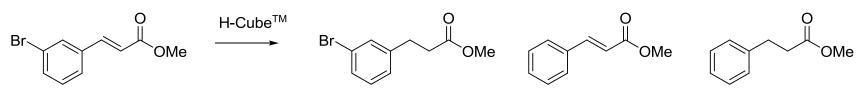
Scale-up in Continuous Mode vs. Stacked Injections



- Styrene reduction yield unaffected by increasing injection volume
- High yield at 0.2 M achieved with stacked injections (0.25 mL)
- At 0.6 M, stacked injections increased yield ~15%



More "Complex" Scenario: Adsorption Effects



undesired side-products

- Goal: 1 g scale, high yield, low impurity profile.
- Minimal catalyst screen showed 5% Rh/C CatCart[™], THF as best option.
- DoE optimization, 2.0 mL injections, 3 factors (n=3 for each):
 - Initial conc.: 50 and 250 mM

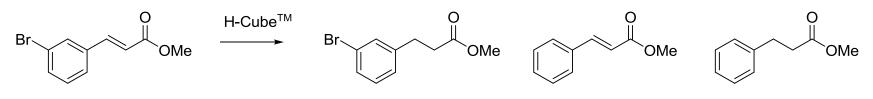
- Pressure: "Full" and 50 bar

- Flow rate: 0.5 and 2.0 mL/min

- DoE optimized conditions (50 mM, "full" mode, 2.0 mL/min, 30 °C)
 - afford **95%** yield in 2 mL injection (24 mg reactant)
 - afford 60% yield in continuous mode (1 g reactant)

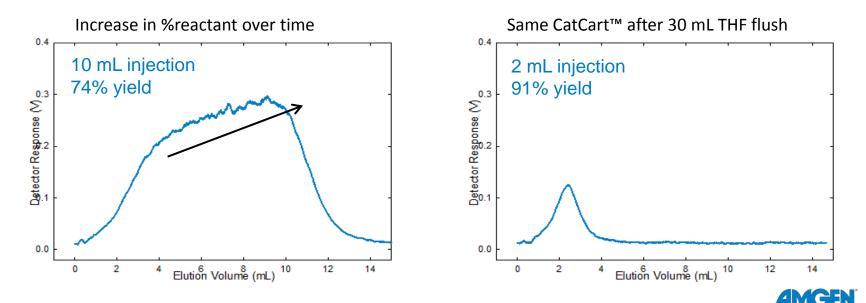


More "Complex" Scenario: Adsorption Effects



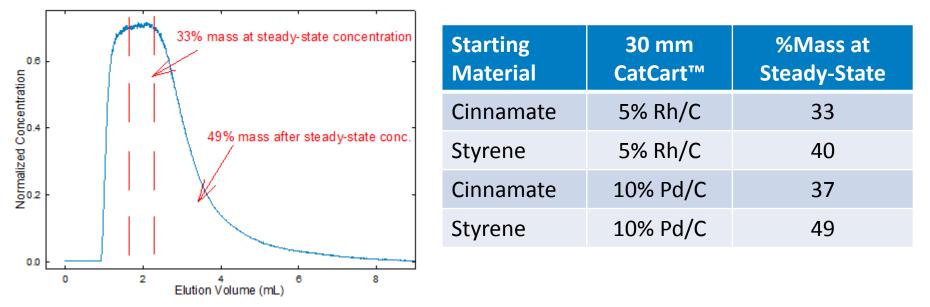
undesired side-products

- Deactivation observed over 10 mL injection
- Increasing temperature to 60 °C increased yield ~10%
- Catalyst recovers after washing



Effect of Chemotype and Catalyst on Adsorption

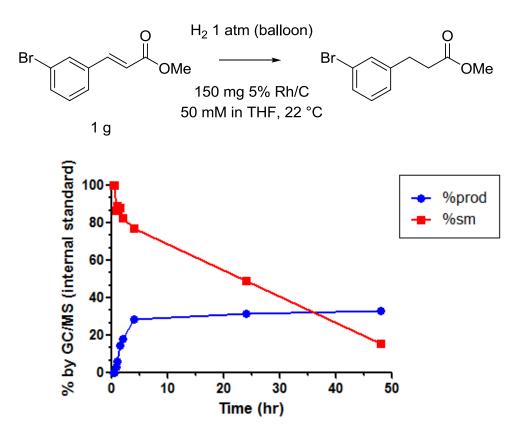
50 mM methyl 3-Br cinnamate THF, 2 mL at 2.0 mL/min, no H2



- Mass delivered at the steady-state concentration is chemotype and catalyst dependent.
- Study of these adsorption effects is in progress.



Comparison to Batch



- 33% yield after 48 hr in batch mode, with 51% by-products
- 60% yield in 45 min in continuous flow, <1% by-products</p>



Conclusions

What we've recommended to our colleagues...

For simple reductions on large scale (1-10 g), the stand alone H-Cube can be used with 2 mL injections for steady state reaction optimization prior to continuous flow scale-up.

> For the typical Med Chem application (<1 g), use dynamic screening followed by stacked injections for best results.

Scale in batches, using multiple CatCarts, when catalyst deactivation may be an issue.

Use the controlled mode feature with caution, with the understanding that higher pressures lead to higher variability and failed runs due to instability.



Thank you

At Amgen :

- David Wernick (UCLA intern)
- Callie Bryan (Medicinal Chemistry Research Technologies)
- John Eschelbach (Discovery Analytical Sciences)
- Jim Petersen (Research Automations Technologies)
- Alan Allgeier (Catalysis and Hydrogenation Group)
- Peter Grandsard
- Randall Hungate

At ThalesNano:

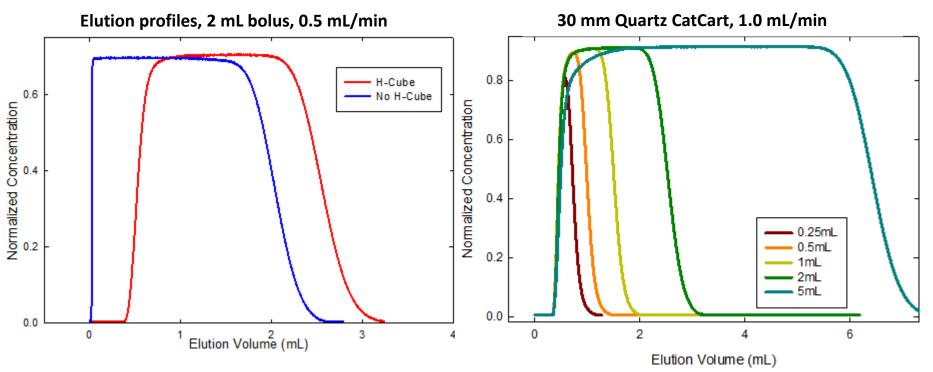
- Richard Jones
- Laszlo Urge
- Paul Whittles
- Alan Boyle

RSC/SCI Symposium coordinators and speakers Glaxo SmithKline



Dispersion by UV in the H-Cube™ Reactor

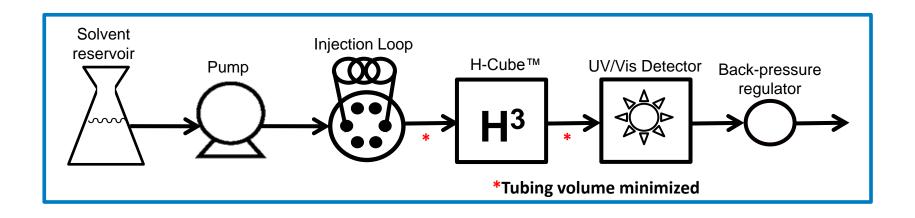
- 1. Bolus caffeine solutions, with and without the H-Cube[™] (quartz CatCart[™])
- 2. Injection volumes were varied



- The H-Cube[™] introduces dispersion.
- A steady-state concentration equal to that injected can be reached.
- 2 mL or larger injection is needed to achieve significant steady-state.



Characterization by UV

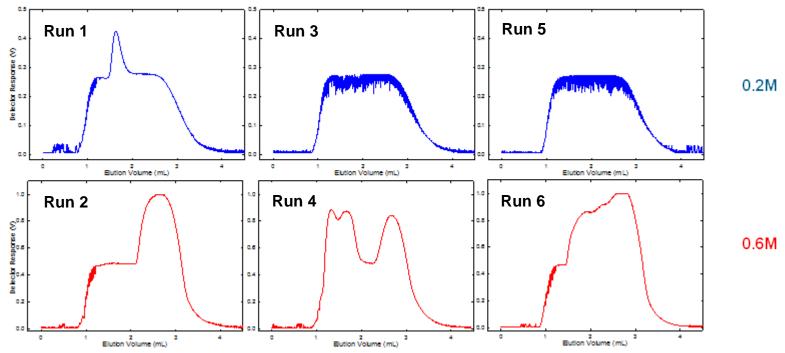


- UV detector was added in-line to follow the course of styrene reduction and examine dispersion effects
- $\epsilon_{styrene}$ >> $\epsilon_{ethylbenzene}$
- An increase in absorbance is associated with a decrease in product formation
- Under styrene reduction conditions *where hydrogen is limiting*, UV monitoring affords an indirect measure of hydrogen production



Hydrogen flow variability by UV

- 2 mL injections @ 0.2 M or 0.6 M styrene in MeOH
- 80 bar, 1.0 mL/min, 30 mm 10% Pd/C, 30 °C
- Monitored at 265 nm



Reaction rate drops significantly at several points, suggesting interruption of hydrogen flow.

