



Oilfield Fluids: Tales of Mud and Worms

Geoffrey Maitland
Department of Chemical Engineering



Rideal Lecture
Wednesday 28th March 2012

Collaborators

Schlumberger:

Louise Bailey, Isabelle Couillet,
Trevor Hughes

Imperial College:

Edo Boek, John Crawshaw

Utrecht University:

Henk Lekkerkerker, Annemieke ten Brinke,
Marcel Vogel, Dzina Kleshchanok

Strasbourg ICS, CNRS

Francoise Candau, Jean Candau

Twente University:

Wim Briels, Johan Padding (Eindhoven)

Bristol University:

Terence Cosgrove, Vania Croce

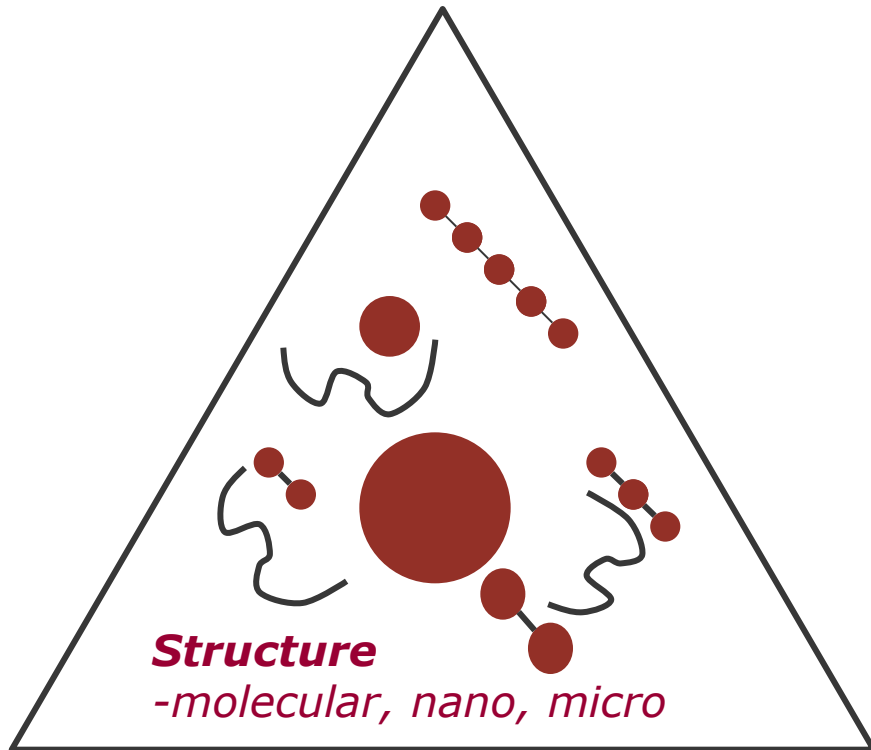
Cecile Dreiss (KCL)

Lecture Outline

- Design of Fluids and Materials
 - Advanced Formulation and (More) Systematic Design of Fluids
- The Worm's Tale
 - Smarter Fracturing Fluids
- The Potter's Tale
 - Clays for Drilling Fluids – enhancing performance
- Some Conclusions

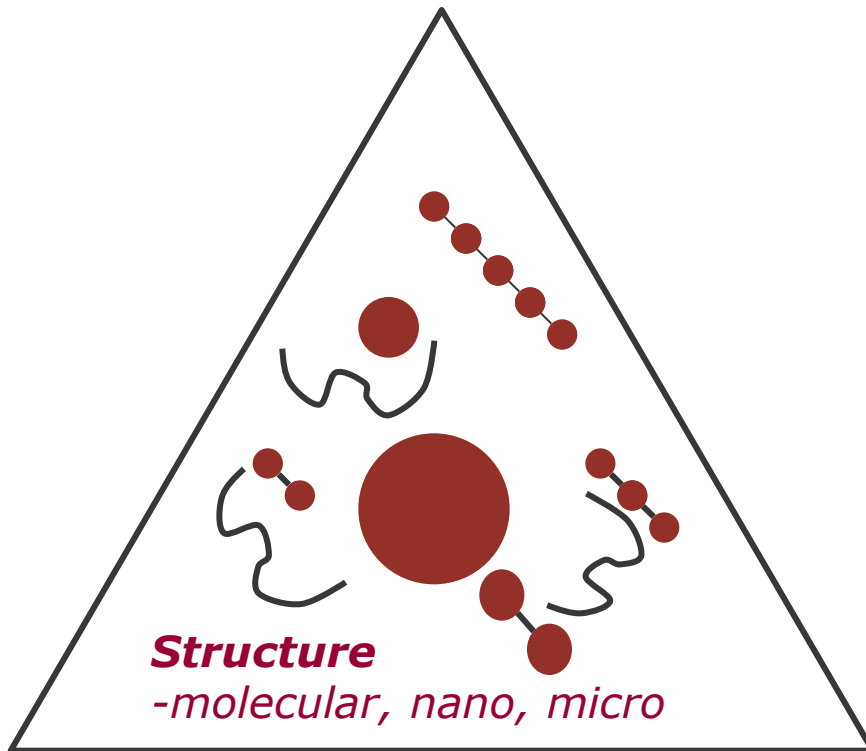
From Understanding to Designing Fluids

Composition – molecules
and molecular assemblies



From Understanding to Designing Fluids

Composition – molecules
and molecular assemblies



Structure
-molecular, nano, micro

Forces

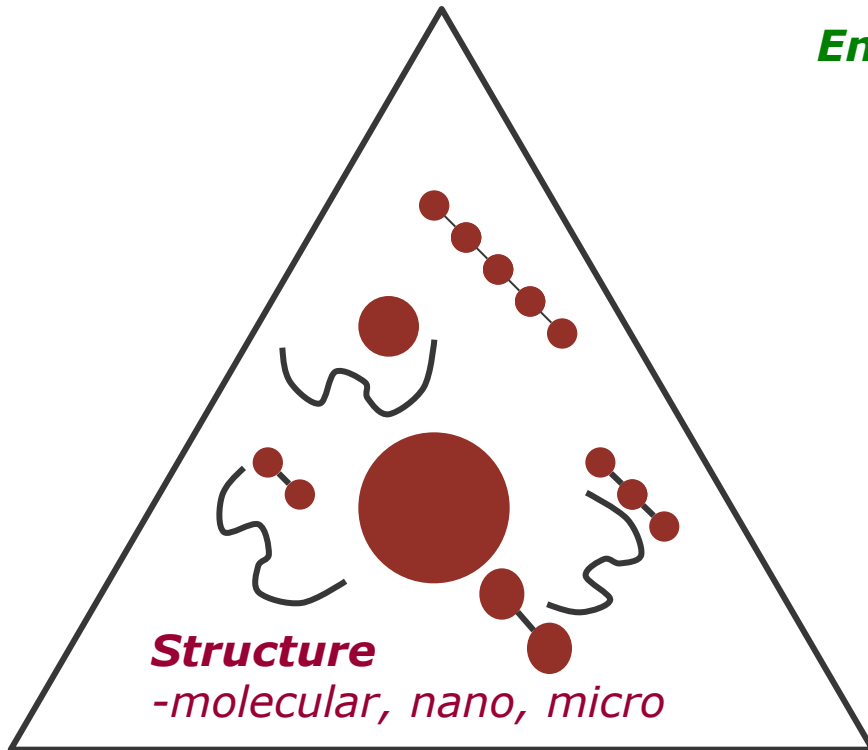
Bulk Properties



Process

From Understanding to Designing Fluids

Composition – molecules
and molecular assemblies



Environmental Compliance

Market acceptability

Cost

Material availability

Process

Bulk Properties

Forces

From Understanding to Designing Fluids

Composition – molecules and molecular assemblies

**Which Components?
How much of each?**

Structure
-molecular, nano, micro

Environmental Compliance

Market acceptability

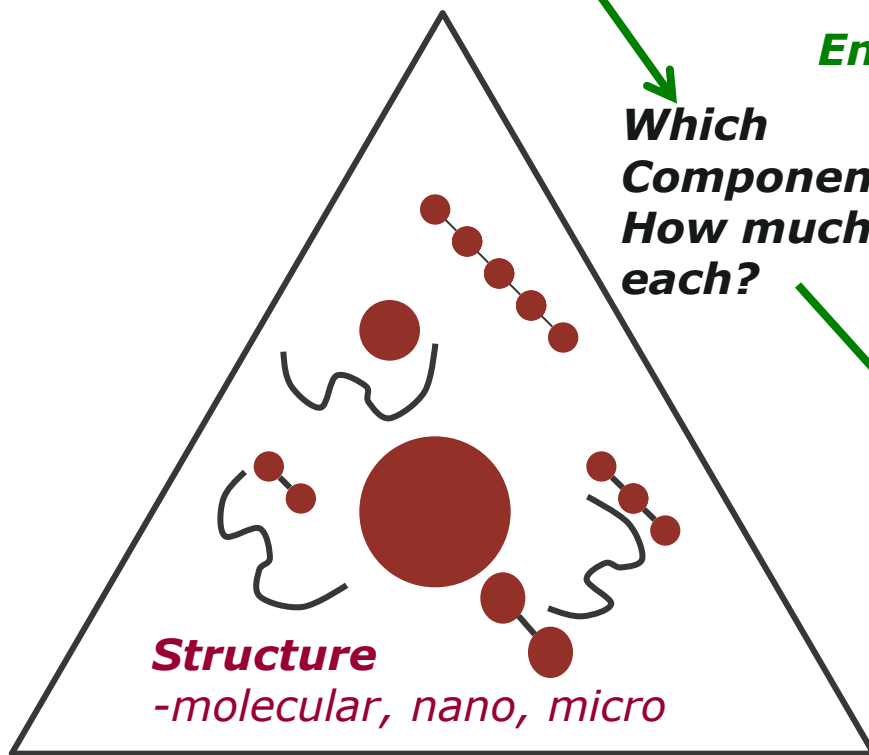
Cost

Material availability

Process

Bulk Properties

Forces

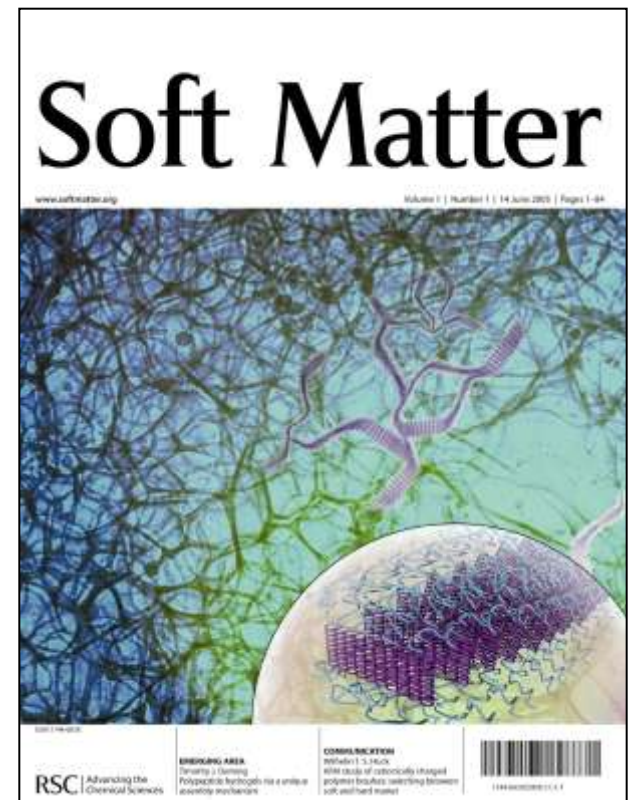


From Empirical Formulation to Systematic Fluid/Materials Design

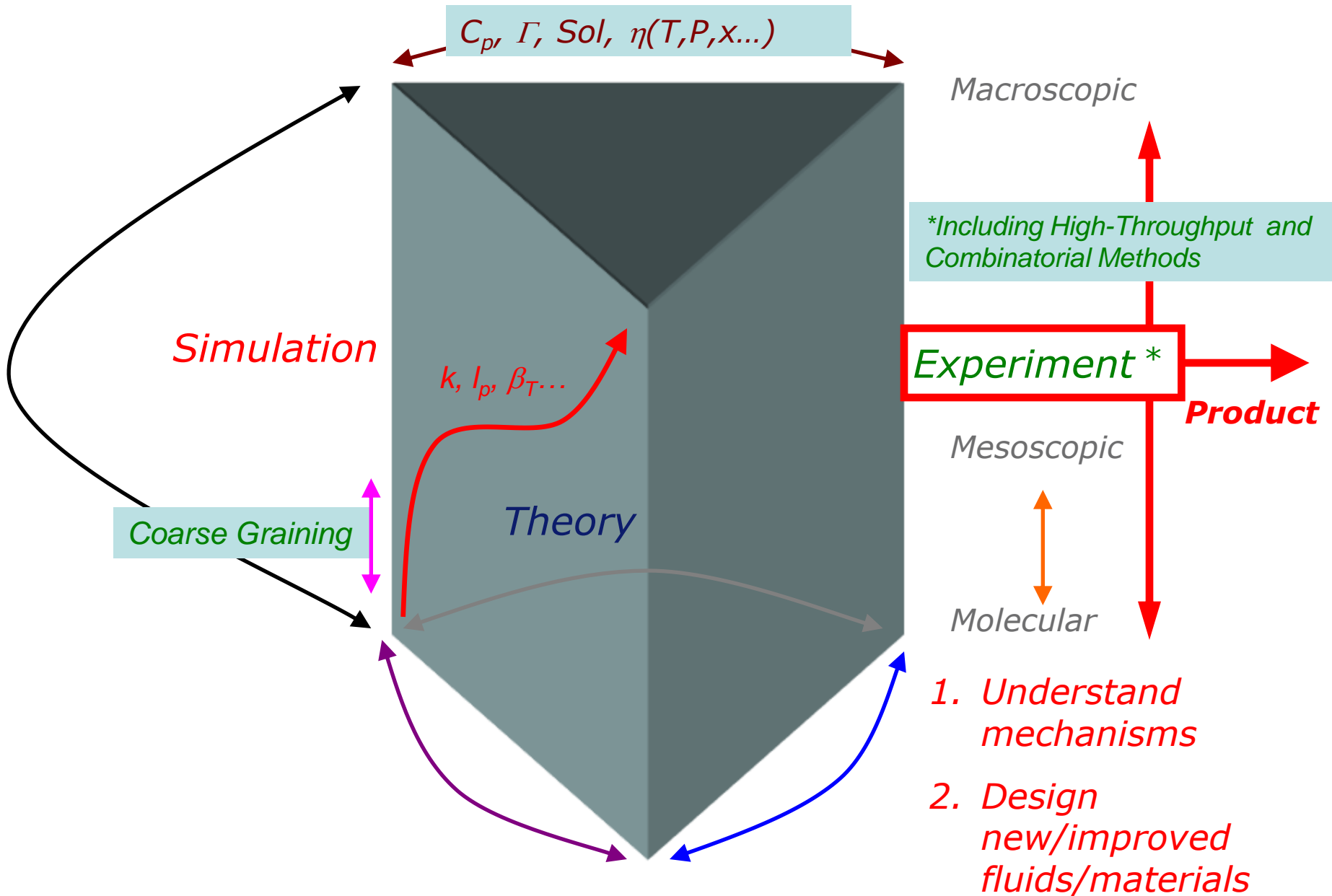
Editorial:

G.C. Maitland

Transforming 'formulation':
systematic soft materials design
Soft Matter, 2005, 1(2), 93 - 94



Systematic Fluid Formulation

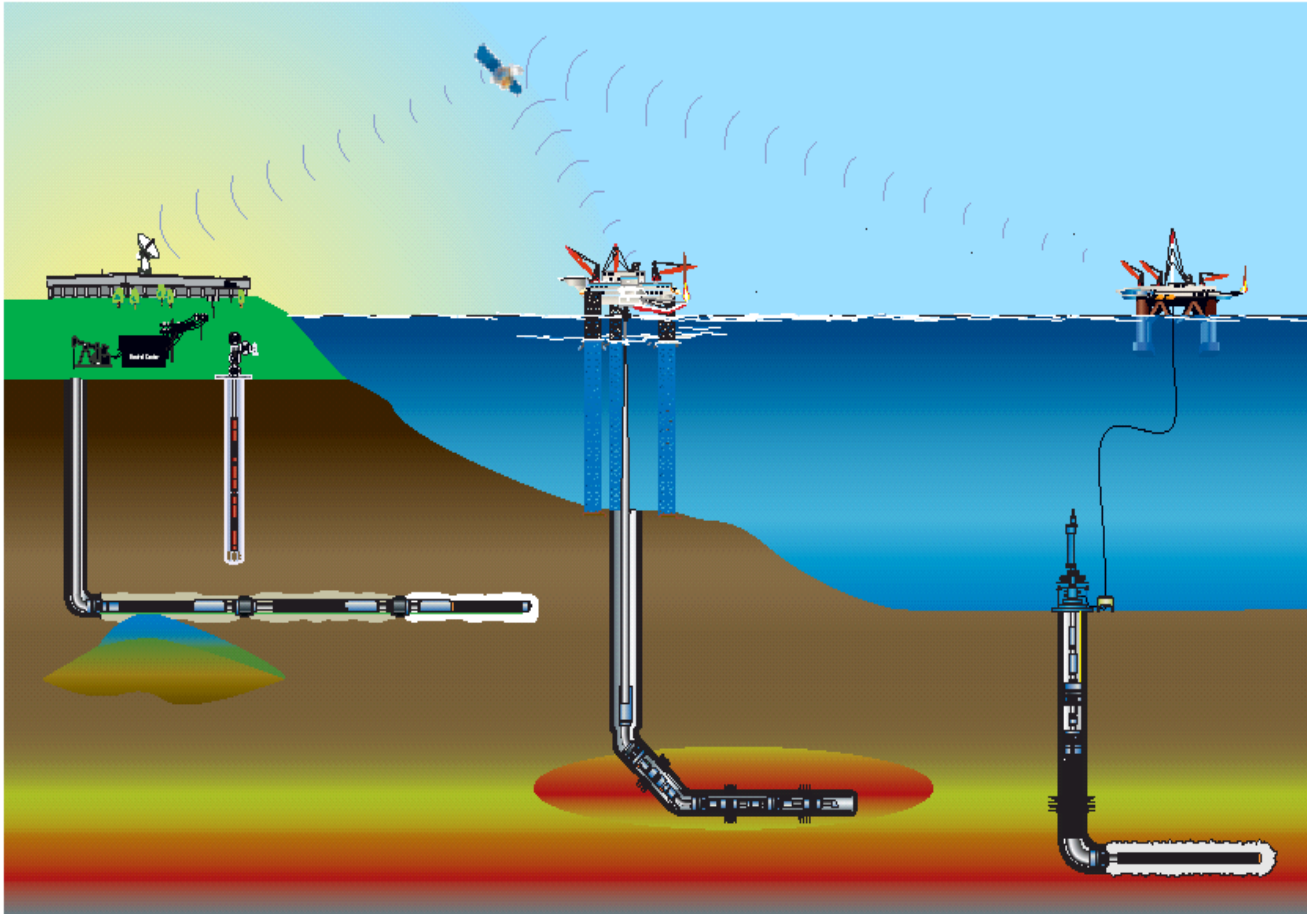


Main building blocks for (oilfield) functional fluids

- Hydrocarbons
 - Aliphatics, aromatics, polar...
- Polymers
- Surfactants
- Colloids
 - Mineral colloids
 - Anisotropic clays...

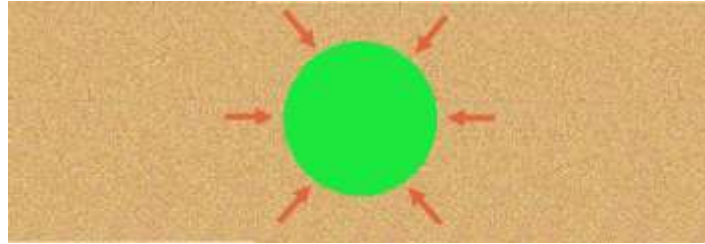
The Worm's Tale

Stimulating an oil-gas reservoir by Hydraulic Fracturing



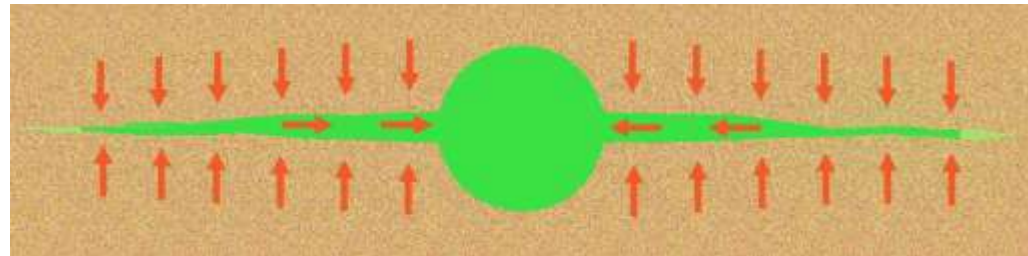
Hydraulic Fracturing

*Before
Treatment*



Flow restricted by radial geometry

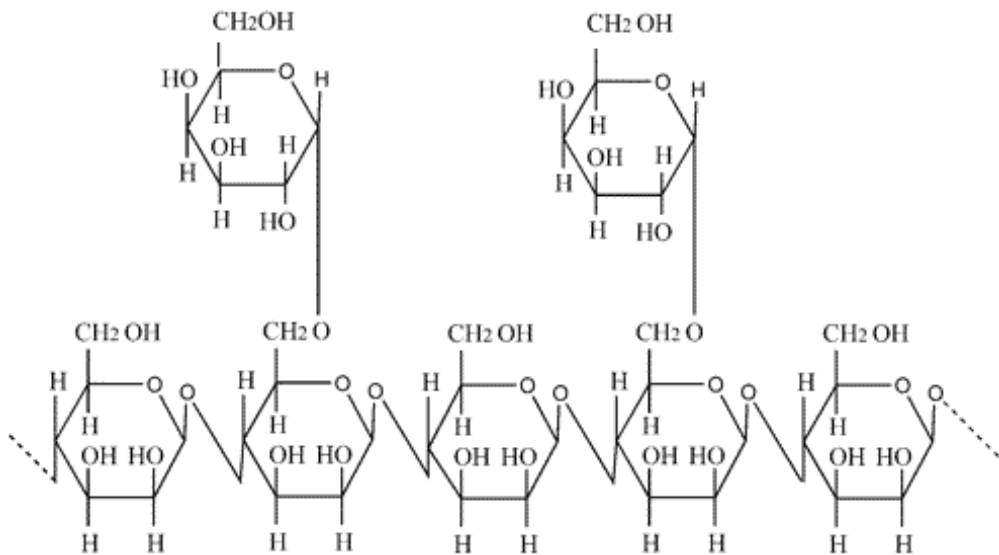
*After
Treatment*



Increased productivity through fractures

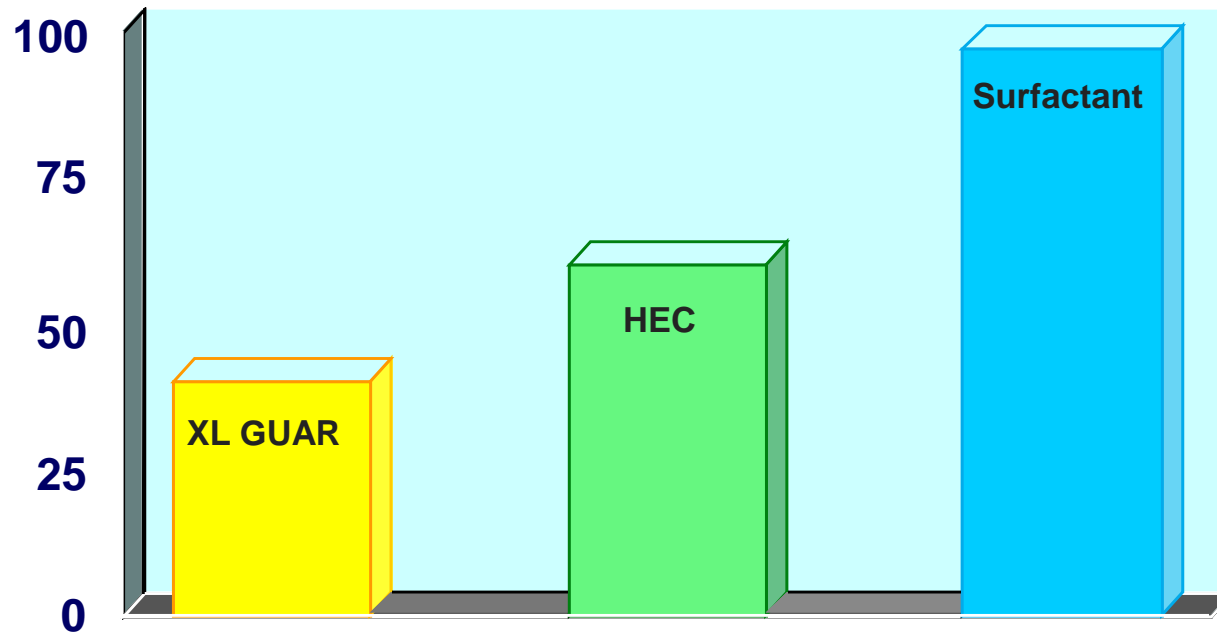
Aqueous Solutions of Guar – the Standard Fracturing Fluid

Guar: Galactomannose, $M \sim 10^5$ - 10^6



The Problem - Polymer vs Surfactant Fluids: Fracture Permeability

**Retained
Permeability (%)**



Low Production...Worms to the rescue!

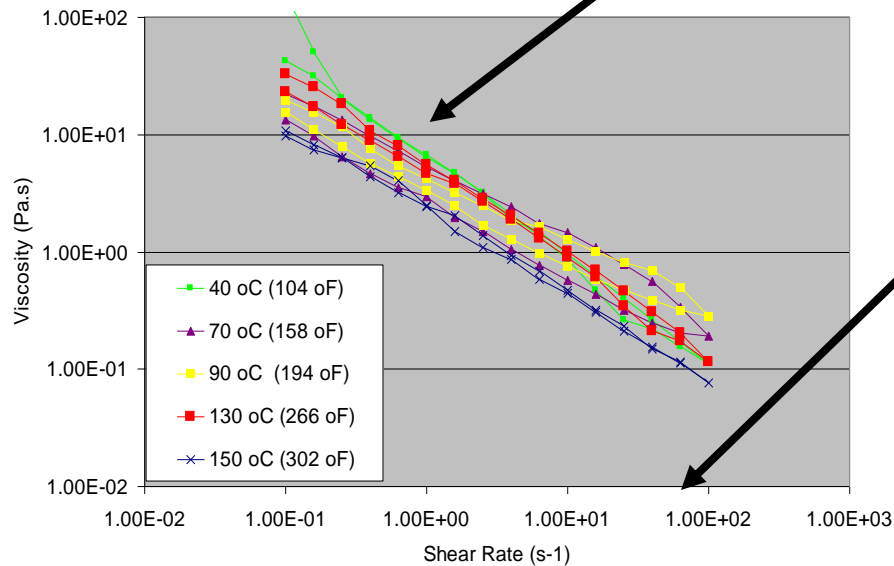
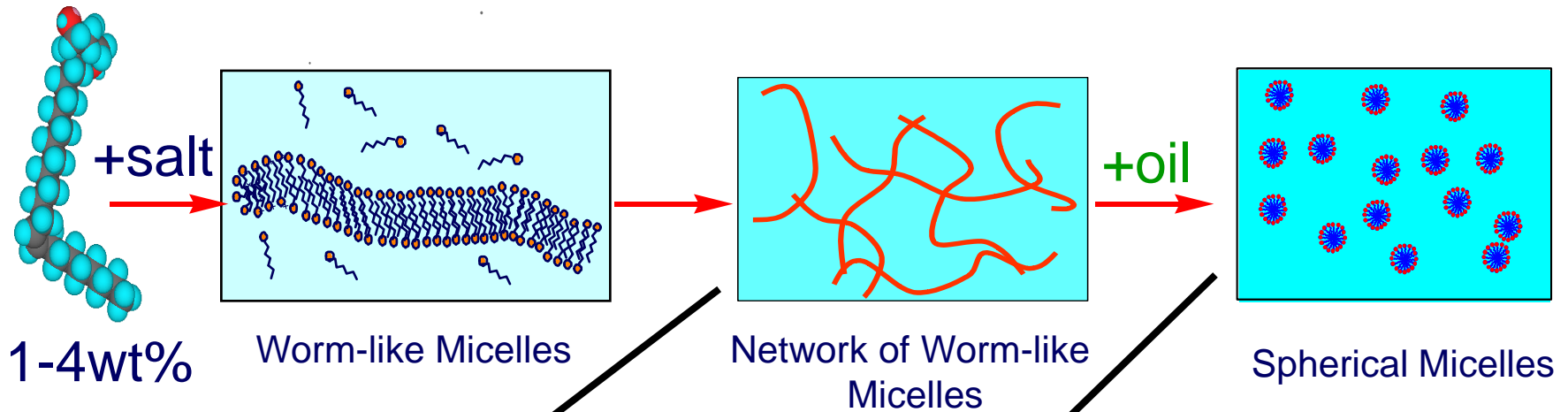
Problem:

Guar Polymer Fracturing Fluids give
<50% Theoretical Production from
Fractures

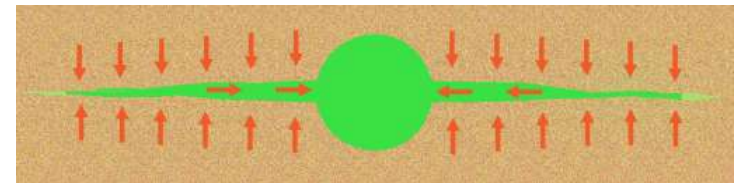
Solution:

Shower Gels for Deep Hot Wells -
Wormlike Surfactant Micelles at $>150^{\circ}\text{C}$

Oil-responsive Viscoelastic Surfactants



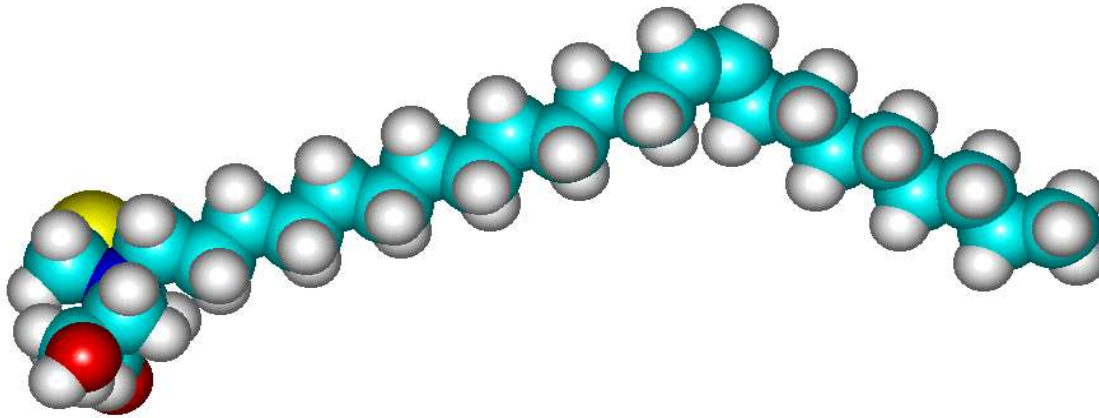
Hydraulic Fracturing



One Source of Worms...

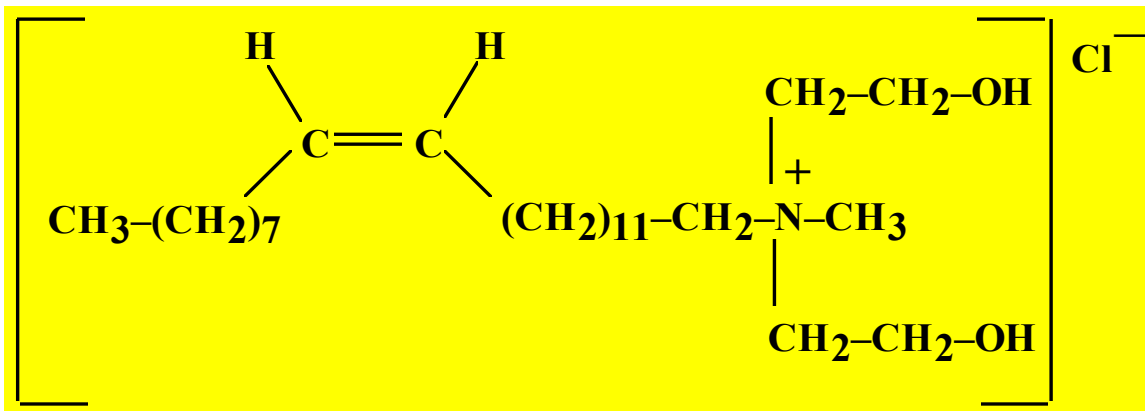


Viscoelastic Surfactant Fracturing Fluids



Erucyl bis (2-hydroxyethyl) methyl ammonium chloride

EHAC



- **Hydrophobic tail**

- C₂₂ chain
- cis double bond at C₁₃

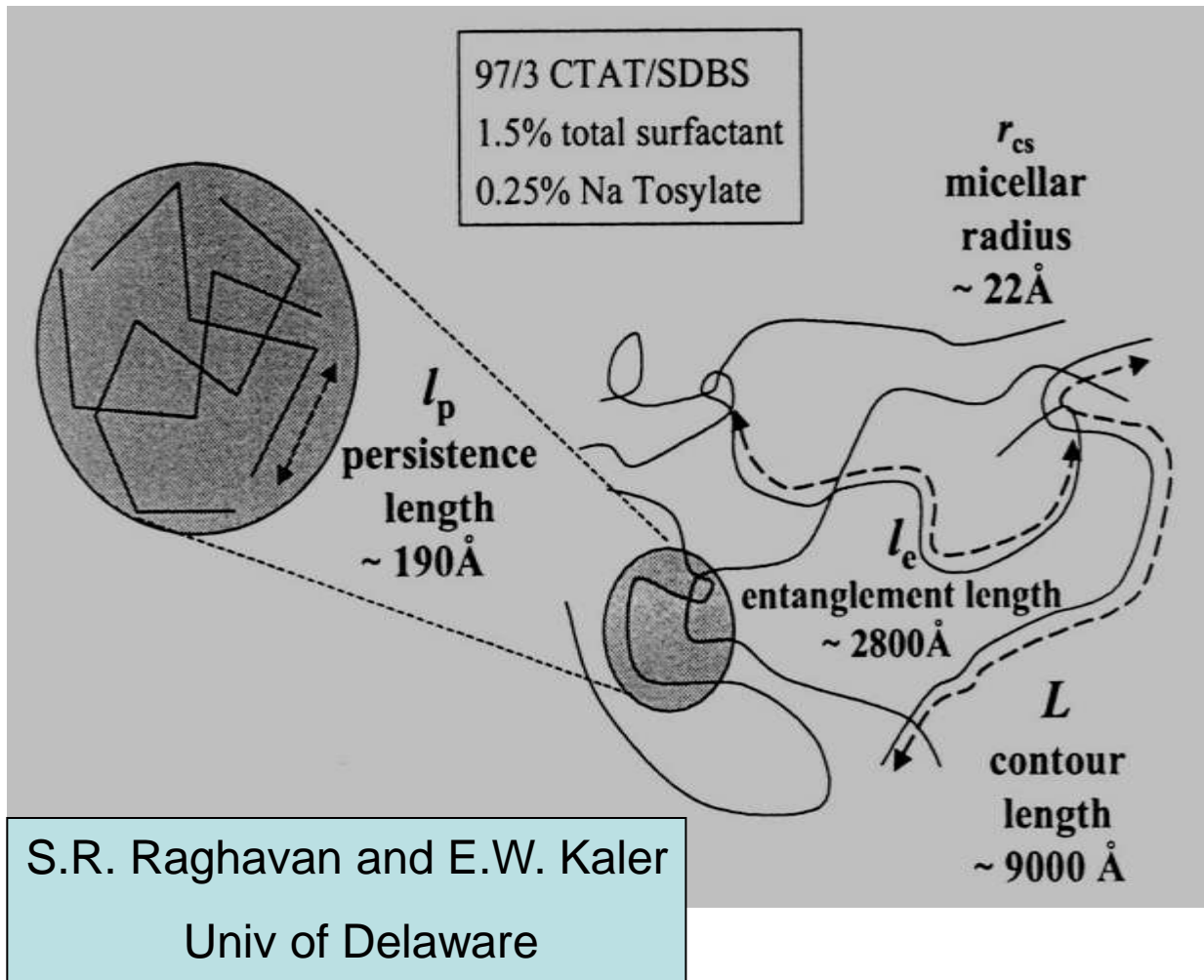
- **Hydrophilic head group**

- quaternary ammonium with 2 hydroxyethyl groups

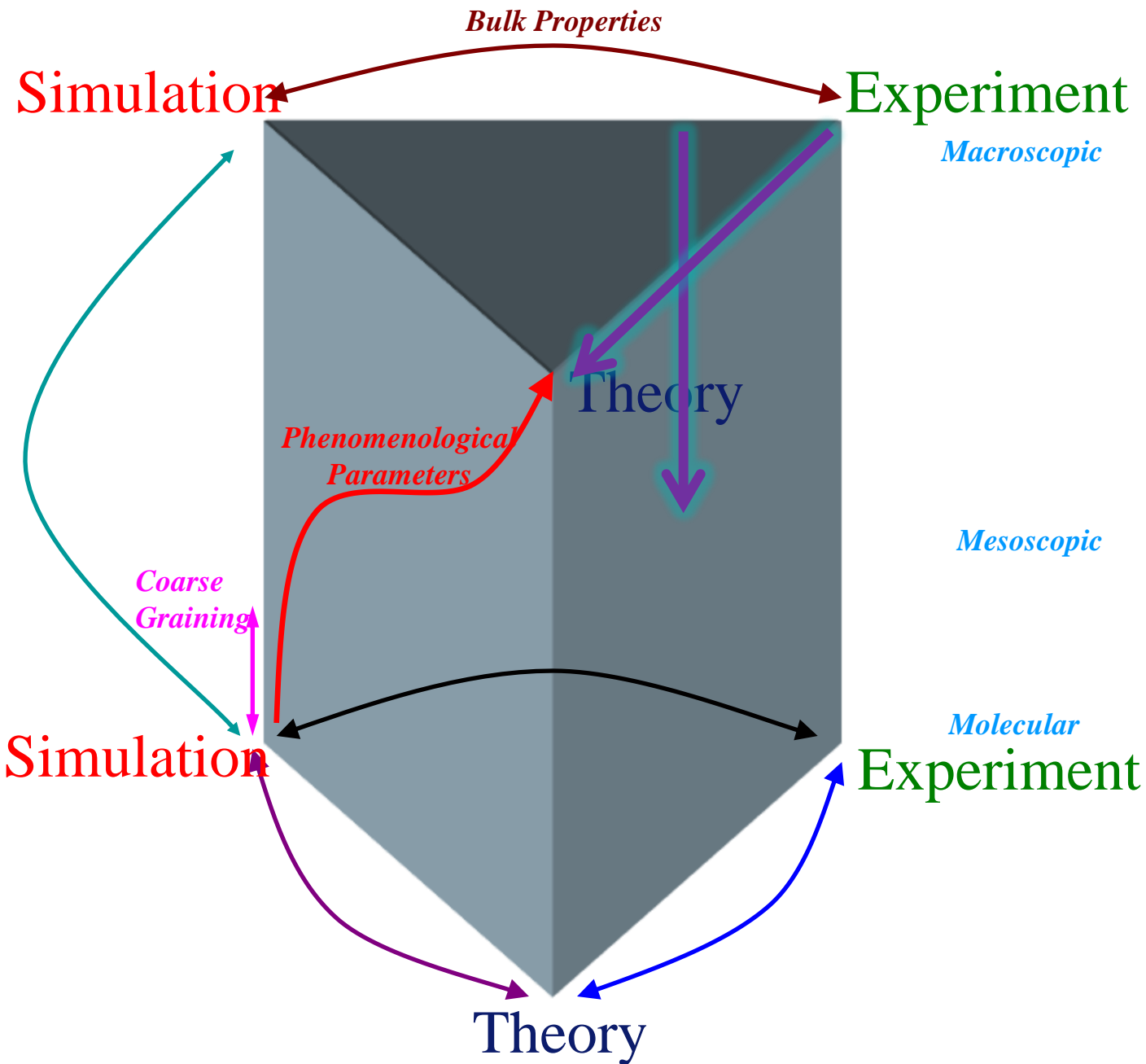
- **Derived from rape seed oil**

- **Blended with iso-propanol**

Typical Lengthscales



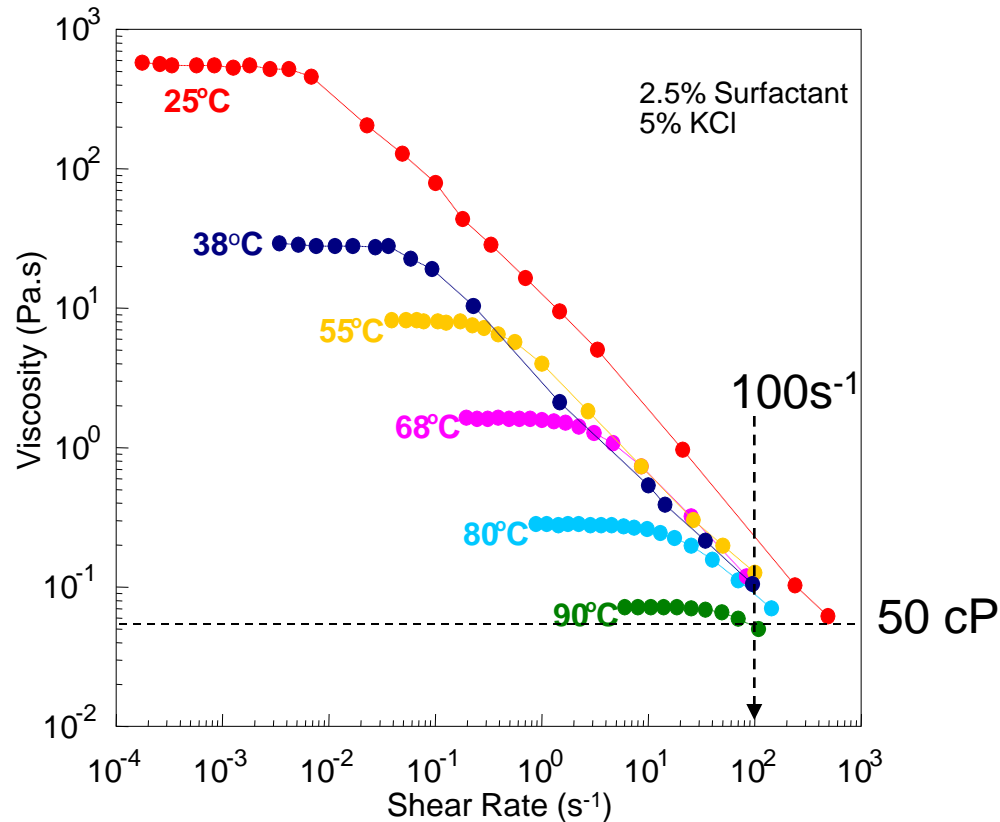
Type of Study



Bulk Rheology

Continuous Shear Flow

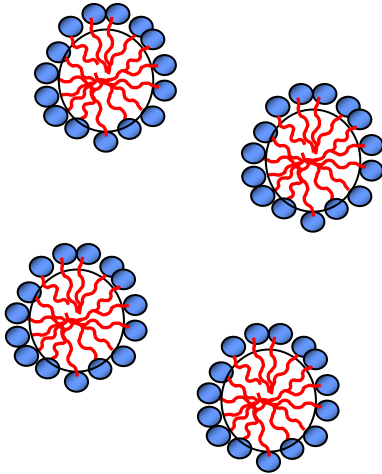
VES Shear Viscosity



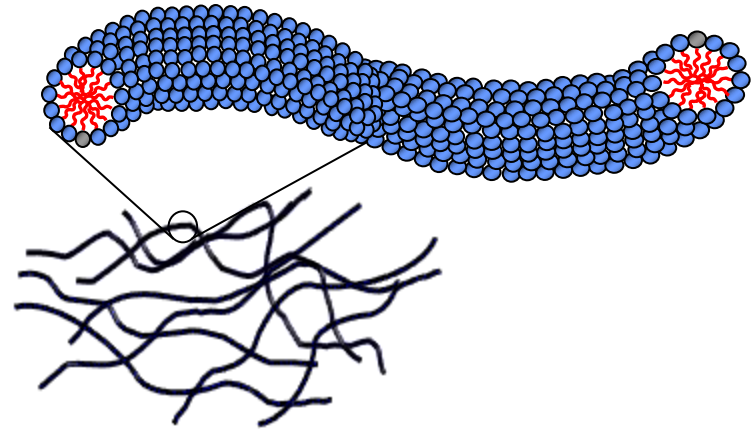
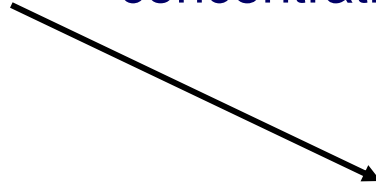
- Zero-shear viscosity, η_0 decreases as $T \uparrow$
- Relaxation time, $\tau_R (= 1/\gamma_c)$ decreases as $T \uparrow$
- Viscosity at high shear-rates is nearly independent of T

Origin of Viscoelasticity and High Viscosity

Spherical Micelles



Increasing salt,
concentration



*Transient Network
of Wormlike Micelles*

Micelles are very long, 1-5 μm

Since $\tau_R \sim \eta \sim L^3$

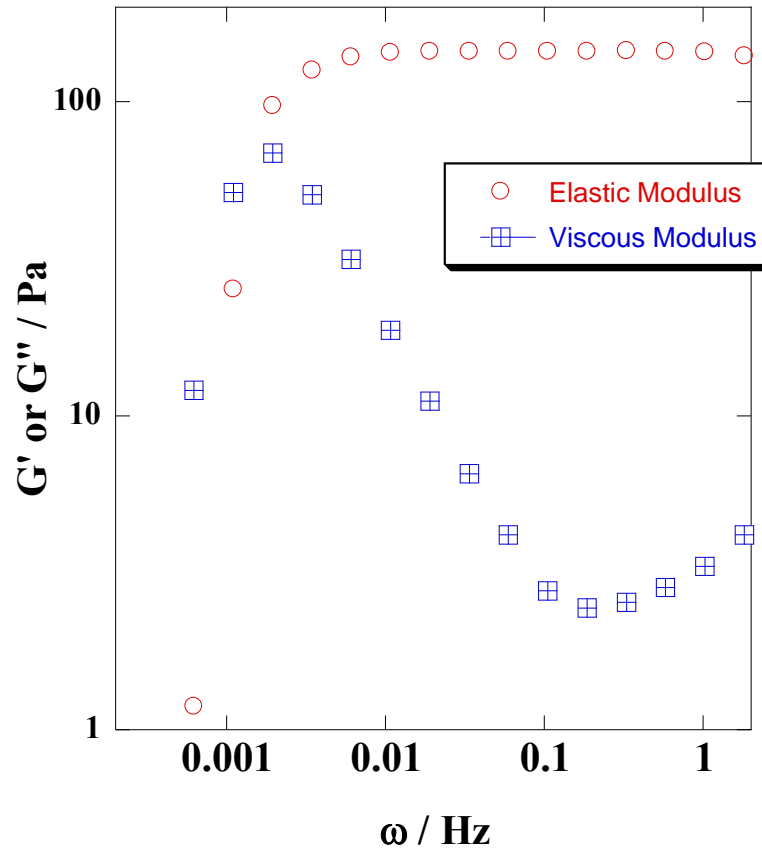
\Rightarrow micelles relax slowly

\Rightarrow high viscosity

Bulk Rheology

Oscillatory Shear Flow

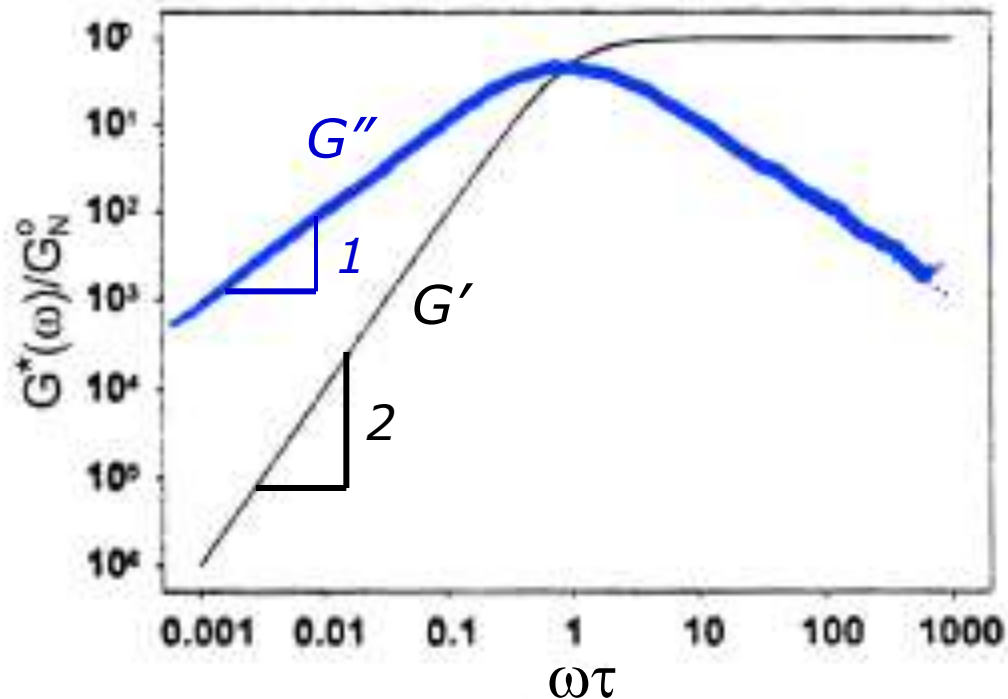
Display Simple Linear Viscoelastic Behaviour



VES Surfactant Solution

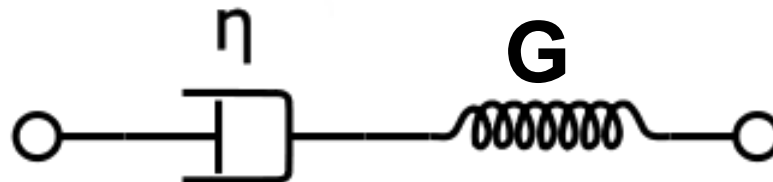
Maxwell Model for Linear Viscoelasticity

$$G' = \frac{G \omega^2 \tau^2}{1 + \omega^2 \tau^2} \quad G'' = \frac{G \omega \tau}{1 + \omega^2 \tau^2}$$

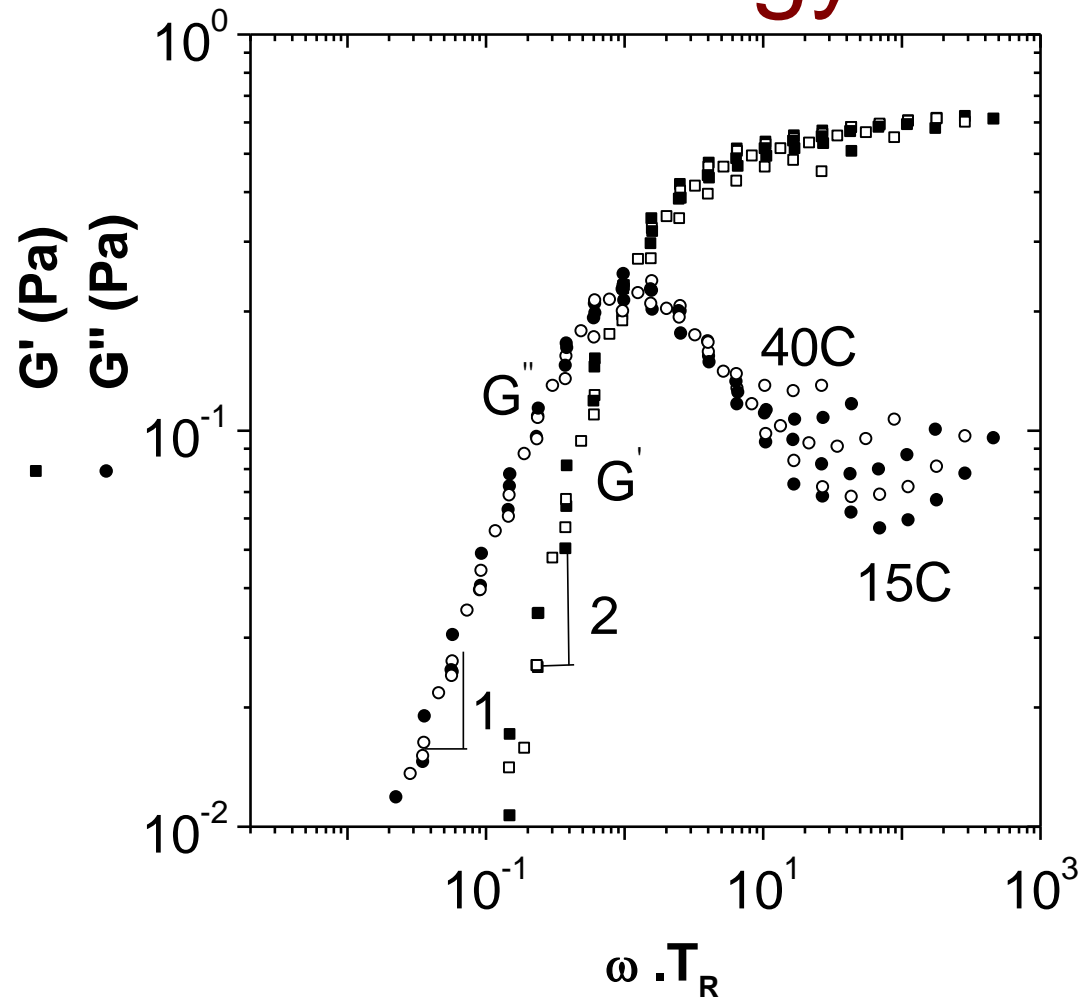


Relaxation Time
 $\tau = \eta/G$

$$\tau + \frac{\eta}{G} \frac{d\tau}{dt} = \eta \frac{d\gamma}{dt}$$

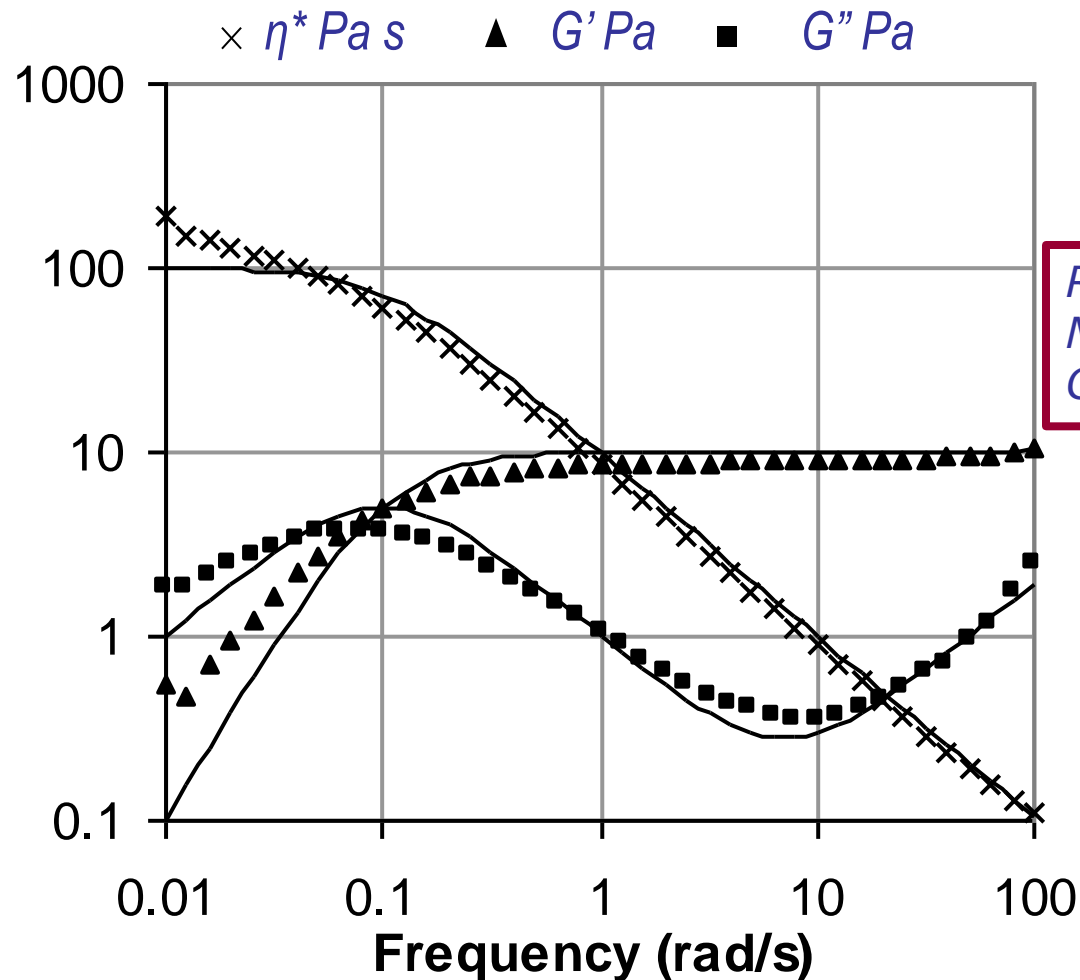


Dynamic shear rheology master curve



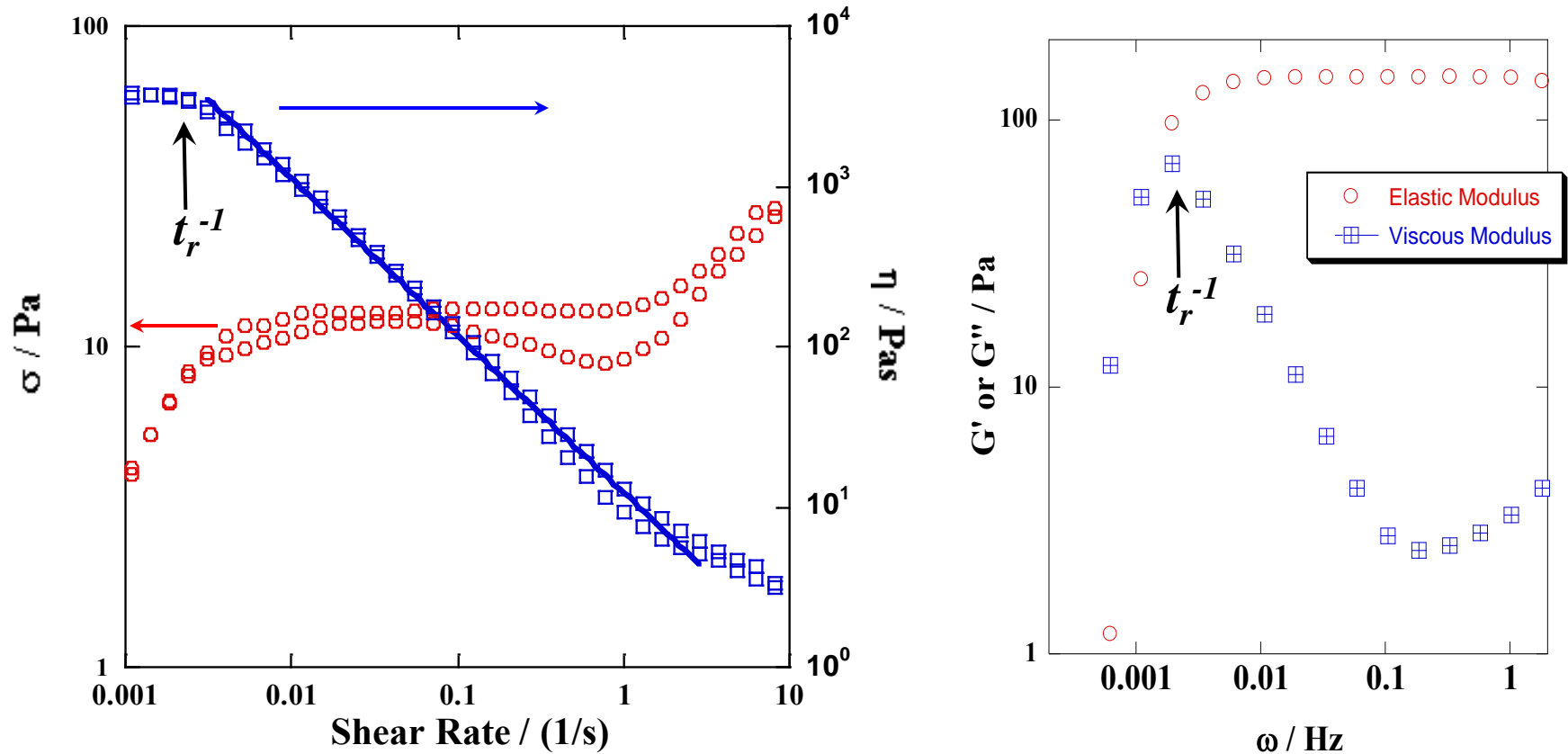
Rheological master curves for dynamic shear for a sample at 14.4 mM active EHAC concentration with 400mM KCl, obtained by scaling the data generated at various temperatures (15,20,25,30,35 and 40 °C).

Linear Viscoelastic Regime



*3 wt% EHAC surfactant, 3 wt% potassium chloride solution at 40 °C.
Data fitted to a **2 element Maxwell model**.*

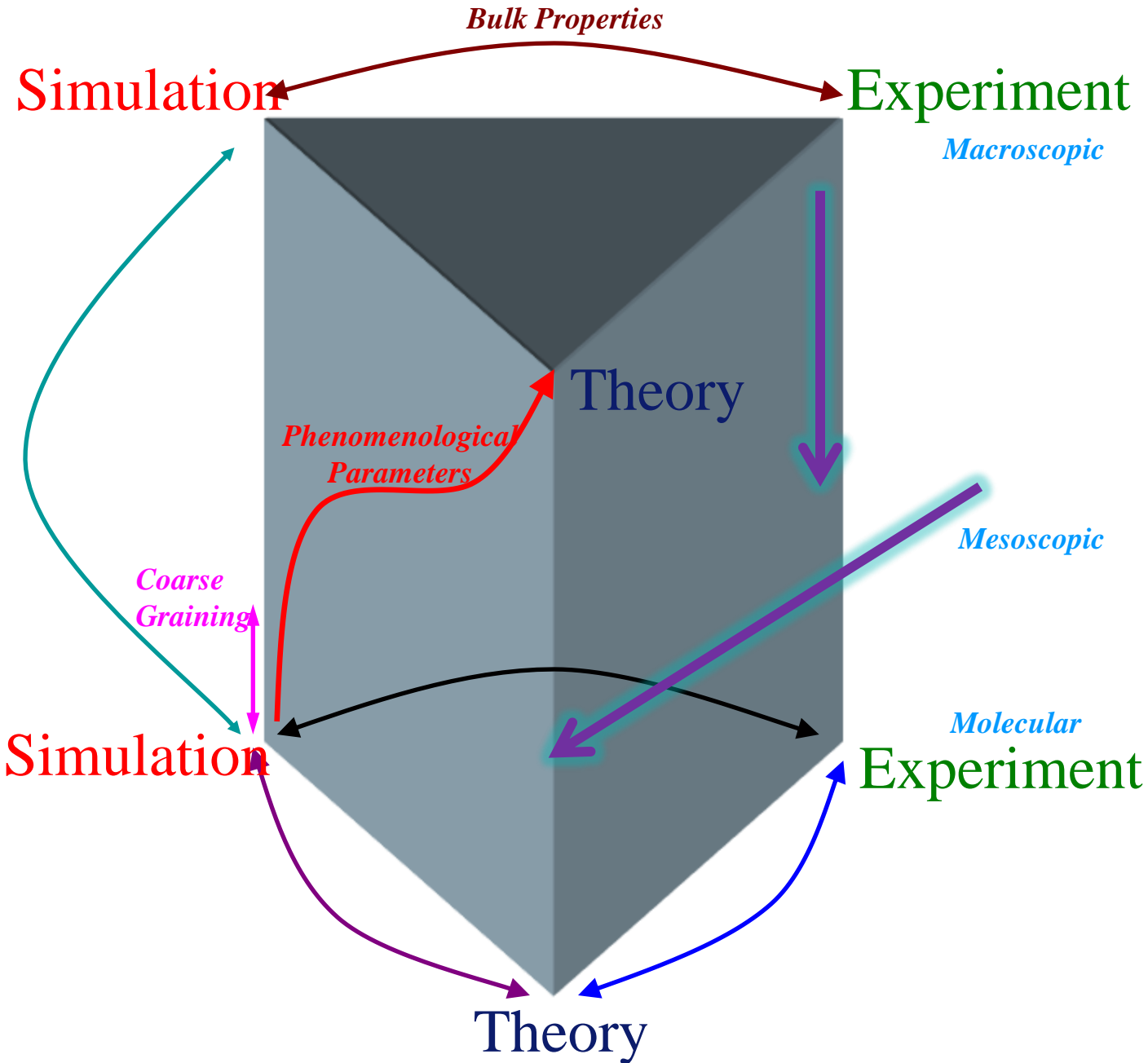
Bulk Rheology of VES Fluids



Both types of behaviour in line with the 'Reptation-Reaction' model of Cates, later adapted to $\eta(\dot{\gamma})$ by Spenley, Cates and McLeish.

$$t_r = (\tau_R \tau_b)^{1/2}$$

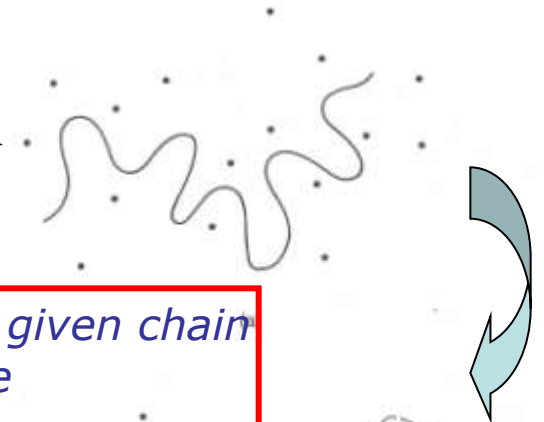
Type of Study



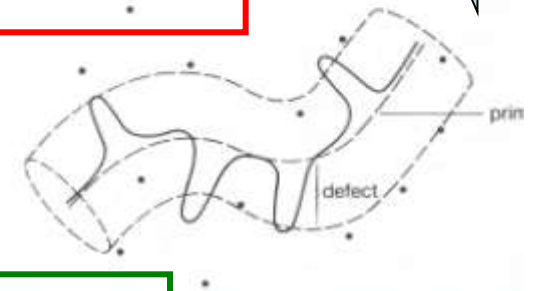
Chain Constraints – Reptation in a Tube



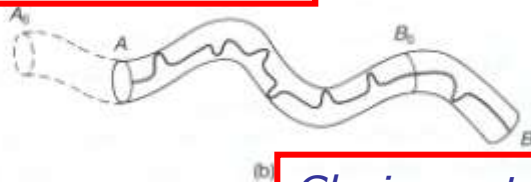
*Repulsive interchain forces →
Entanglements - moving obstacles*



*Obstacle course for a given chain
represented by a tube*



Reptation time τ_R



*Chain reptates down the tube
which is continually renewed
as other chains move*

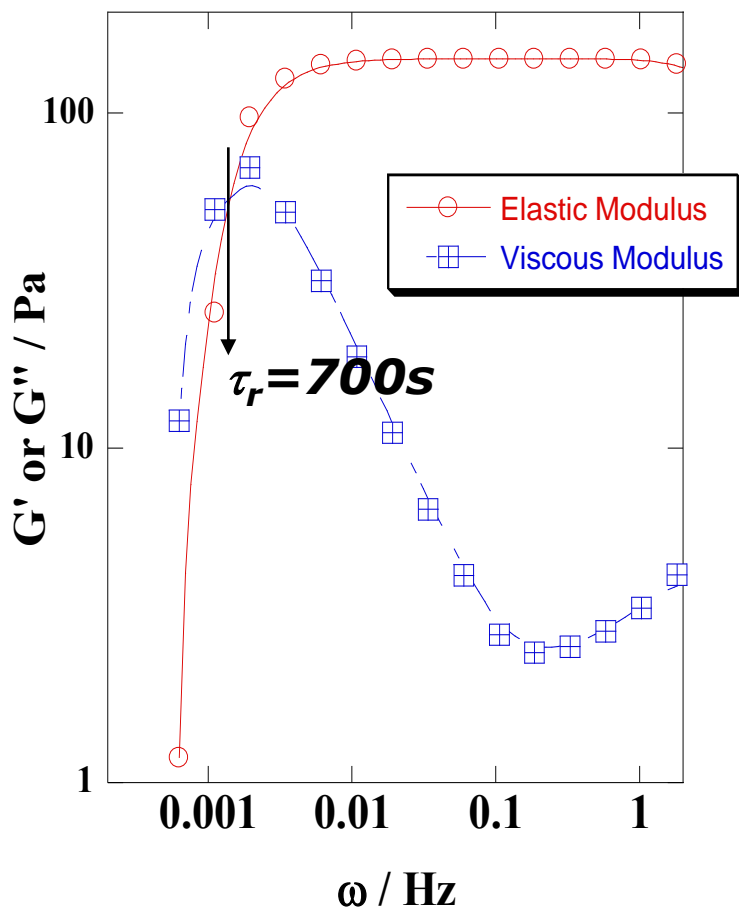
$$\eta \sim \tau_R \sim L^3$$

Cates-type models

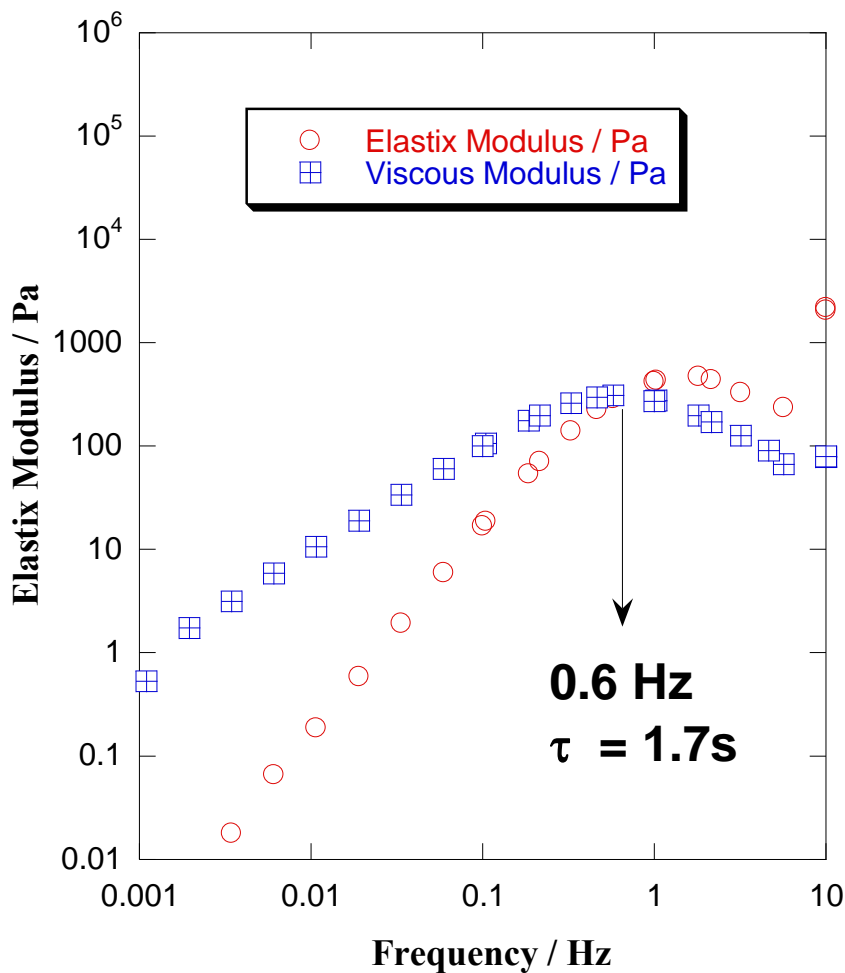
- Assume two main processes:
 - Reptation, τ_{rep}
 - Chain scission-rehealing, $\tau_{\text{br}} = (KL)^{-1}$
- Slow scission limit, $\tau_{\text{br}} \gg \tau_{\text{rep}}$
 - Terminal relaxation time $\tau_R = \tau_{\text{rep}}$
 - $\eta_0 = L^3 c^{15/4}$
- Fast breaking limit, $\tau_{\text{br}} \ll \tau_{\text{rep}}$
 - $\tau_R = (\tau_{\text{br}} \tau_{\text{rep}})^{1/2}$
 - Maxwell behaviour for G' , G'' with $\tau = \tau_R$
 - $\eta_0 \sim Lc^3$
- Rouse modes at higher frequency if $\tau_{\text{Rouse}} < \tau_{\text{br}}$

Effect of Headgroup on Relaxation Time

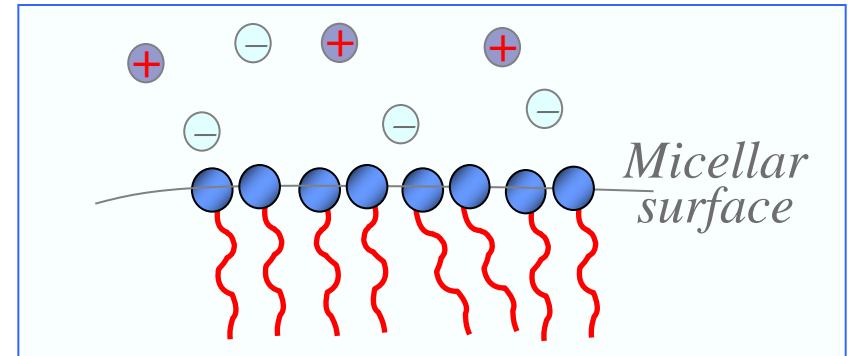
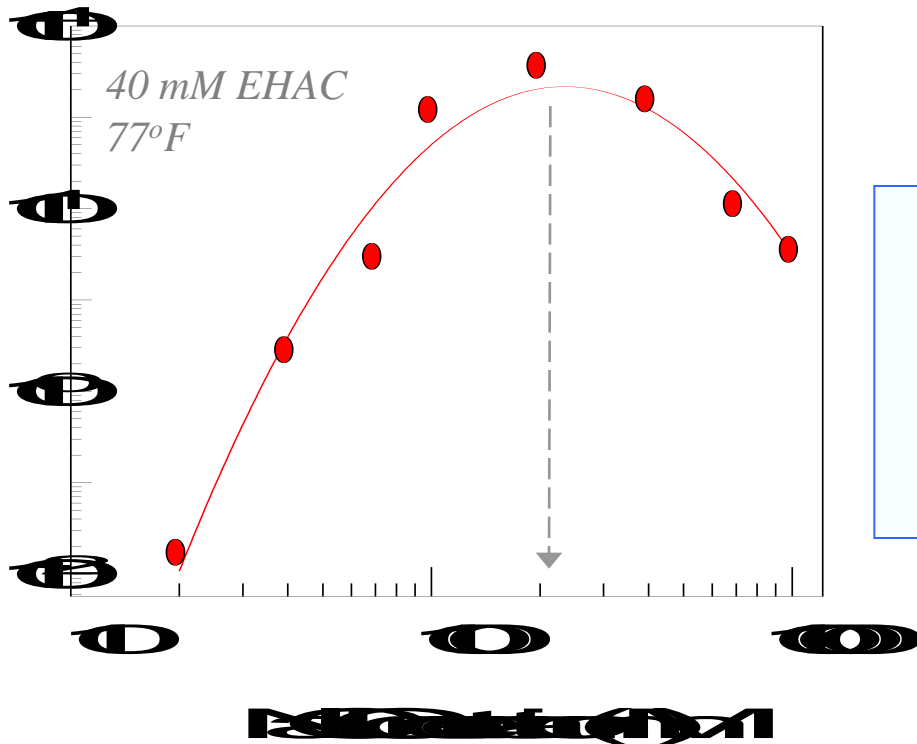
C_{22} - Erucyl



C_{18} - Oleyl



Screening salt: grows wormlike micelles



Spherical to wormlike micelles observed by SANS

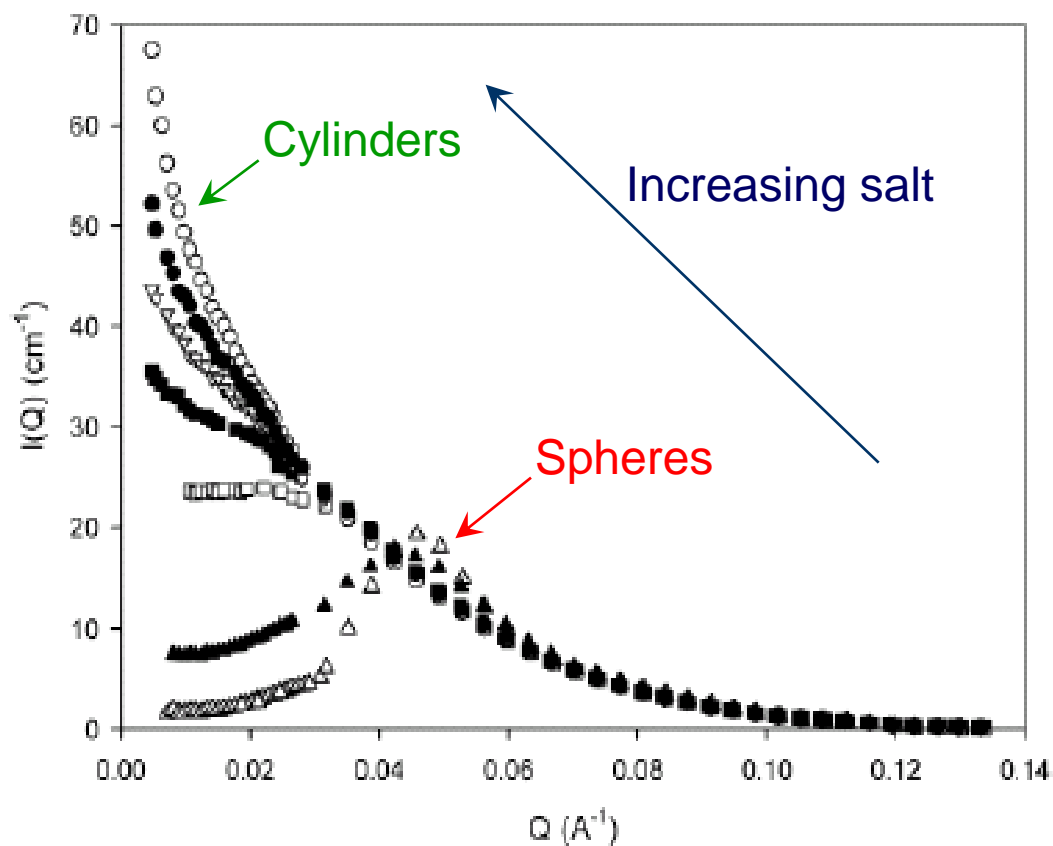
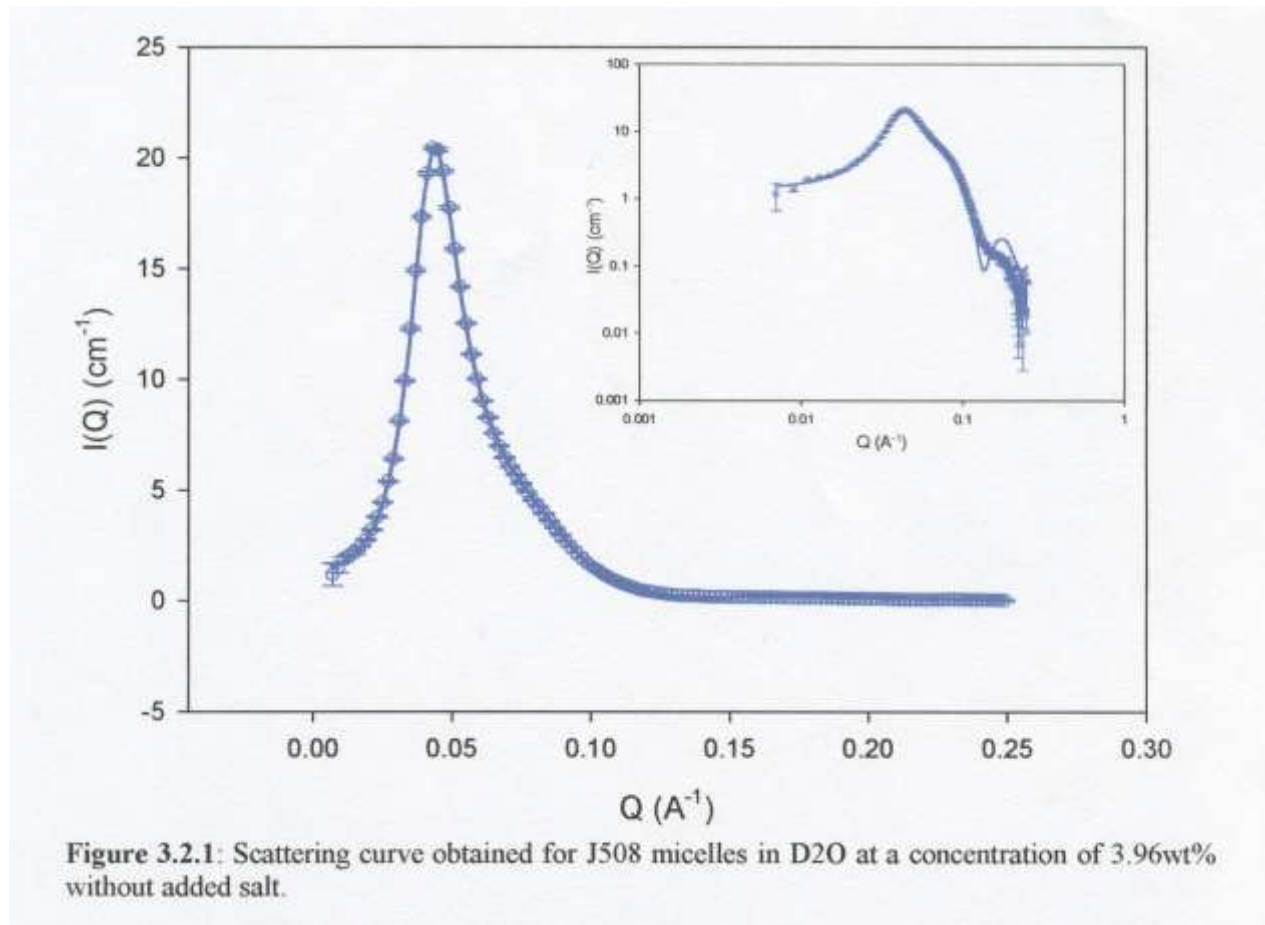


Figure 5. Scattering intensity $I(Q)$ versus scattering vector Q for polymer-like micelles formed by EHAC in D_2O as a function of KCl content at 40 °C. (Δ , no KCl; \blacktriangle , 0.10 wt % KCl; \square , 0.25 wt % KCl; \blacksquare , 0.50 wt % KCl; ∇ , 0.75 wt % KCl; \bullet , 1.0 wt % KCl; \circ , 2.0 wt % KCl.)

V.Croce, T. Cosgrove, G.C. Maitland, T.L. Hughes and G. Karlsson, *Langmuir* **19** 8536-41 (2003)

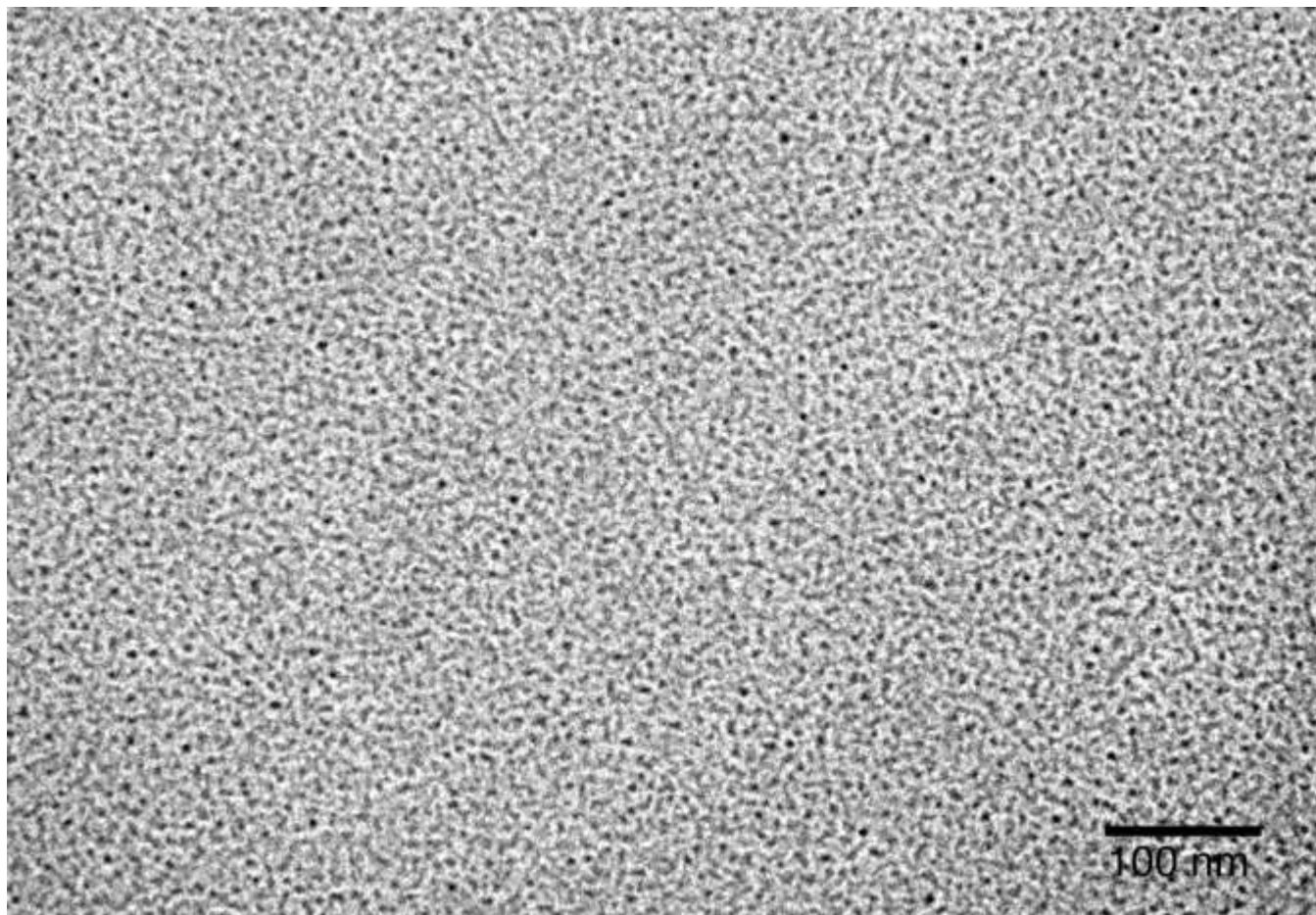
SANS study of micelle growth – no salt



Spherical micelles, $R = 33.3 \text{ \AA}$

Data by Vania Croce, University of Bristol

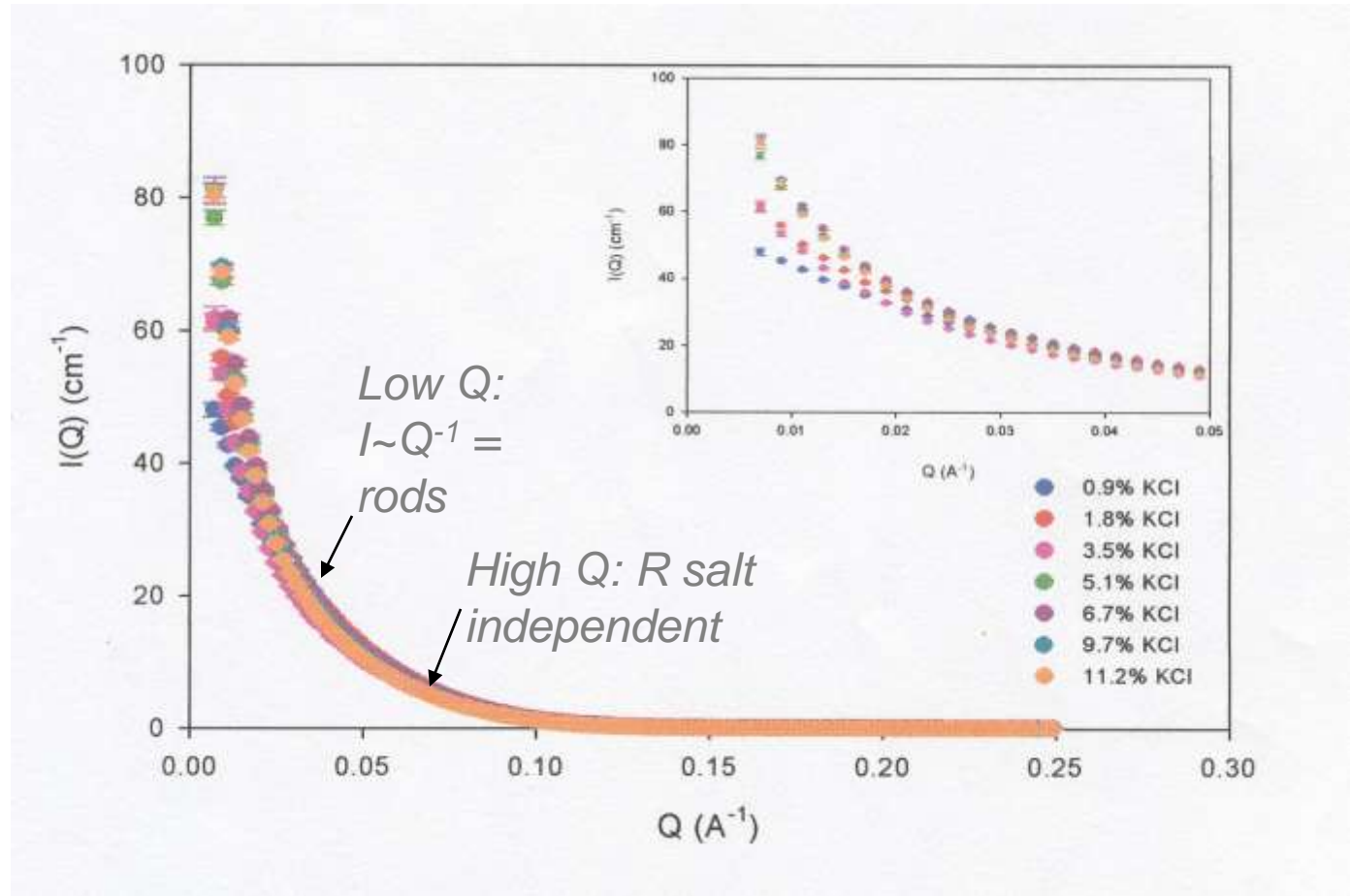
4.5 wt% EHAC...no salt



Spherical Micelles, $R \sim 33\text{\AA}$

*Cryo-TEM by Goran Karlsson, Uppsala University
and Vania Croce, University of Bristol*

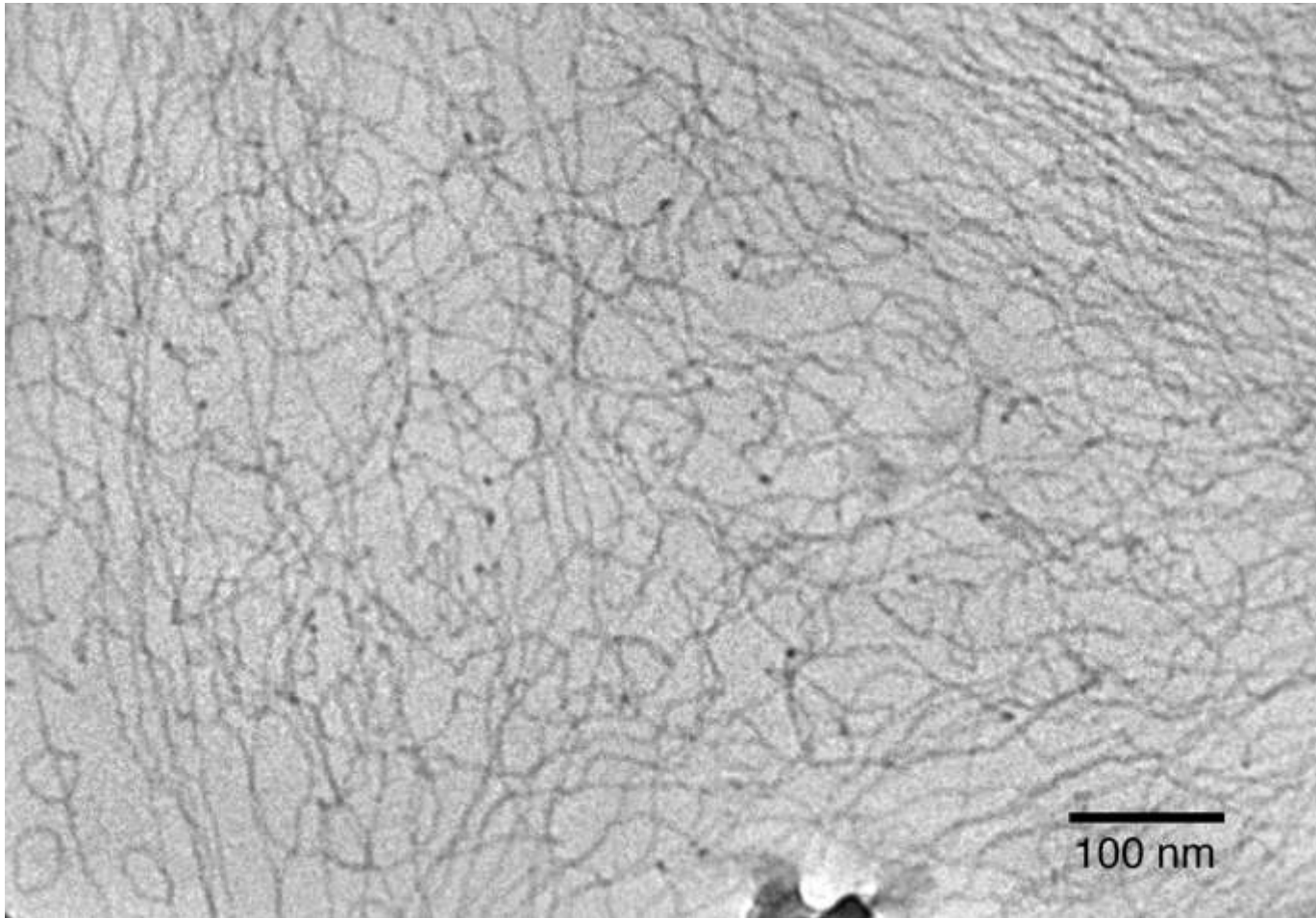
SANS study of micelle growth – added salt



Rodlike micelles, $R = 21 \text{ \AA}$

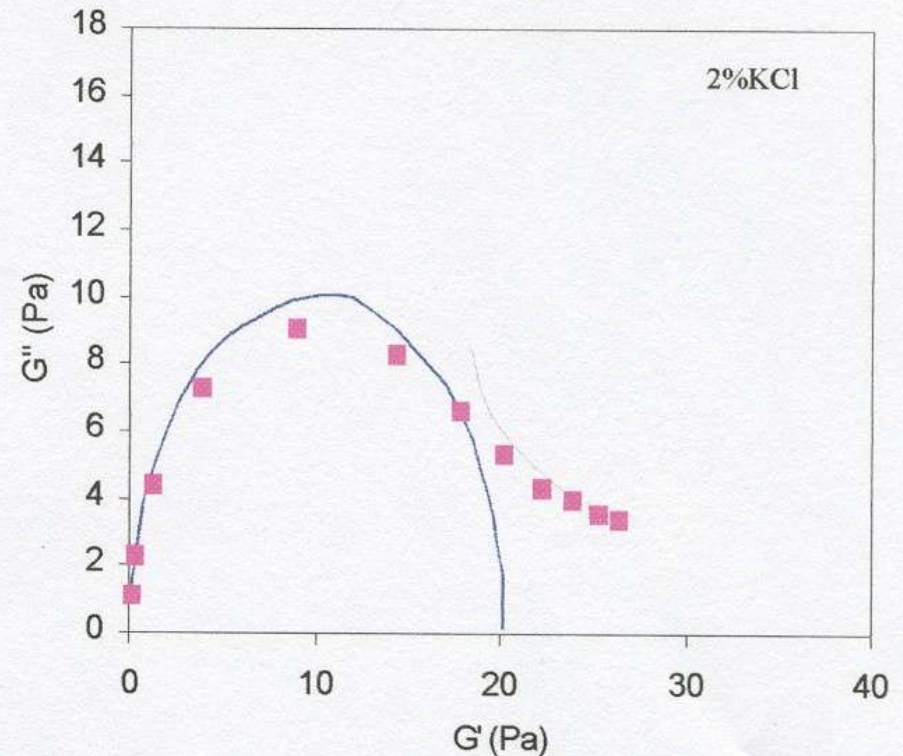
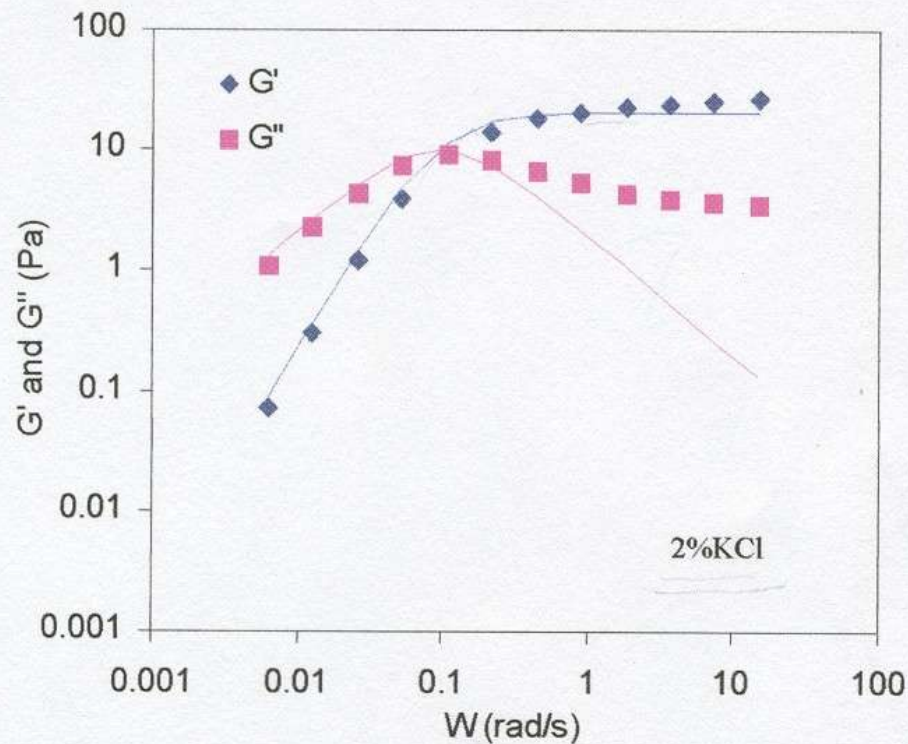
Data by Vania Croce, University of Bristol

Add 2% KCl...peak viscosity



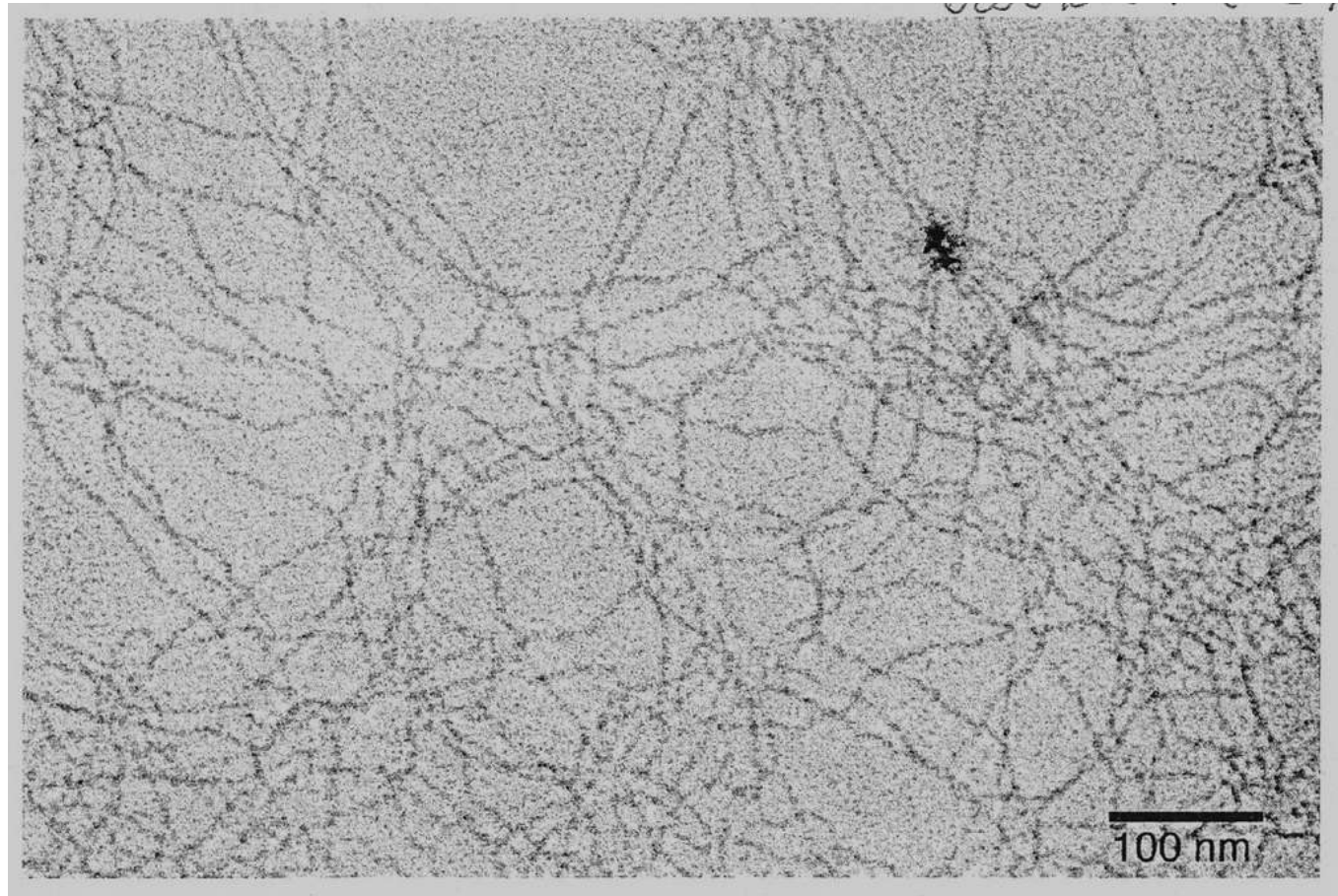
*Entangled Wormlike Micelles
Cryo-TEM by Goran Karlsson, Uppsala University
and Vania Croce, University of Bristol*

Maxwell behaviour...plus Rouse internal modes at high frequency



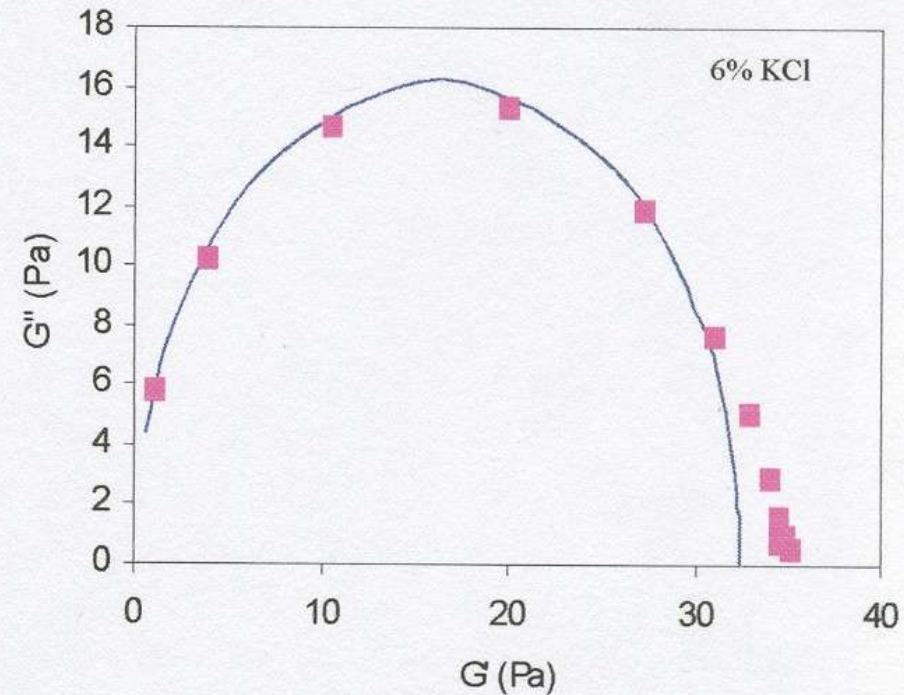
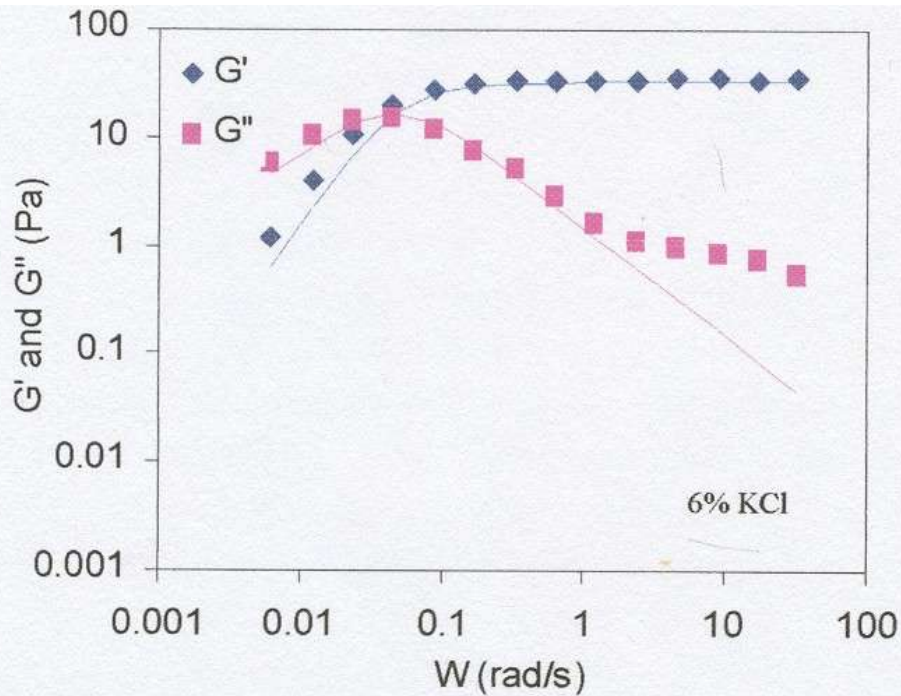
Data: Vania Croce, Univ of Bristol

6% KCl ...viscosity falling... ...branched micelles



Branched Wormlike Micelles
Cryo-TEM by Goran Karlsson, Uppsala University
and Vania Croce, University of Bristol

6% KCl - approaching Maxwell behaviour...



Data: Vania Croce, Univ of Bristol

12% KCl – essentially Maxwell behaviour...

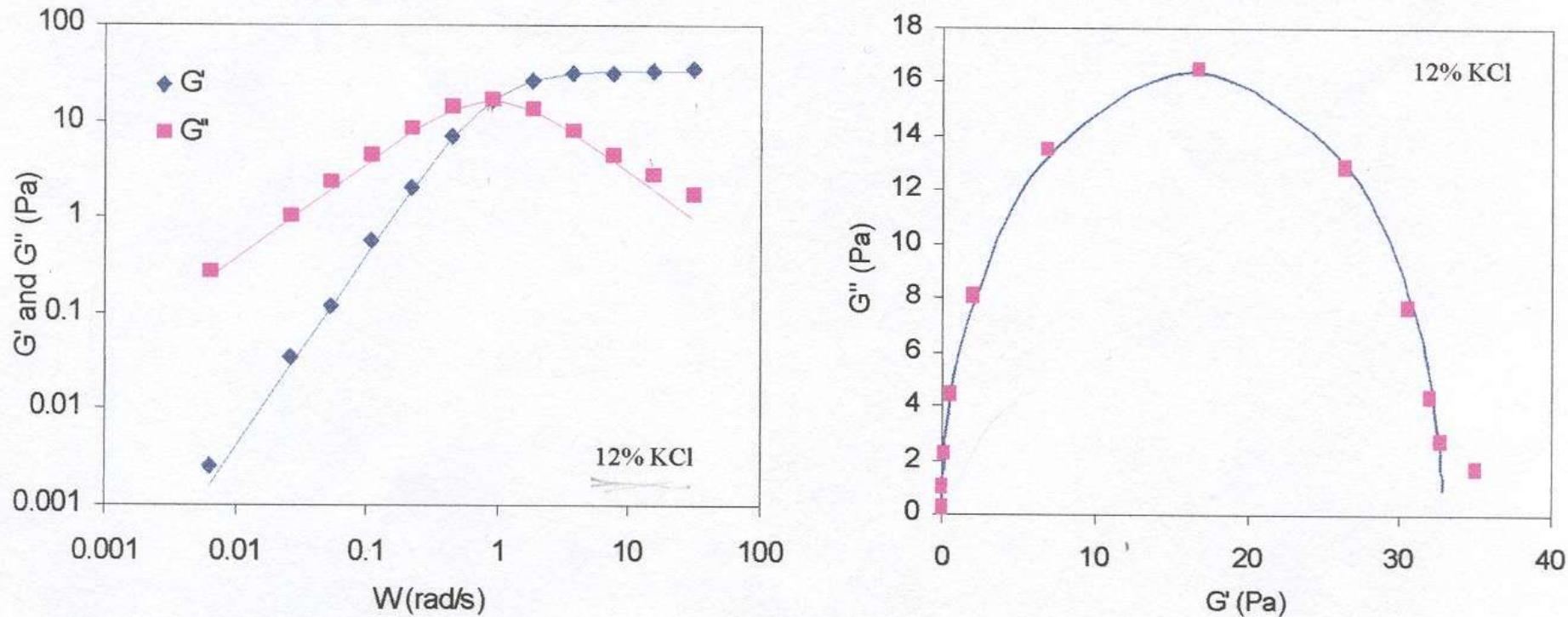
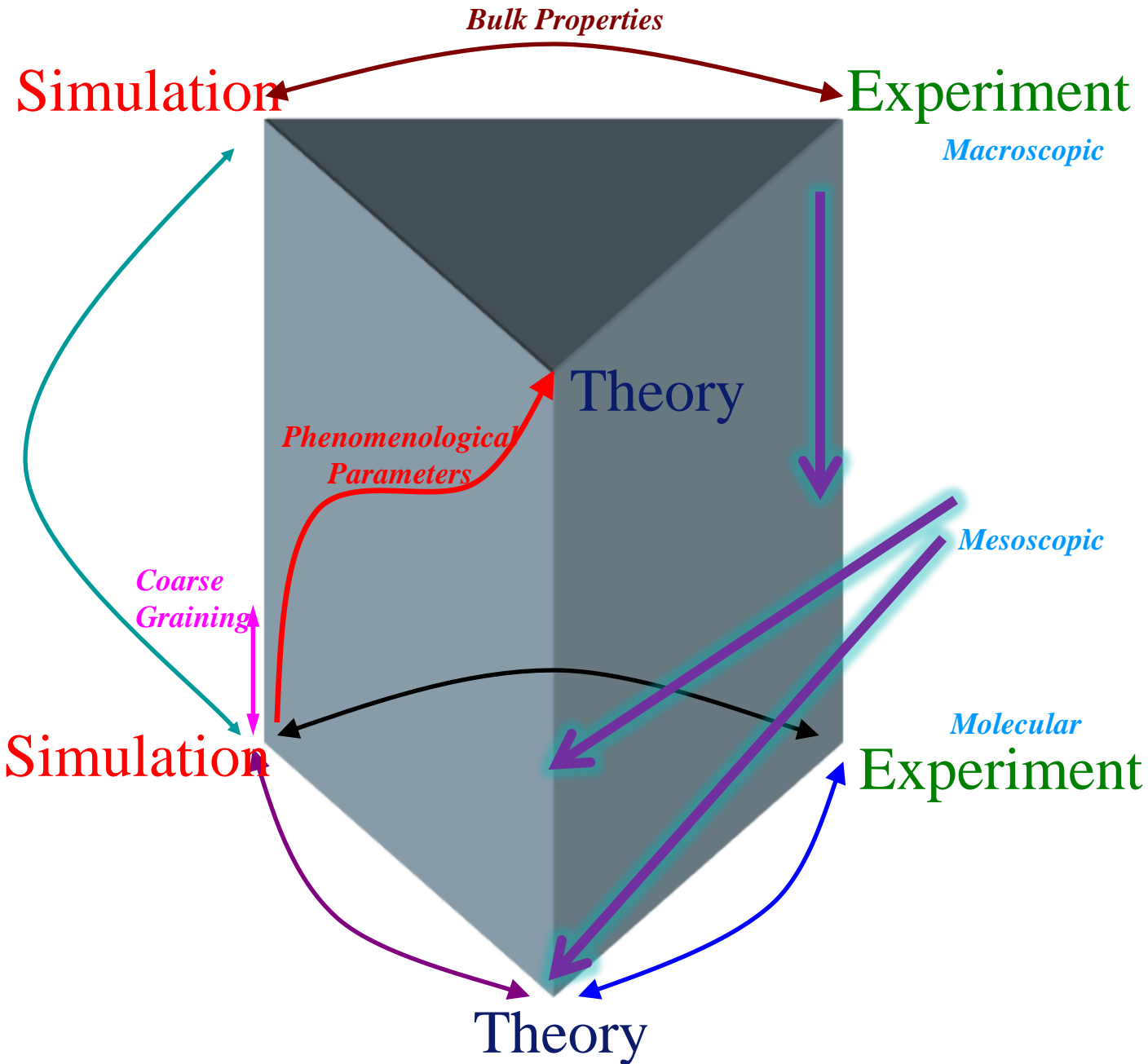


Figure 3.1.9: Evolution of G' and G'' with frequency and the Cole-Cole representation for a solution with 4.5wt % of surfactant concentration with different amounts of salt at 25 °C.

Data: Vania Croce, Univ of Bristol

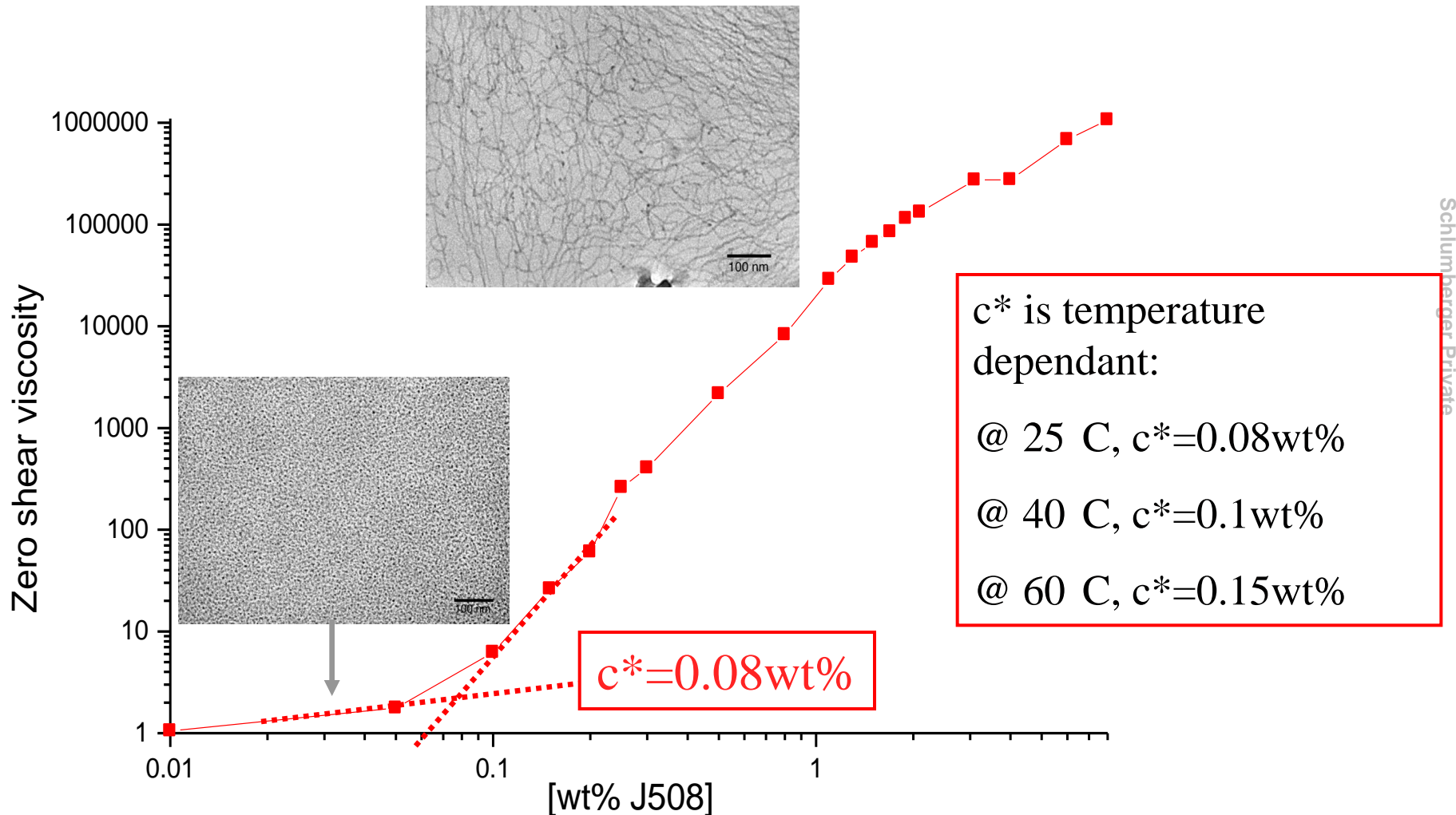
Type of Study



Probing the Microstructure

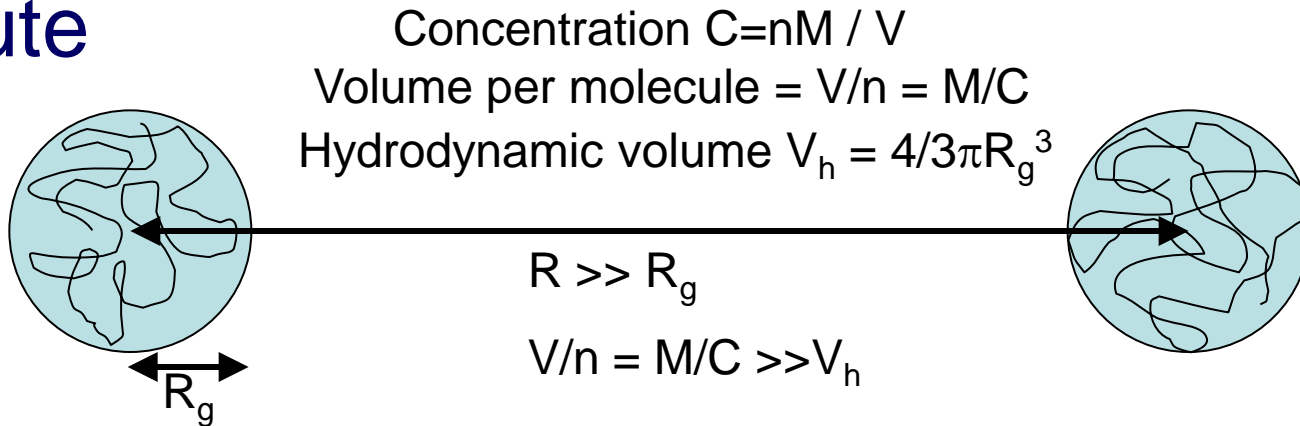
Rheology and Light Scattering

VES – onset of entanglement regime

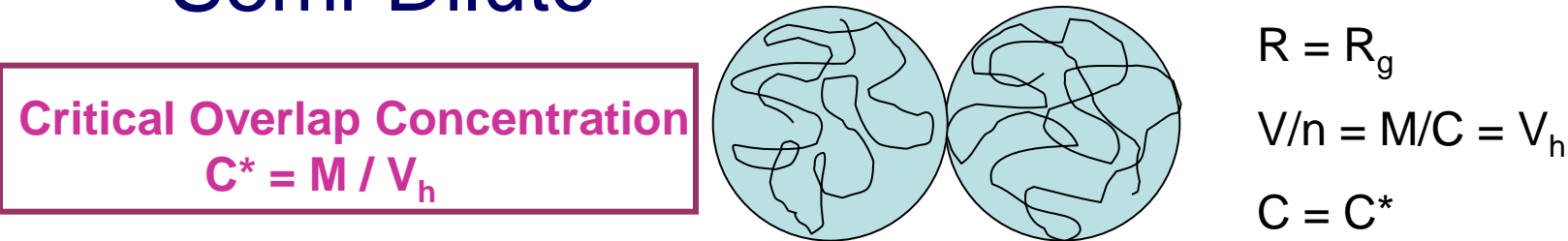


Concentration Regimes

- Dilute



- Semi-Dilute

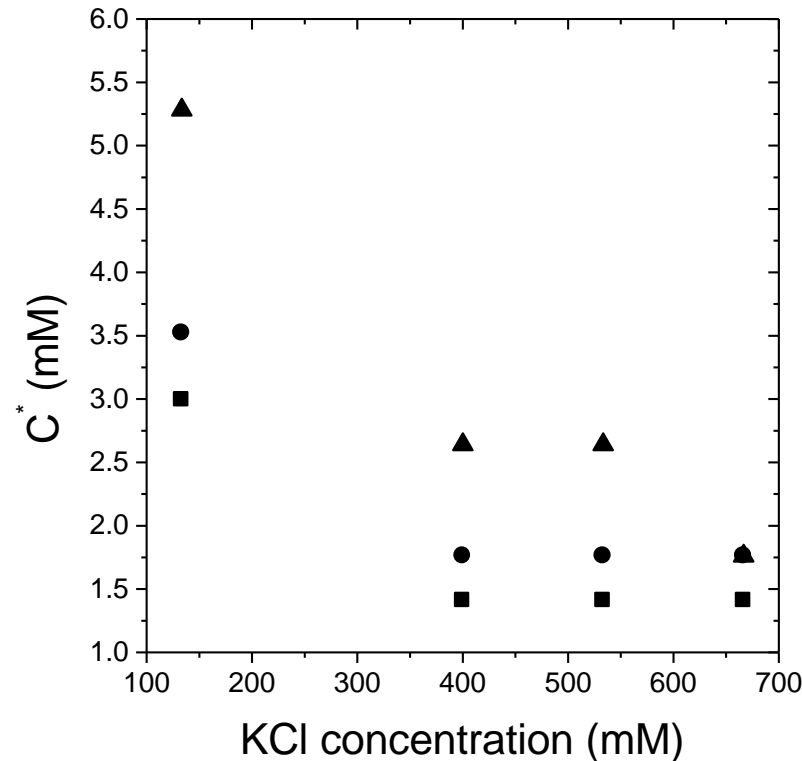


- Concentrated



Critical Overlap Concentration c^* versus Temperature, Salt

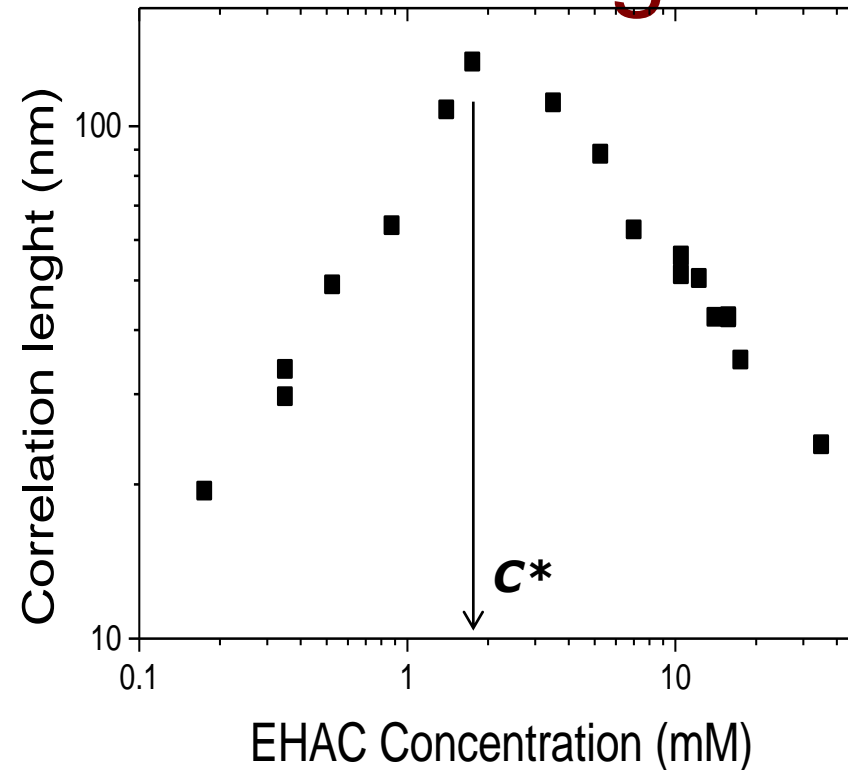
Note: IPA solvent reduces c^ by about 30%*



*Data:
Isabelle Couillet*

Crossover concentration C^ of EHAC solutions versus KCl concentration at 25°C (), 40°C () and 50°C ().*

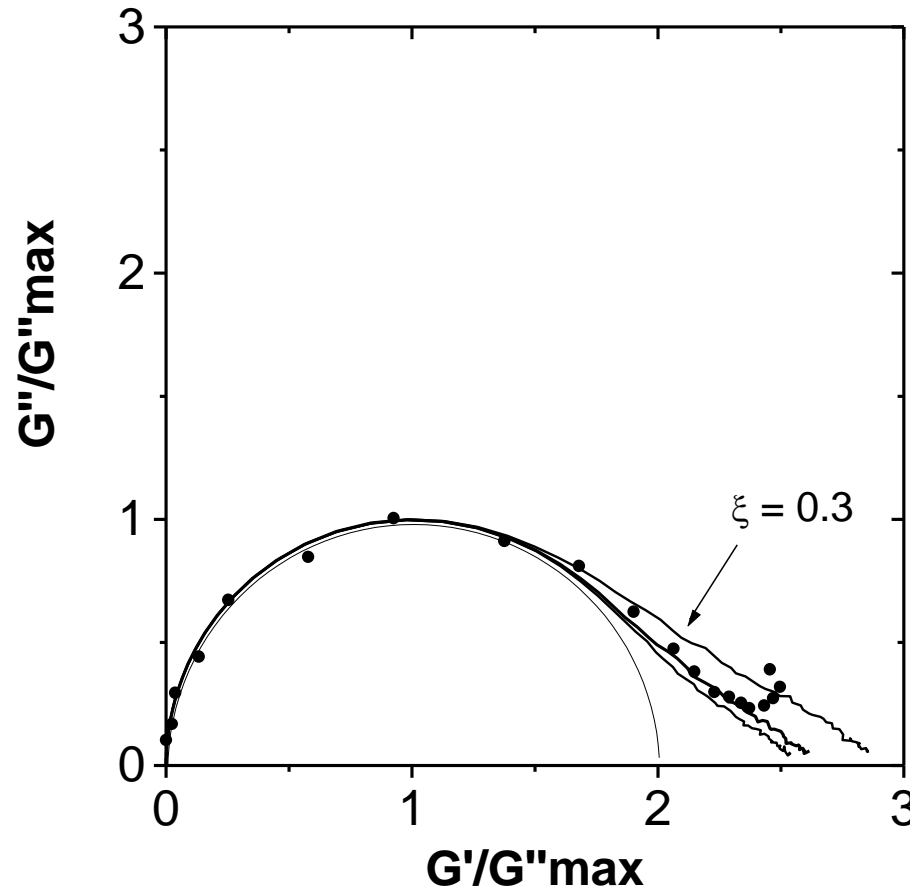
Correlation length from static light scattering



*Variation of the correlation length ξ versus active EHAC concentration
With 400mM KCl at 25°C.*

Correlation Length ξ from Ornstein-Zernicke Equation: $I(q)^{-1} = I(0)^{-1}[1 + q^2\xi^2]$

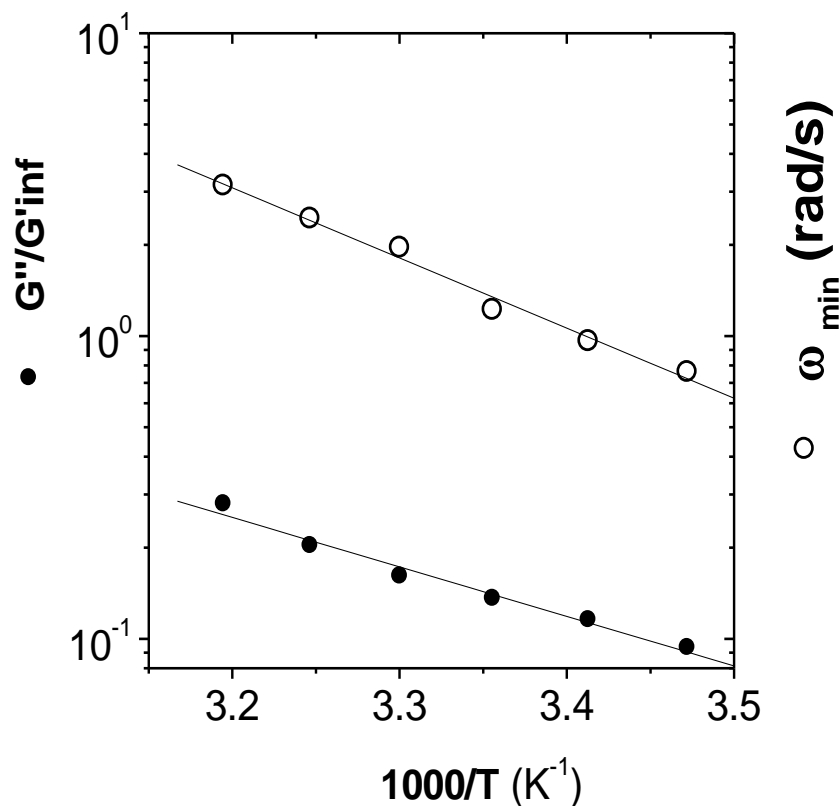
Estimation of $\zeta = \tau_{\text{break}}/\tau_R$



*Data:
Isabelle Couillet*

Normalized Cole-Cole plot for a solution of EHAC at an active concentration 14.4 mM with $T=15^\circ\text{C}$, $[\text{KCl}]=400\text{mM}$. The dotted lines are the calculated Cole-Cole plots for different values of the parameter ζ (0.1, 0.13 and 0.3).

Direct Determination of E_{sciss}



$$G''_{min}/G'_{inf} \sim I_e / \langle L \rangle$$

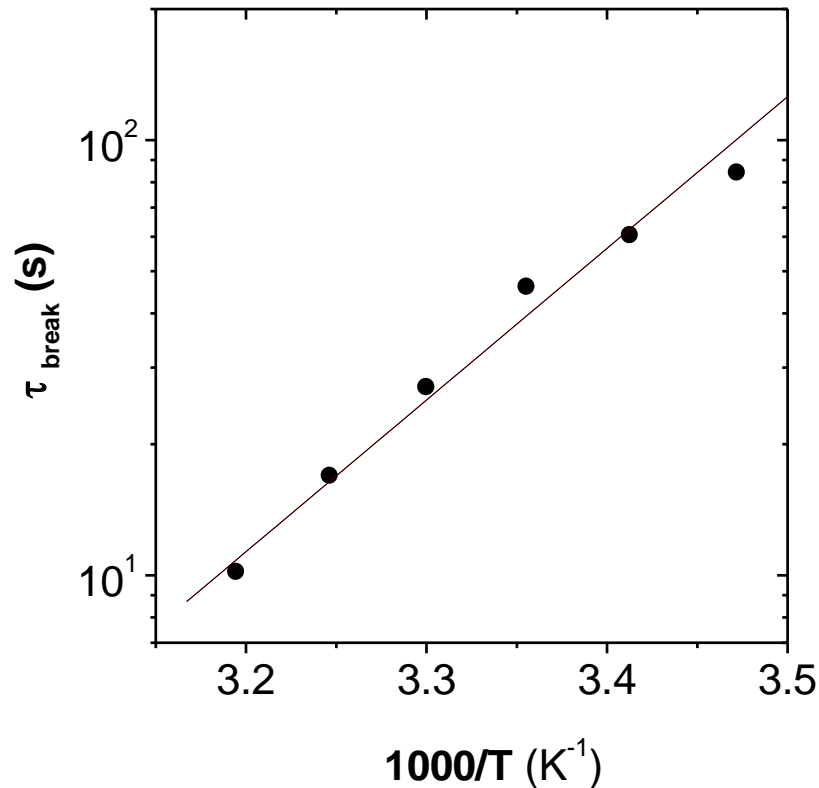
$$\sim \exp[-E_{sciss}/2kT]$$

$$E_{sciss} = 28kT$$

Semi-log variation of G''_{min}/G'_{inf} (•) and ω_m (○) as a function of $10^3/T$ for a solution with an active EHAC concentration of 14.1 mM, and 400 mM KCl

Data: Isabelle Couillet

Activation Energy for Micelle Breaking



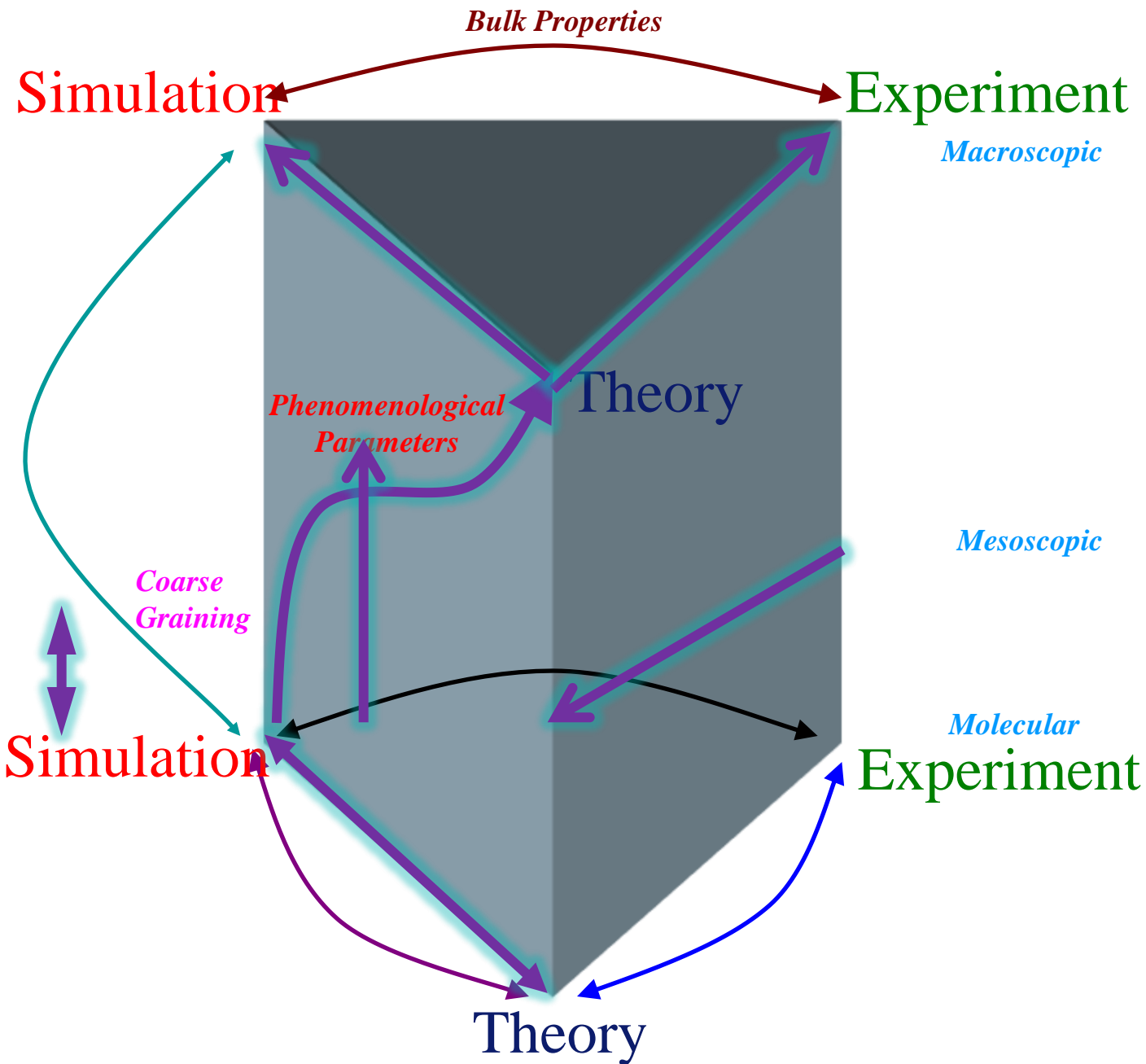
$$E_{\text{break}} = 25.5kT$$

$$\begin{aligned} E_R &= 0.5(E_{\text{break}} + E_{\text{rep}}) \\ &= 0.5(E_{\text{break}} + 1.5 E_{\text{sciss}}) \\ &= 34kT \end{aligned}$$

$$E_{\text{sciss}} = 28kT$$

Arrhenius plot of the breaking time τ_{break} versus $10^3/T$ for active EHAC concentration of 14.1 mM and 400 mM KCl

Type of Study



Simulation: from Micro to Meso to Macro

1. Micro-scale

- Atomistic Molecular Dynamics simulation of micelles
- Coarse-grained micelle MD
- Output: persistence length, compressibility, scission/end cap/branching energies, ...

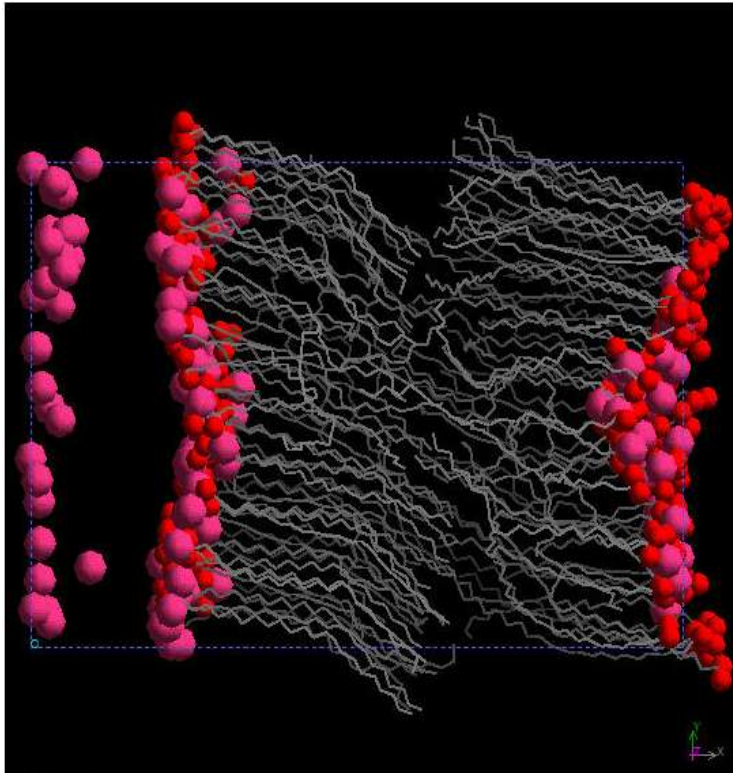
2. Mesoscopic simulation of wormlike micellar VES fluids

- Coarse-grained micelle MD
- Output: rheology of bulk VES fluid

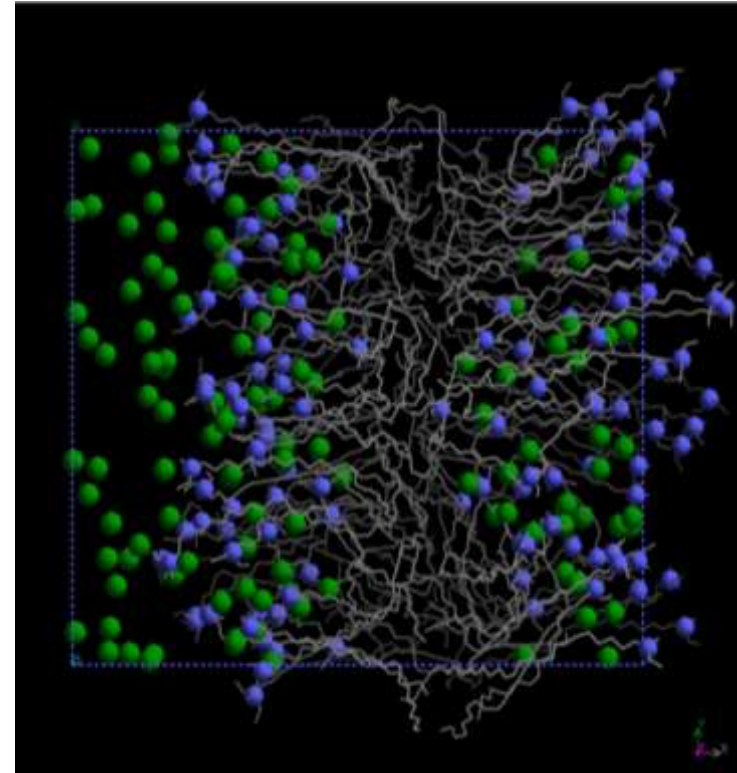
3. Macro-scale: fluid dynamics

- flow in porous media: leak-off and clean up of frac fluid
- particle laden flow: proppant transport, shear banding,...

MD simulation of surfactant packing



Erucate (ordered)



EHAC (less ordered)

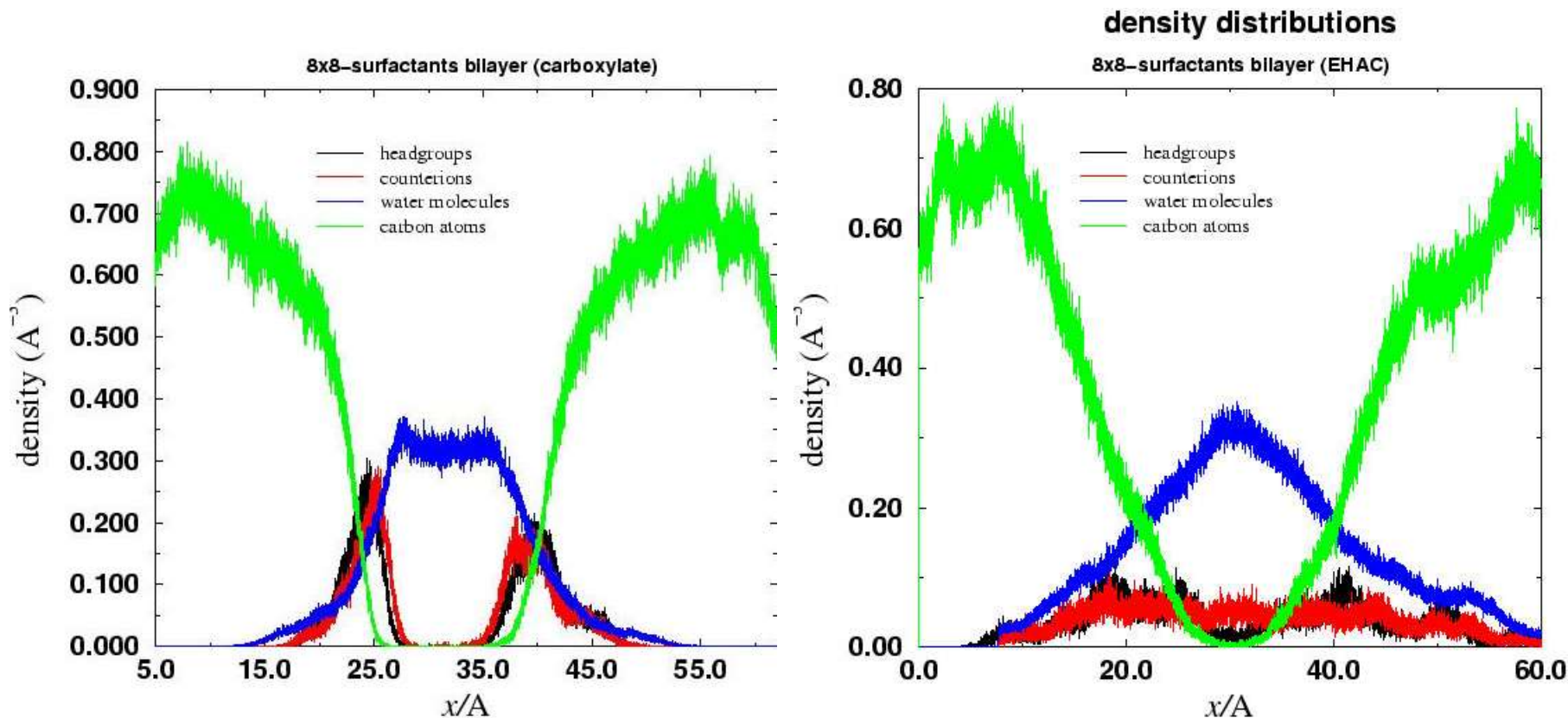
Same tail, different heads: different packing behaviour

Erucate

EHAC

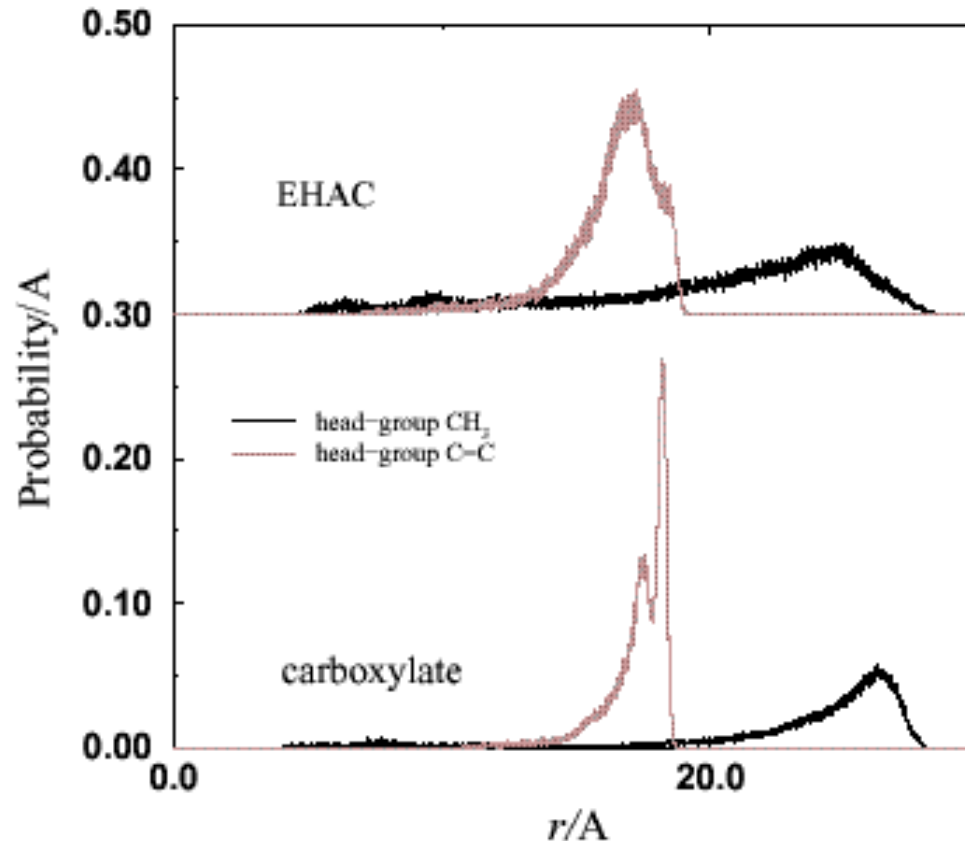
$$0.93 \quad \langle \sum_{i,j} \mathbf{s}_i \cdot \mathbf{s}_j \rangle / N^2 \quad 0.62$$

Density distributions



Penetration of water into membrane core
- similar to cylindrical micelles
(Watanabe & Klein, 1991)

Intra-chain separations



*Peaks at large r are due to fully extended chains –
at smaller distances show tendency to “fold back”*

*Sharper $\text{C}=\text{C}$ peaks show that first part of chain is less flexible*⁶³

Control of Fluid Properties through Design of Chemical Structure

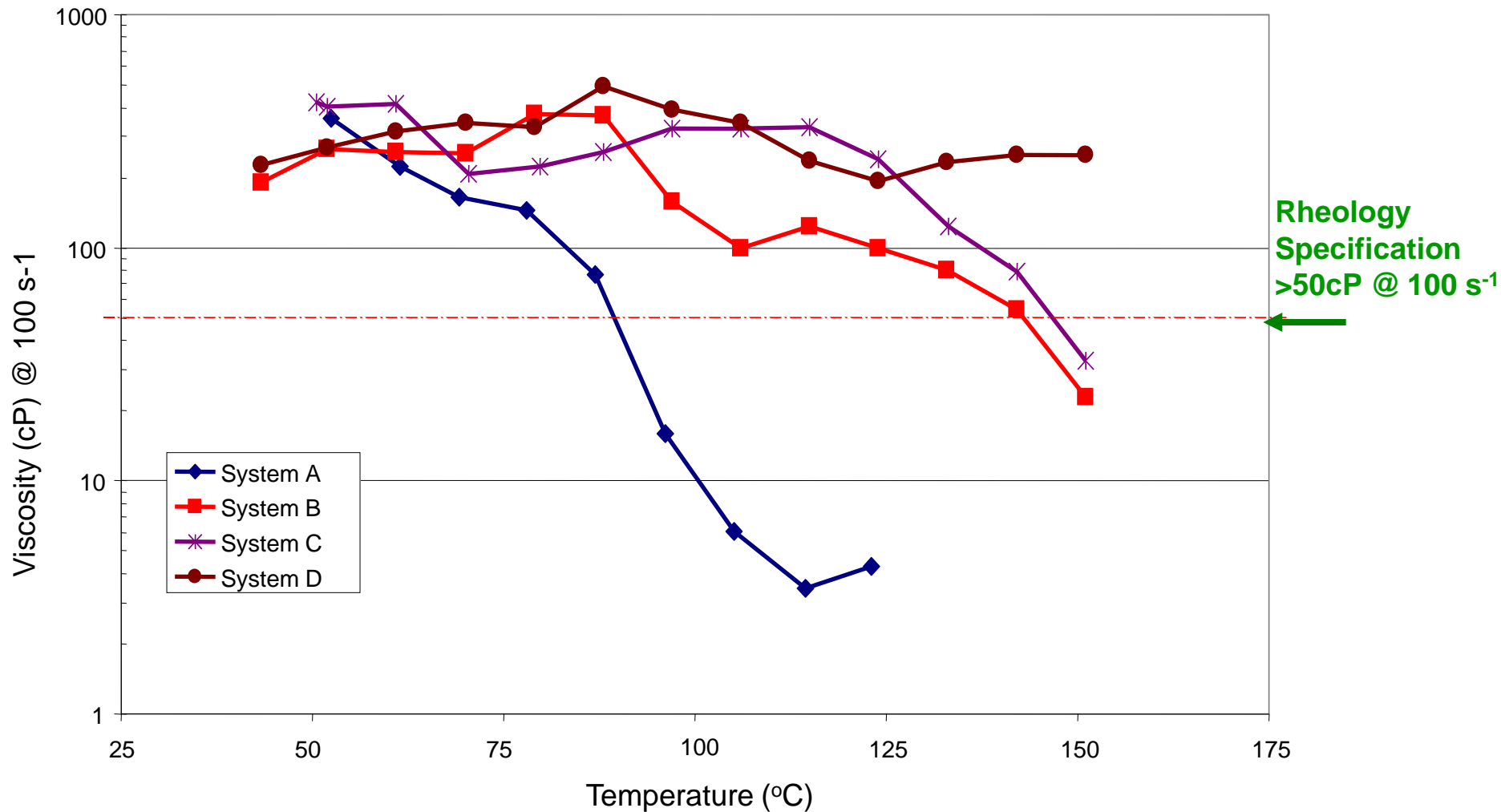
Moving from Formulation towards
Molecular Engineering

Alternative VES Structures



Tune headgroup and tail interactions to increase packing parameter, $P = V_s / la$, and so stabilise wormlike phase to higher temperatures

Improving Temperature Performance



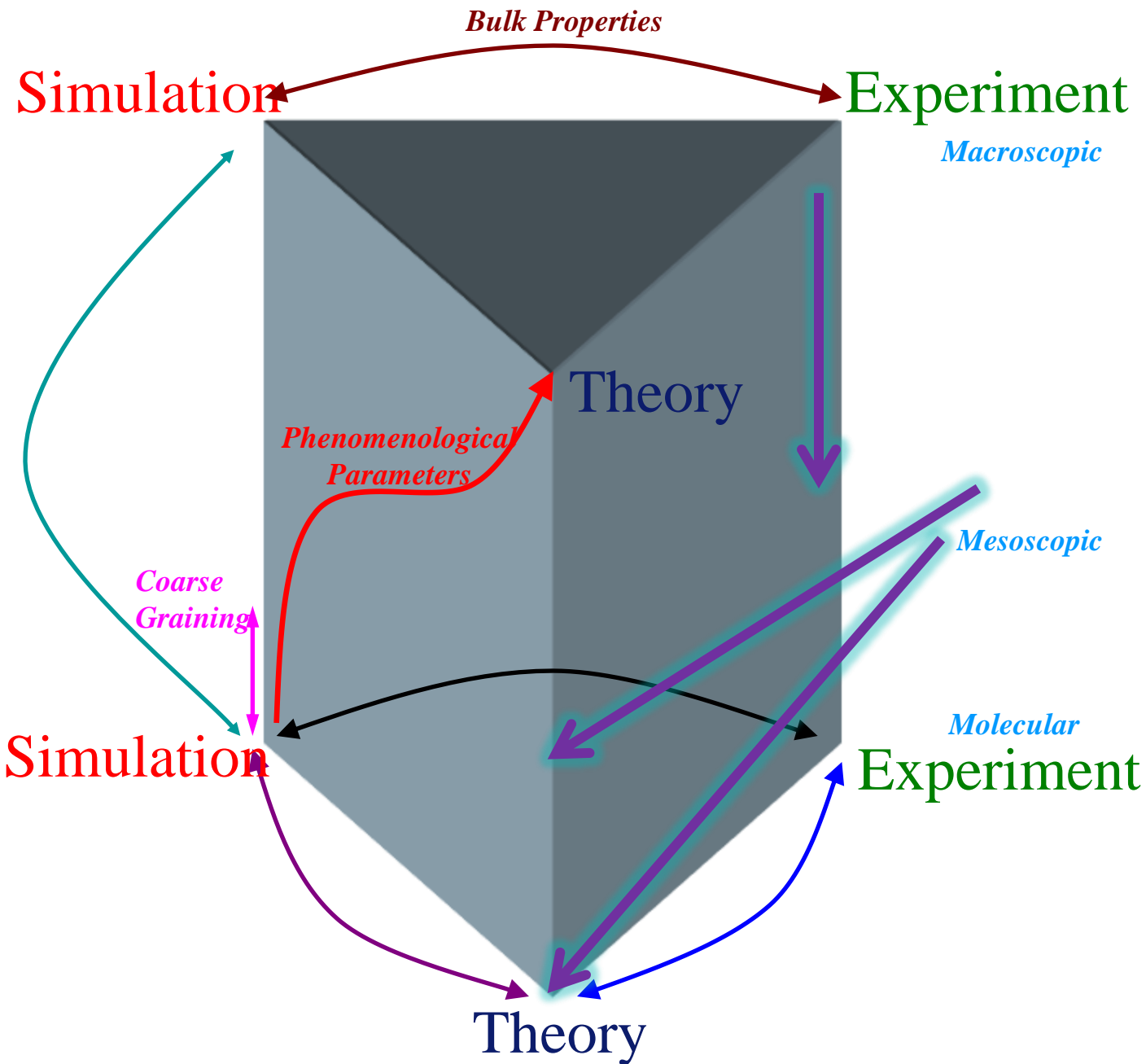
Data: T L Hughes et al, Schlumberger

The major block for using new molecules in the oilfield:

££££££££££££££££

Must leverage on other non-oilfield applications

Type of Study



Tuning Properties by Blends

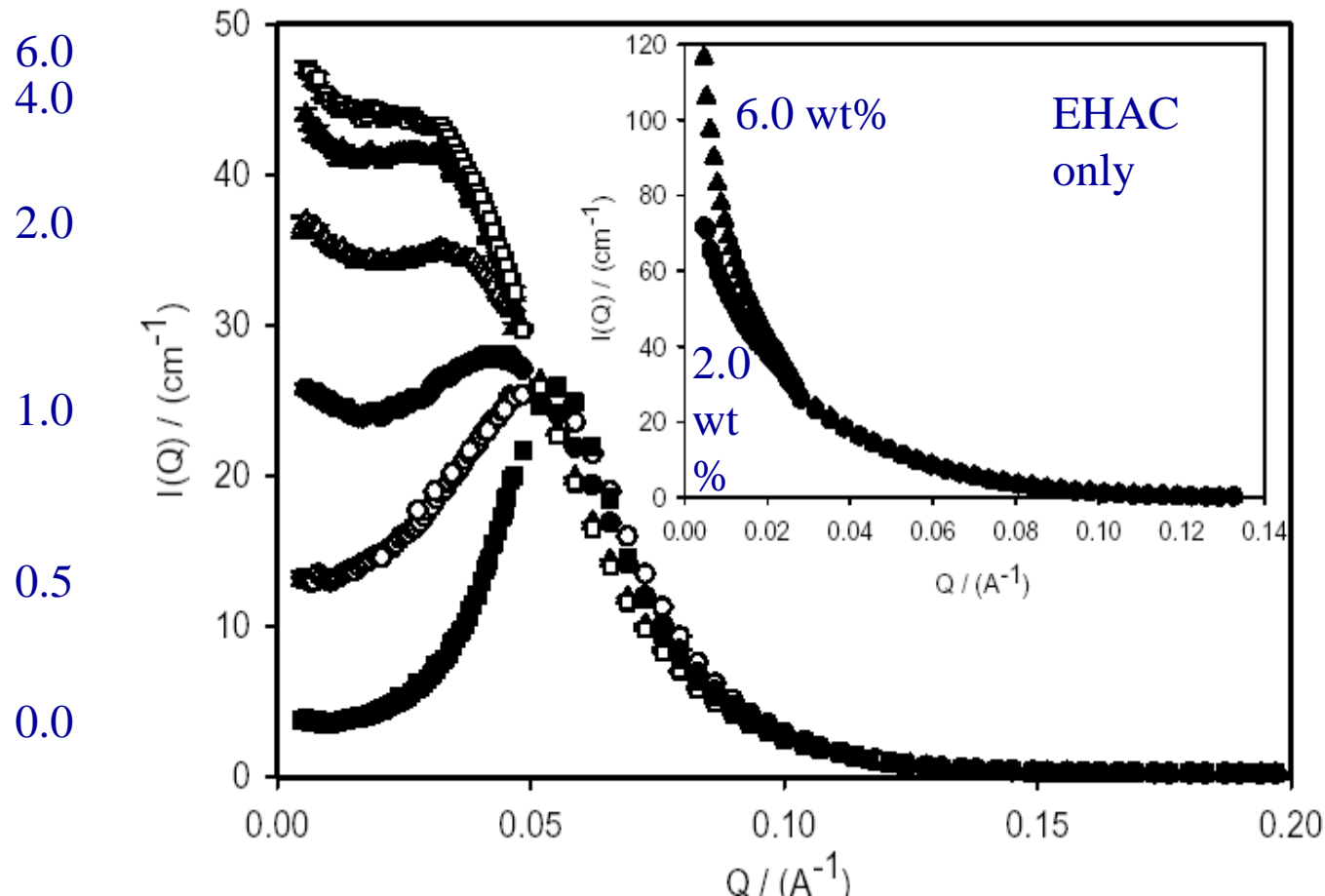
(a) Surfactant Blends

SANS for EHAC-C₁₈E₁₈ mixed micelles vs [salt]

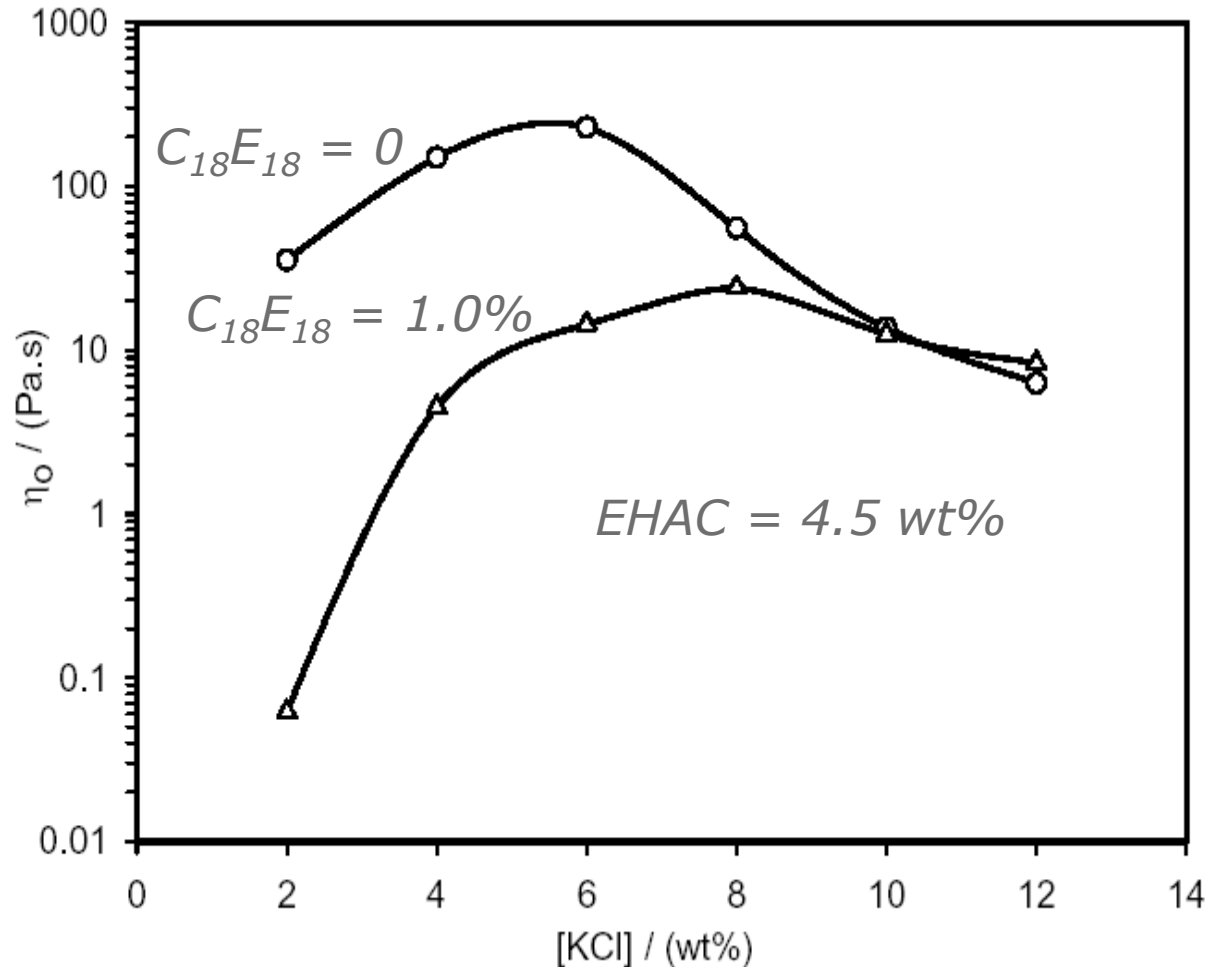
[KCl] wt%

25C

4.5wt% EHAC,
4.0wt% C₁₈E₁₈



Low shear viscosity for EHAC- $C_{18}E_{18}$ mixed micelles



*V Croce, T Cosgrove, C Dreiss, G Maitland, T Hughes and G Karlsson,
Langmuir, **20**, 7984-7990, 2004*

Microstructure associated with rheology changes in mixed worm-micelle fluids

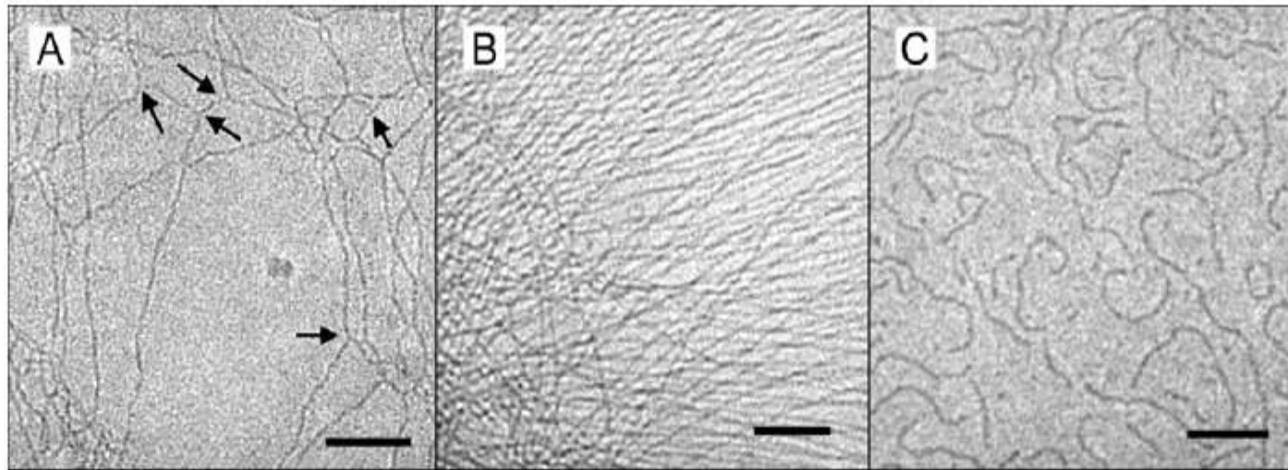


Figure 10. Cryo-TEM images with samples containing 4.5 wt% EHAC with 6.0 wt% KCl varying concentration of $C_{18}E_{18}$. (A: No $C_{18}E_{18}$, B: 1.0wt% $C_{18}E_{18}$ and C: 4.0 wt% $C_{18}E_{18}$). Bar = 100 nm

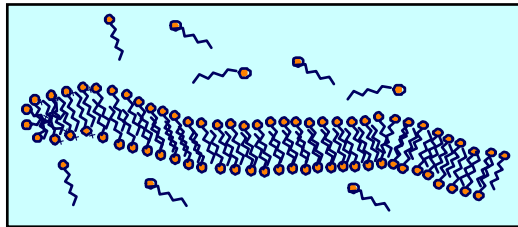
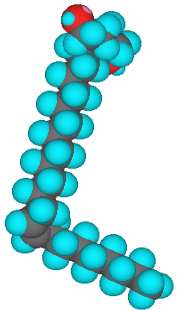
V Croce, T Cosgrove, C Dreiss, G Maitland, T Hughes and G Karlsson, Langmuir, 20, 7984-7990, 2004

Tuning Properties by Blends

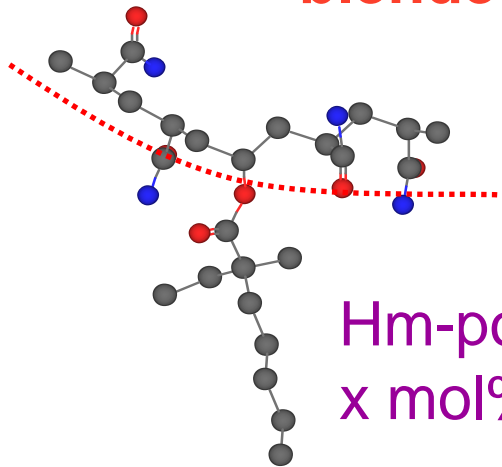
(b) Polymer-Surfactant Blends

Polymer-surfactant mixtures

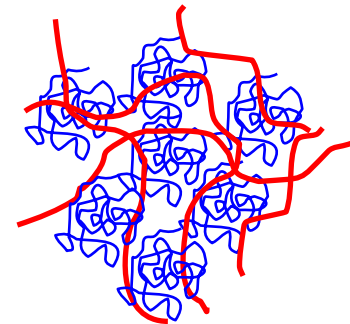
Visco-elastic surfactant (VES) - EHAC



blended with



Hm-polymer
x mol% hydrophobe



- VES/hm-polymer blend
 - visco-elastic physical gel
 - selective response to oil
 - lower concentrations of both polymer and surfactant

Hm-Polymer:Surfactant Mixtures - Enhanced linear viscoelasticity

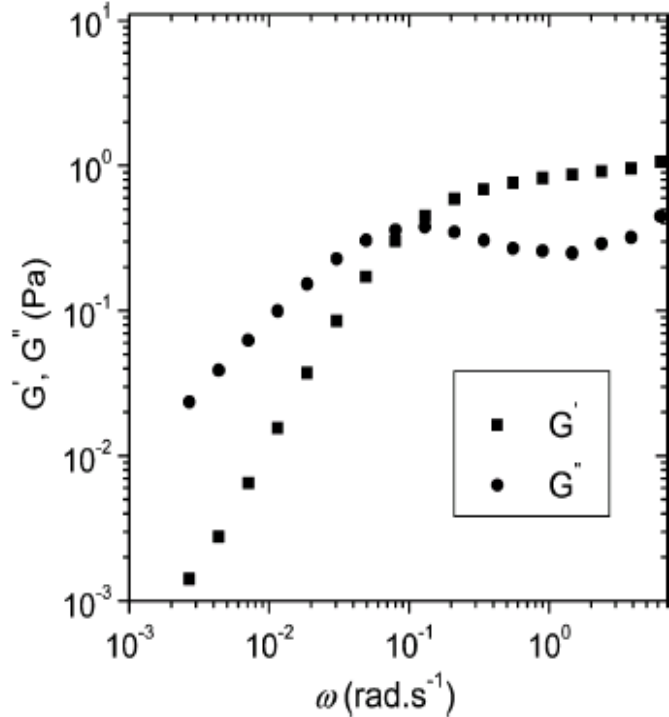


Figure 5. Storage (G') and loss (G'') moduli as a function frequency at 25 °C for a solution of 0.2 wt % hm-HPG, 0.15 % EHAC, and 3 wt % KCl ($R = 0.43$).

*Hm-HPG: $M_w \sim 1.8 \times 10^6$,
 $\langle DP \rangle \sim 3000$,
 C_{22} side groups 10 per chain*

$$R = [C_{EHAC}] / [C_{EHAC} + C_{HmHPG}]$$

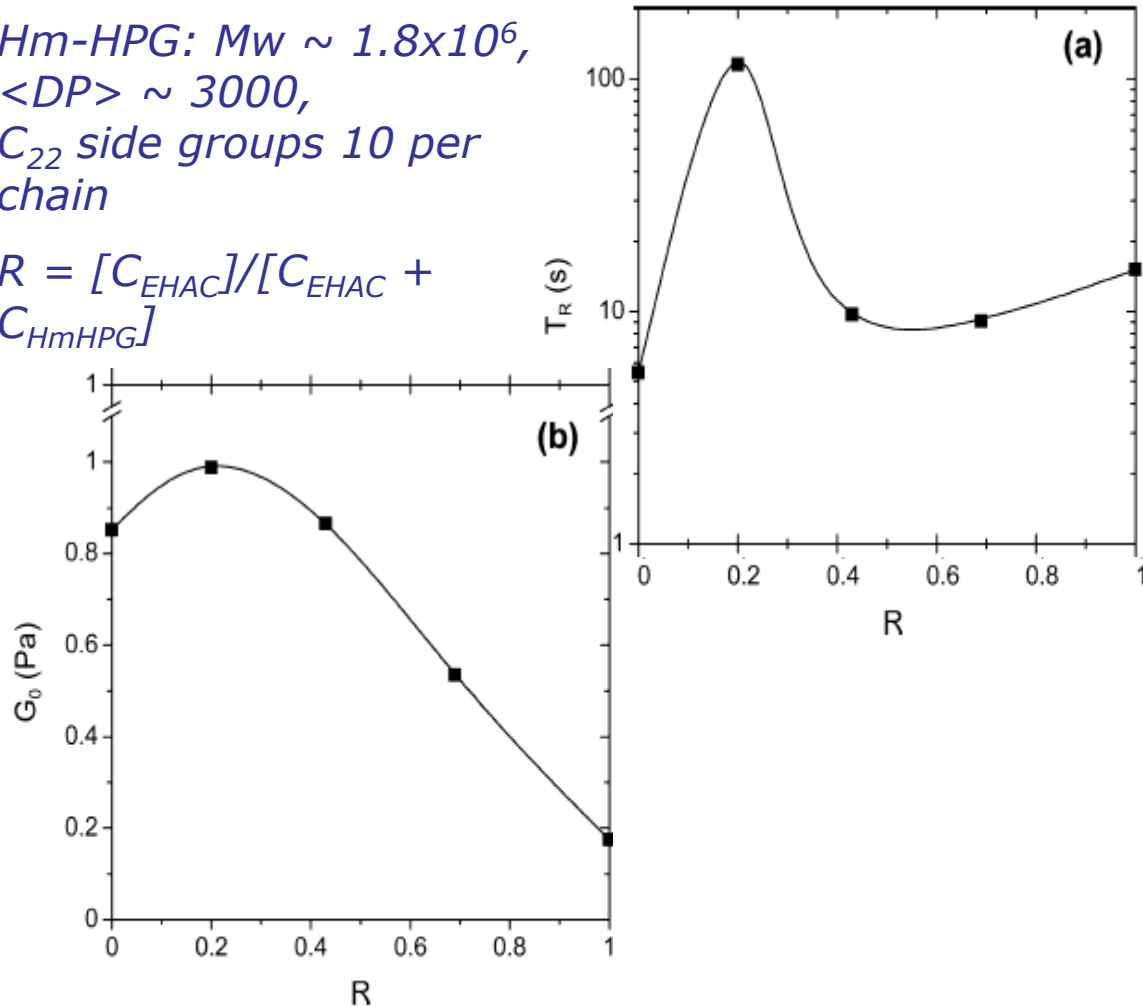


Figure 6. Terminal relaxation time (T_R , a) and pla modulus (G_0 , b) vs R for systems with an overall concentr: $C_M \approx 0.35$ wt %.

*I Couillet, T Hughes, G Maitland and F Candau, Macromolecules, **38**, 5271-5282, 2005*

Hm-HPG:EHAC mixtures – shear viscosity enhancement

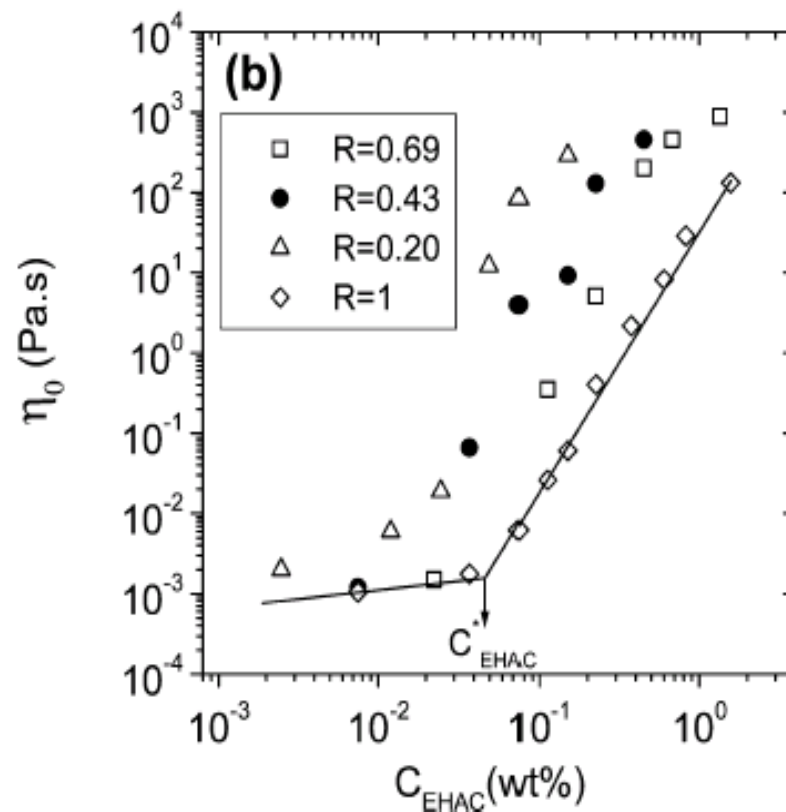
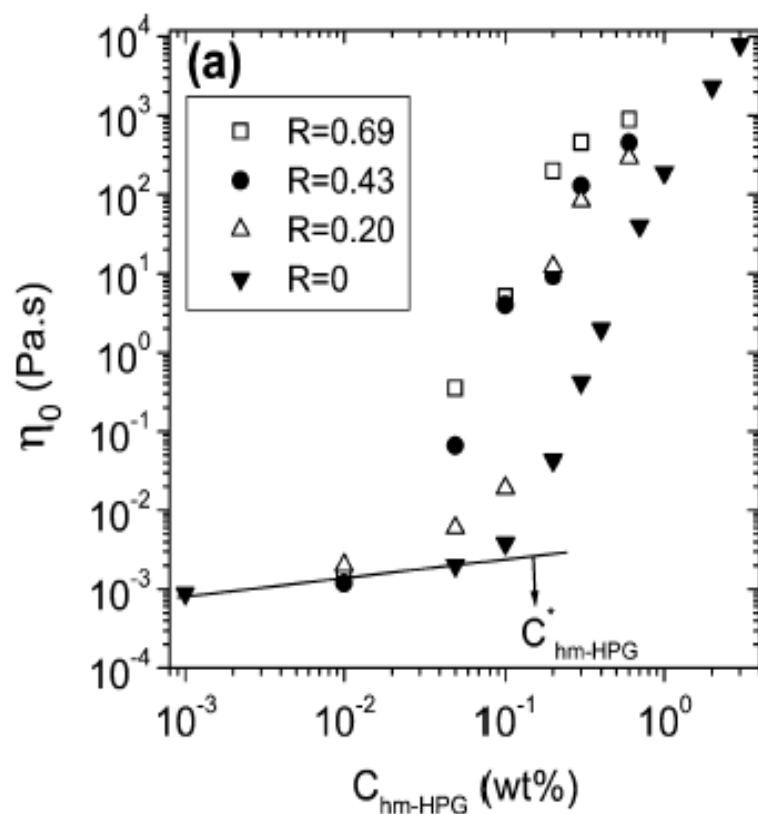


Figure 7. Zero-shear viscosity vs hm-HPG (a) and EHAC (b) concentrations for various compositions of the mixtures at 25 °C. Also are reported the variations corresponding to the single hm-HPG and EHAC components, respectively.

I. Couillet, T.L. Hughes, G.C. Maitland, F. Candau
 Macromolecules, **38**, 5271-5282 (2005)

Hm-HPG:EHAC mixtures – shear viscosity

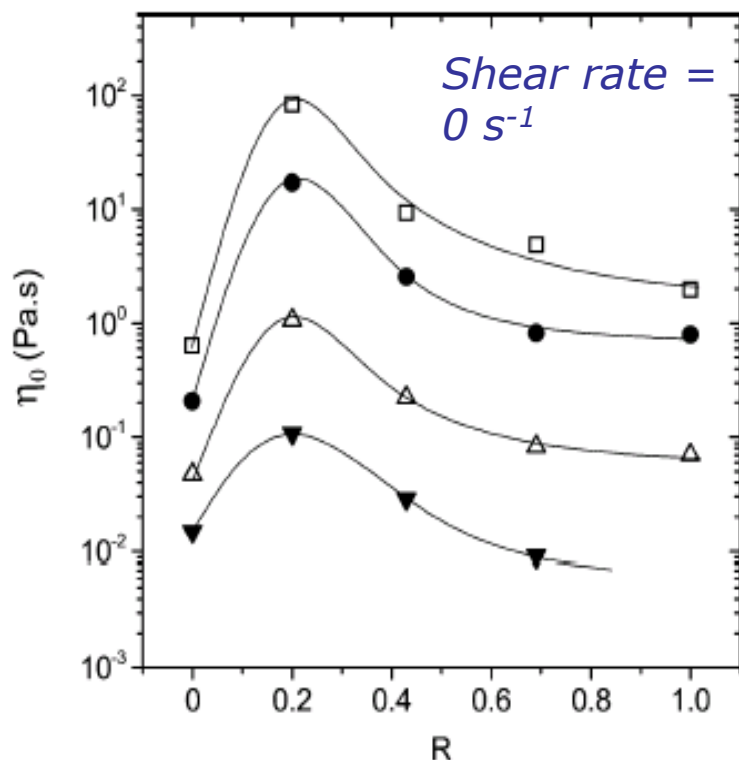


Figure 9. Zero-shear viscosity vs R at various temperatures: (□) 25 °C; (●) 40 °C; (Δ) 60 °C; (▼) 80 °C. Data are for systems with $C_M \approx 0.35$ wt %. The lines drawn through the data are guides for the eye.

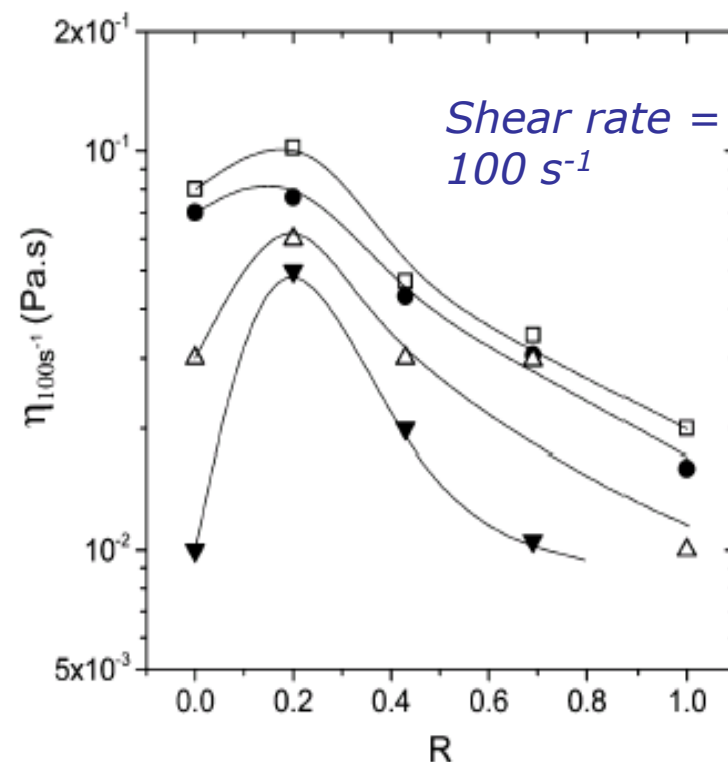
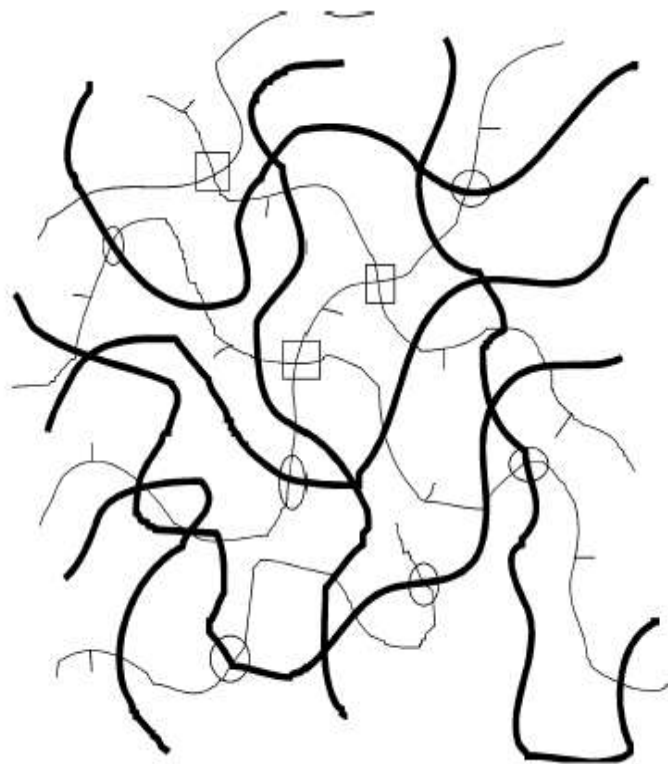


Figure 11. High shear rate viscosity vs R at various temperatures: (□) 25 °C; (●) 40 °C; (Δ) 60 °C; (▼) 80 °C. Data are for systems with $C_M \approx 0.35$ wt %. The lines drawn through the data are guides for the eye.

Hm-HPG: $M_w \sim 1.8 \times 10^6$, $\langle DP \rangle \sim 3000$, C_{22} side groups
10 per chain
 $R = [C_{EHAC}] / [C_{EHAC} + C_{HmHPG}]$

Interpenetrating network of wormlike micelles and hm chains of hm-HPG



Polymer chain



Wormlike micelle



Hydrophobic sequence

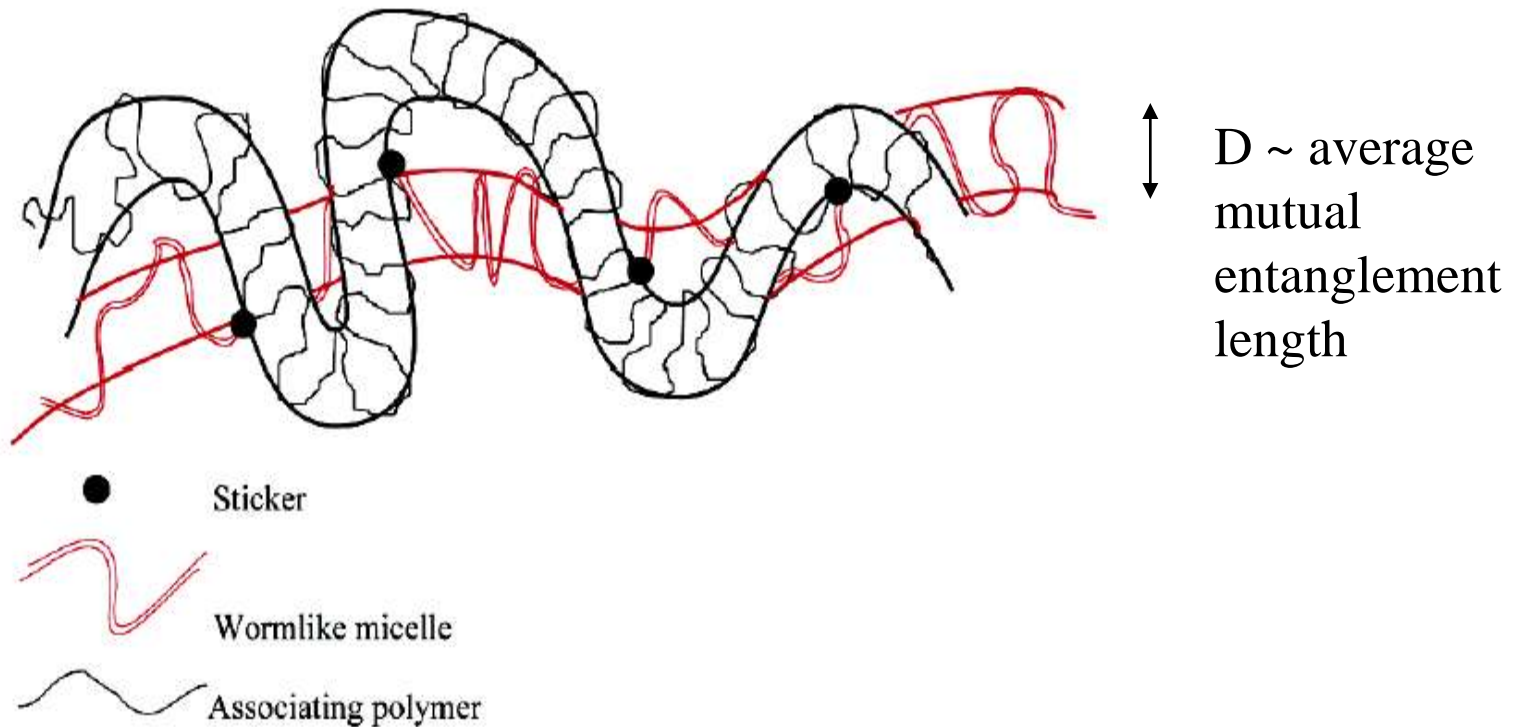


Binary crosslink



Hydrophobic sequence embedded
in a wormlike micelle

Sticky Reptation Model for hm-polymer:wormlike micelle coupling



Needs quantitative model for worm-hm polymer coupled flow

The Potter's Tale



- Or...Mud, Glorious Mud
 - Tubular conduit for fluids...out and in
 - Macro Tubes
 - Clay colloidal particles are everywhere
 - Smectite montmorillonite or Bentonite
 - Clay water-based muds
 - Low permeability filtercakes
 - Soft, swellable shales
 - ...compacted clay rocks

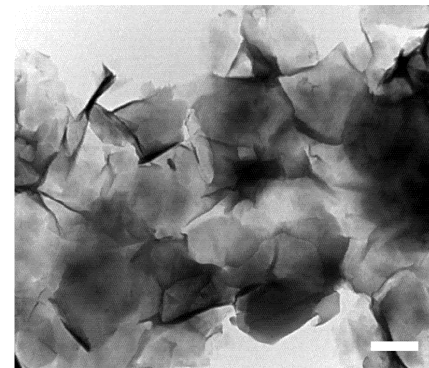


Figure 1: TEM-photograph of Bentonite, bar represents 1 μ m.

The Industrial Driver – Drilling Fluids

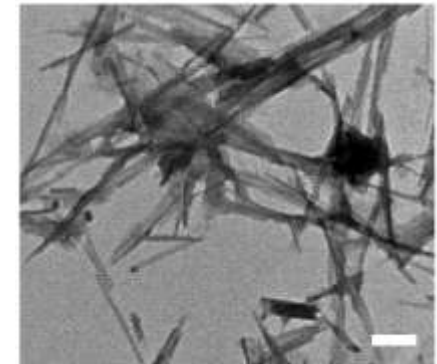
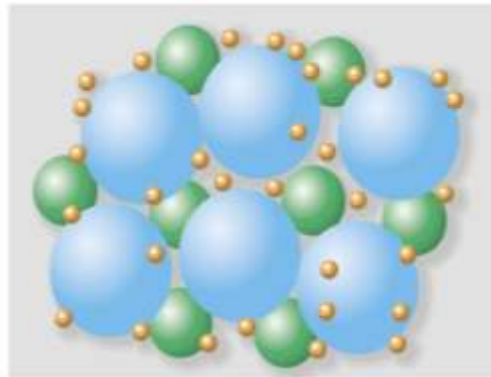
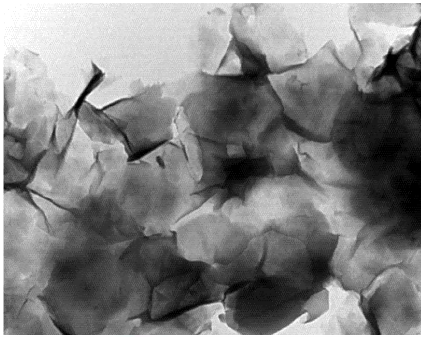
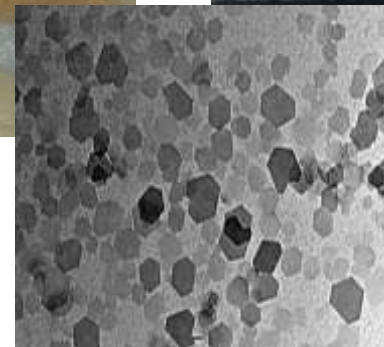
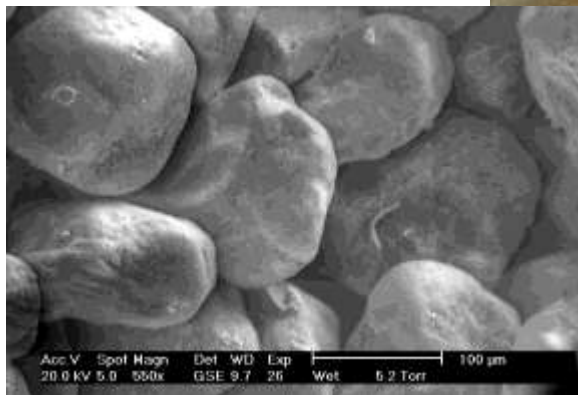
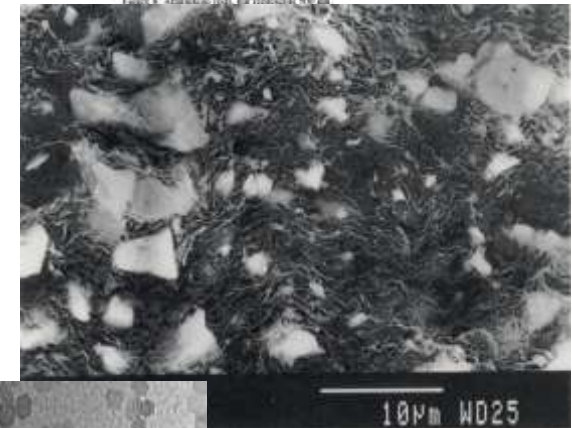
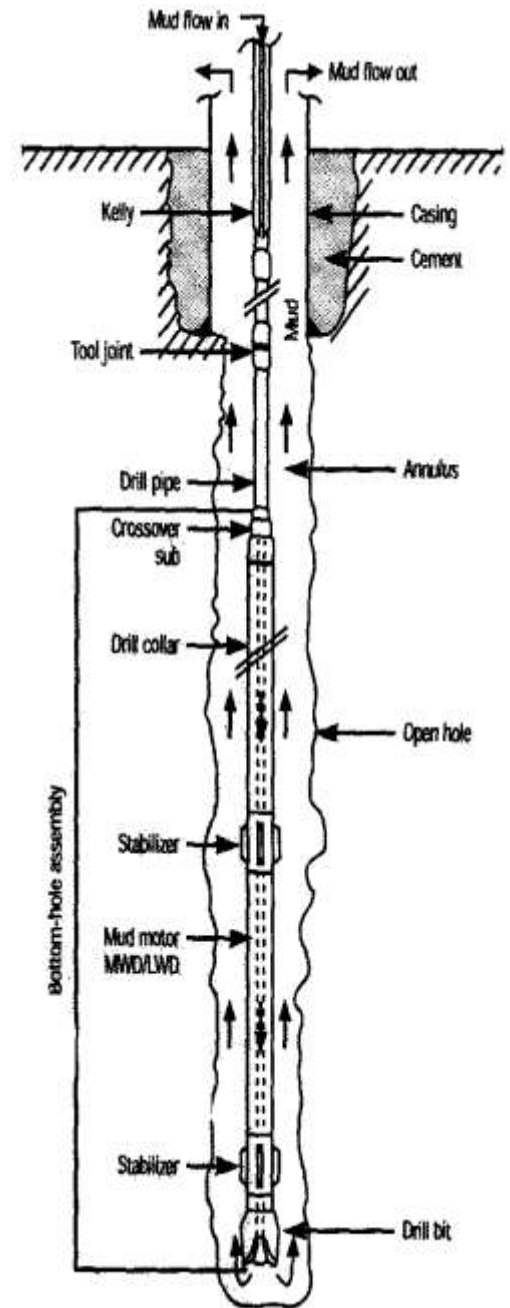


Figure 1. Amorphous silica network, 500 nm



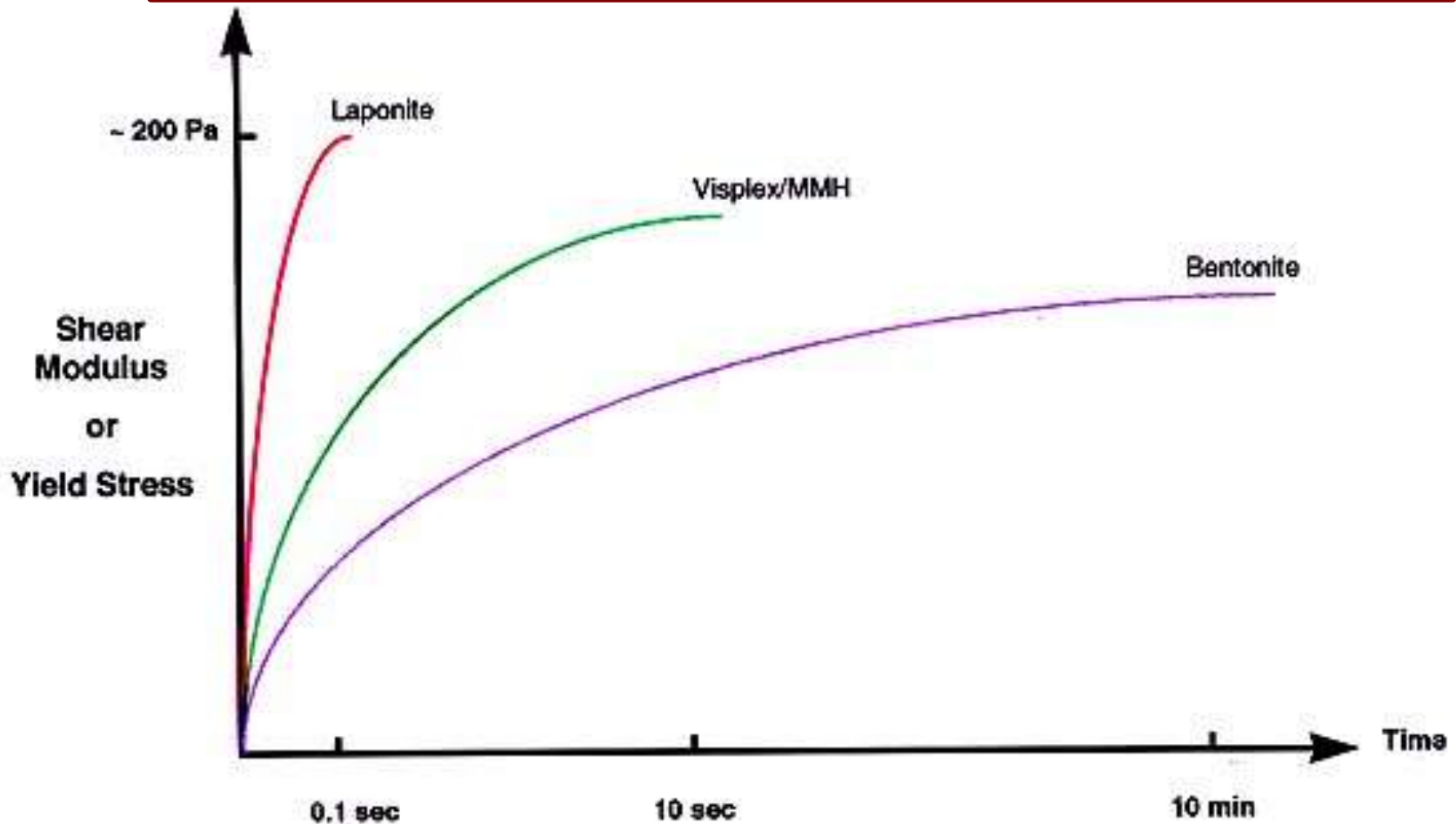
Drilling an oilwell...

- Colloidal clay oilfield drilling fluid
- Rheological behaviour critical
 - Minimize pumping energy
 - Keep cuttings suspended, even when pumps stop



Gelation of mixed colloid drilling fluids on cessation of flow

Concept: Designer Gels or Dial-a-Yield Stress



Base Clay: Montmorillonite or Bentonite

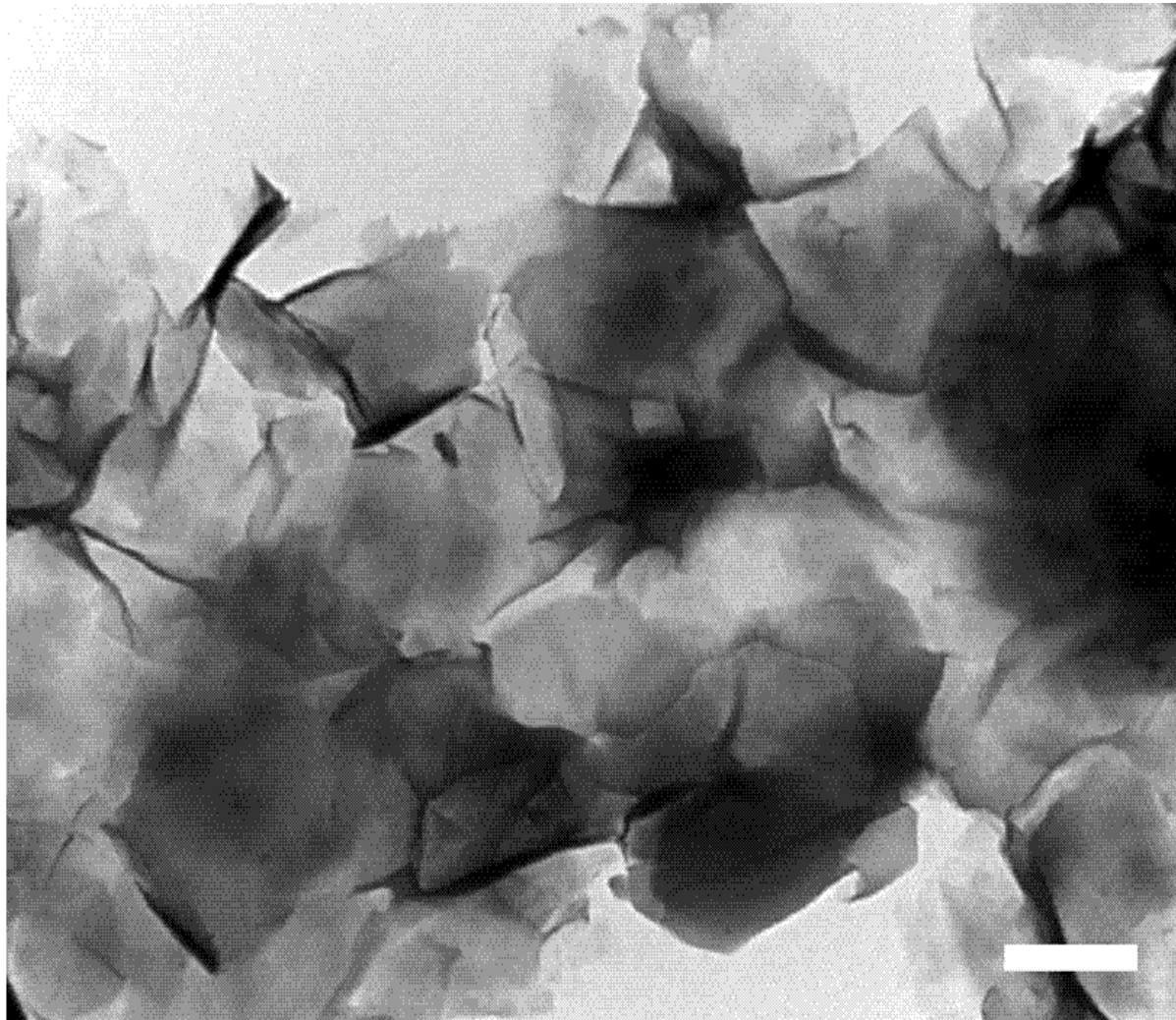
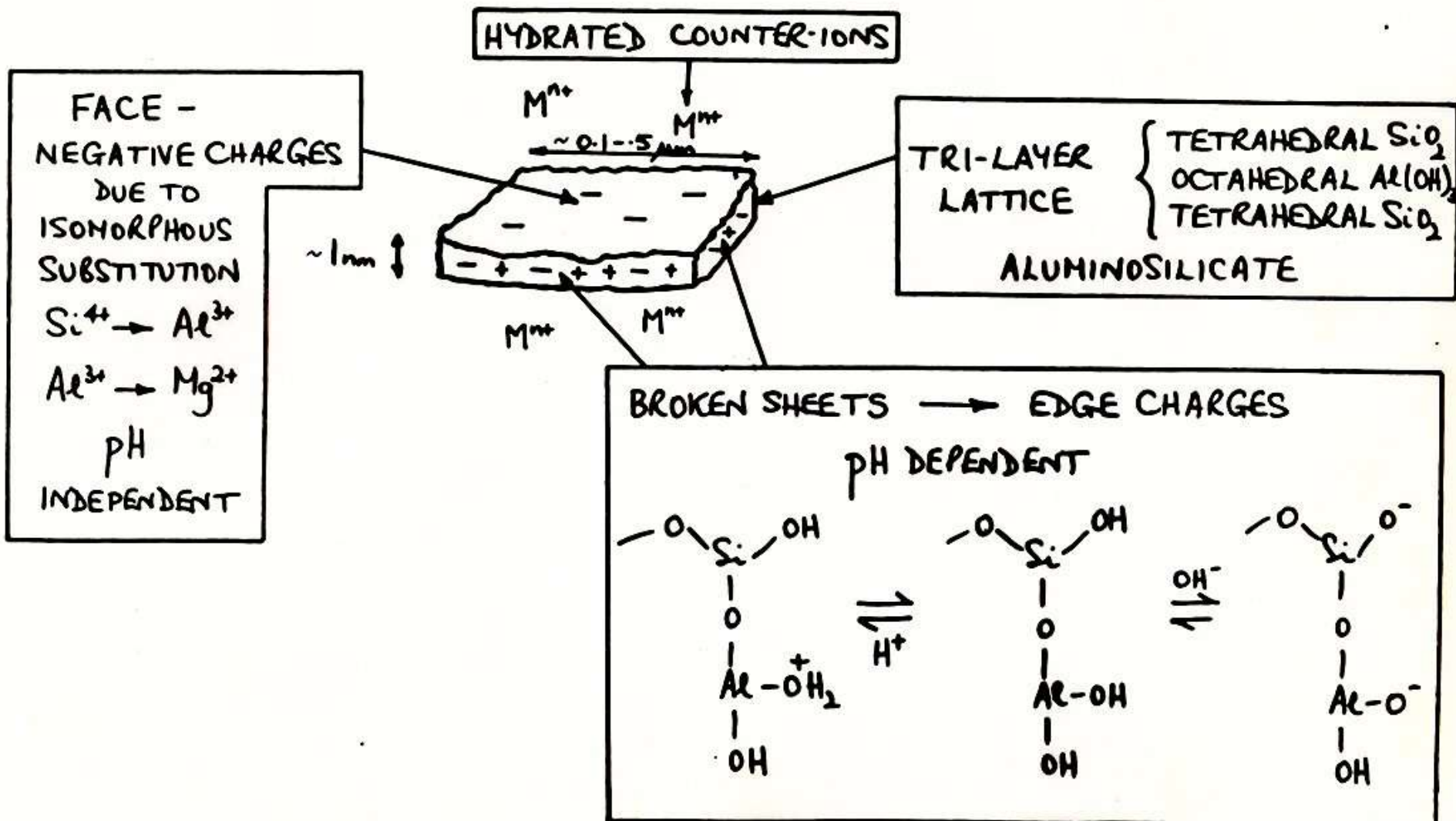
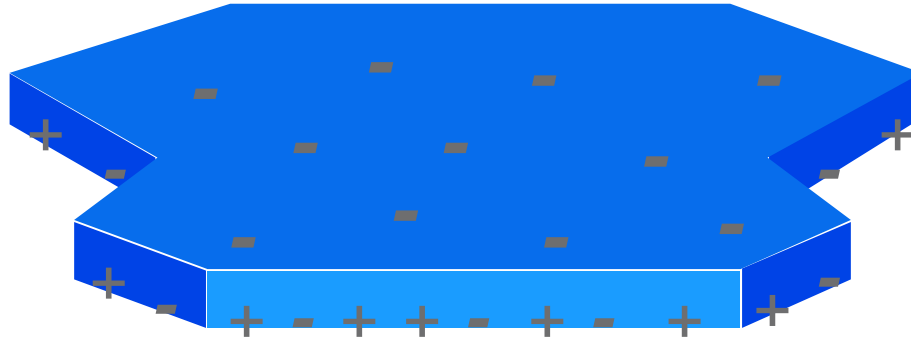


Figure 1: TEM-photograph of Bentonite, bar represents 1 μm .

Montmorillonite Clay Platelets - Bentonite

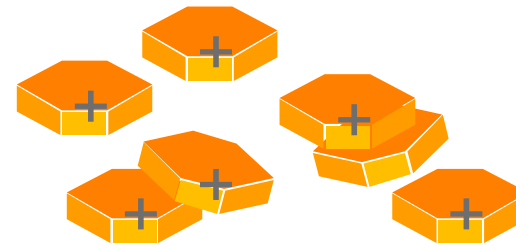


Visplex/Drillplex: Mixed Metal Hydroxide Cationic Colloid



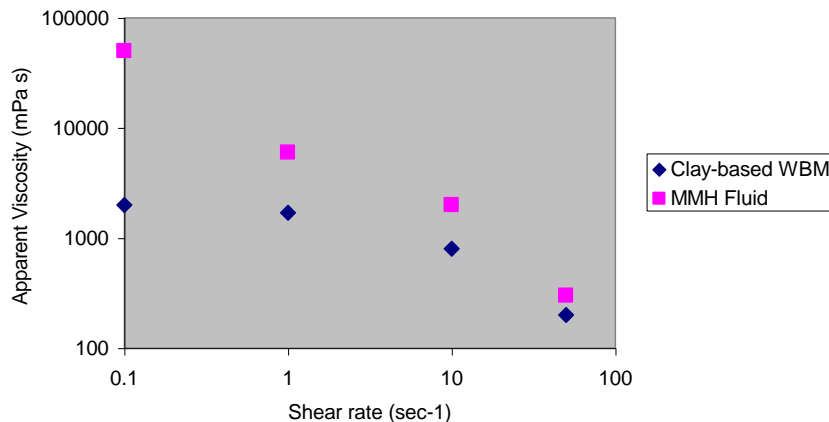
*Bentonite platelet with negative faces.
Edge charges are pH-dependent.*

*VISPLEX crystals:
positive charge due to
electron-deficient lattice*

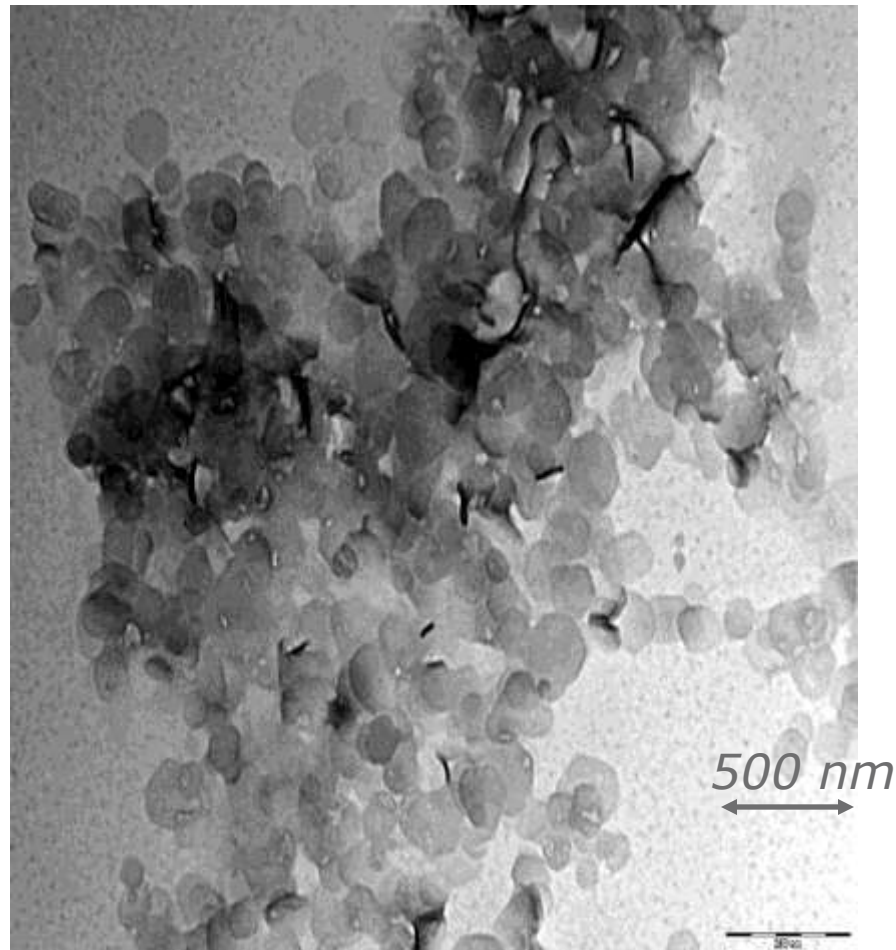


1 micron

hexagonal plates, aspect ratio ~10
plate diameter ~100nm, Mg/Al ~ 1.0



Mixed metal oxide: TEM image



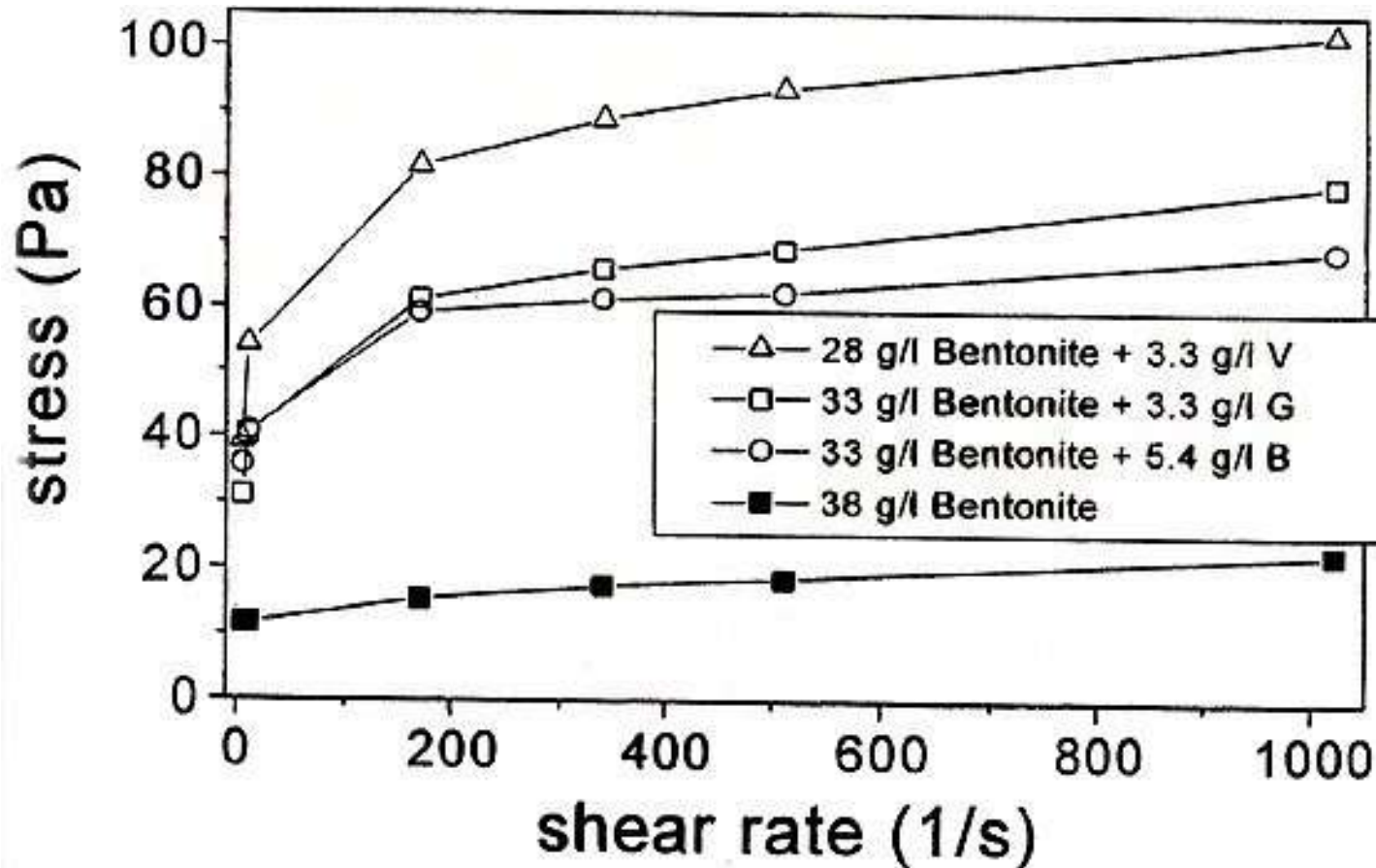
But...problems -

- *Loss of viscosity with salt, brines...seawater*
- *Gel degrades at temperatures higher than 115 °C*

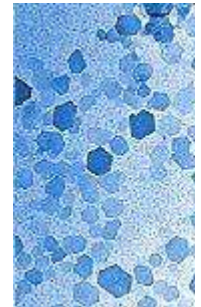
Visplex was renamed Drillplex but still these issues persisted.

Henk Lekkerkerker to the rescue...

Flow curves for mixtures of bentonite and various colloidal thickeners



Gibbsite



Boehmite

Felixplex Patents



(12) UK Patent (19) GB (11) 2 378 716 (13) B

(45) Date of publication: 14.01.2004

(54) Title of the invention: Process fluid

(51) Int Cl⁷: C09K 7/02

(21) Application No: 0119375.4

(22) Date of Filing: 08.08.2001

(43) Date A Publication: 19.02.2003

(52) UK CL (Edition W):
E1F FGP

(56) Documents Cited:
GB 2112042 A US 6025303 B
US 5663122 A US 5532212 A
US 4680128 A US 4675119 A
US 4447341 B US 4230586 B
US 4048077 B

(58) Field of Search:
As for published application 2378716 A viz:
UK CL (Edition S) E1F FGP
INT CL⁷ C09K 7/02
Other: Online: WPI, EPODOC, PAJ
updated as appropriate

(72) Inventor(s):
Felix van der Kooij
Henk Lekkerkerker
Edo Sicco Boek

(73) Proprietor(s):
M-I L.L.C.
(Incorporated in USA - Delaware)
5950 North Course Drive, Houston,
Texas 77072, United States of America

(74) Agent and/or Address for Service:
Mewburn Ellis
York House, 23 Kingsway, LONDON,
WC2B 6HP, United Kingdom

(12) United States Patent
Van Der Kooij et al.

(10) Patent No.: US 7,338,922 B2
(45) Date of Patent: Mar. 4, 2008

(54) PROCESS FLUID

(75) Inventors: **Felix Van Der Kooij**, Schiedam (NL);
Henk Lekkerkerker, Maarn (NL); **Edo**
Sicco Boek, Cambridgeshire (GB)

(73) Assignee: **M-I L.L.C.**, Houston, TX (US)

(*) Notice: Subject to any disclaimer, the term of this
patent is extended or adjusted under 35
U.S.C. 154(h) by 410 days.

(21) Appl. No.: 10/486,043

(22) PCT Filed: Aug. 6, 2002

(86) PCT No.: PCT/GB02/03623

§ 371 (c)(1),
(2), (4) Date: Jul. 2, 2004

(87) PCT Pub. No.: WO03/014252

PCT Pub. Date: Feb. 20, 2003

(65) Prior Publication Data
US 2004/0242431 A1 Dec. 2, 2004

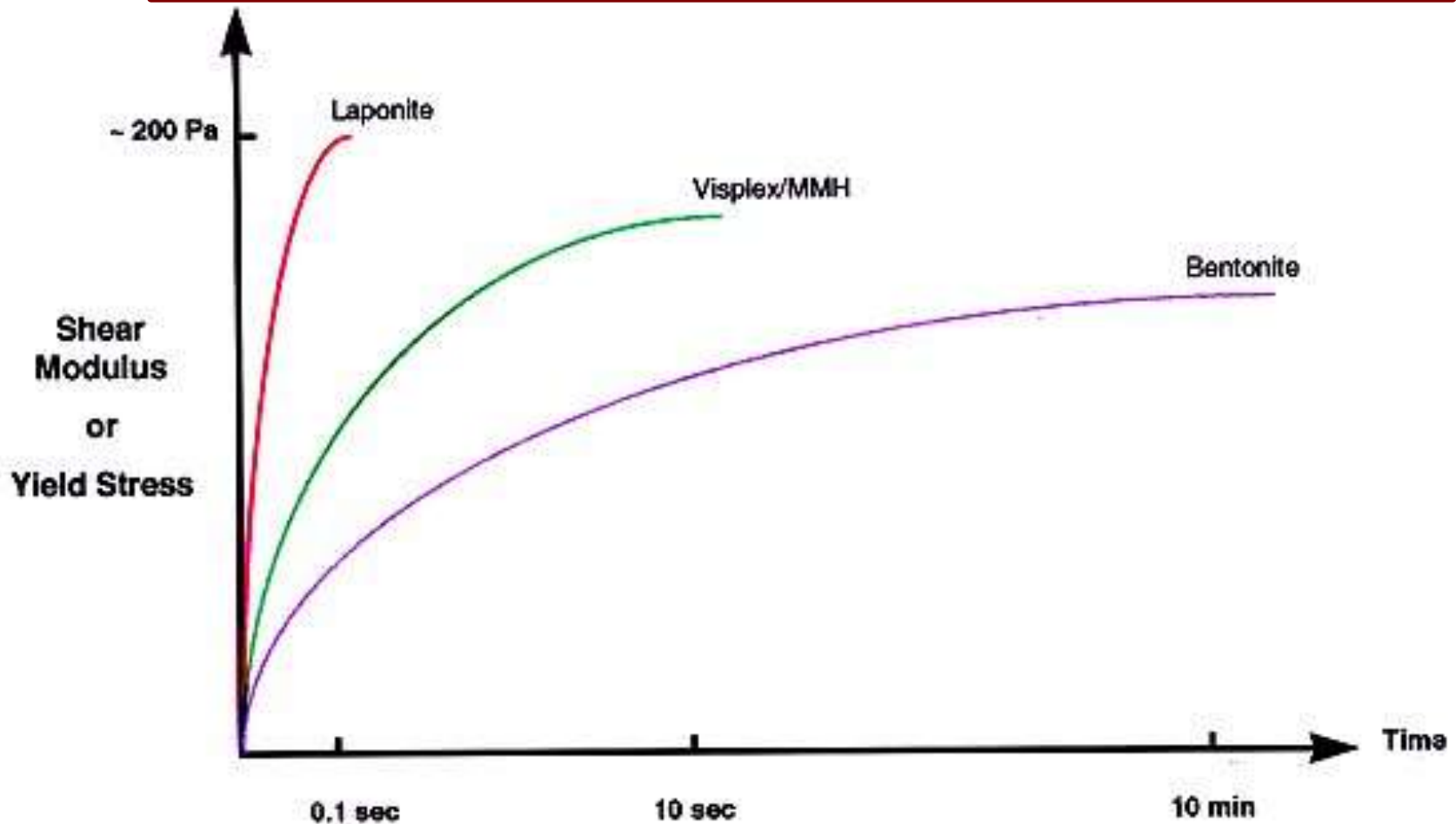
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4,240,915 A	12/1980	Block
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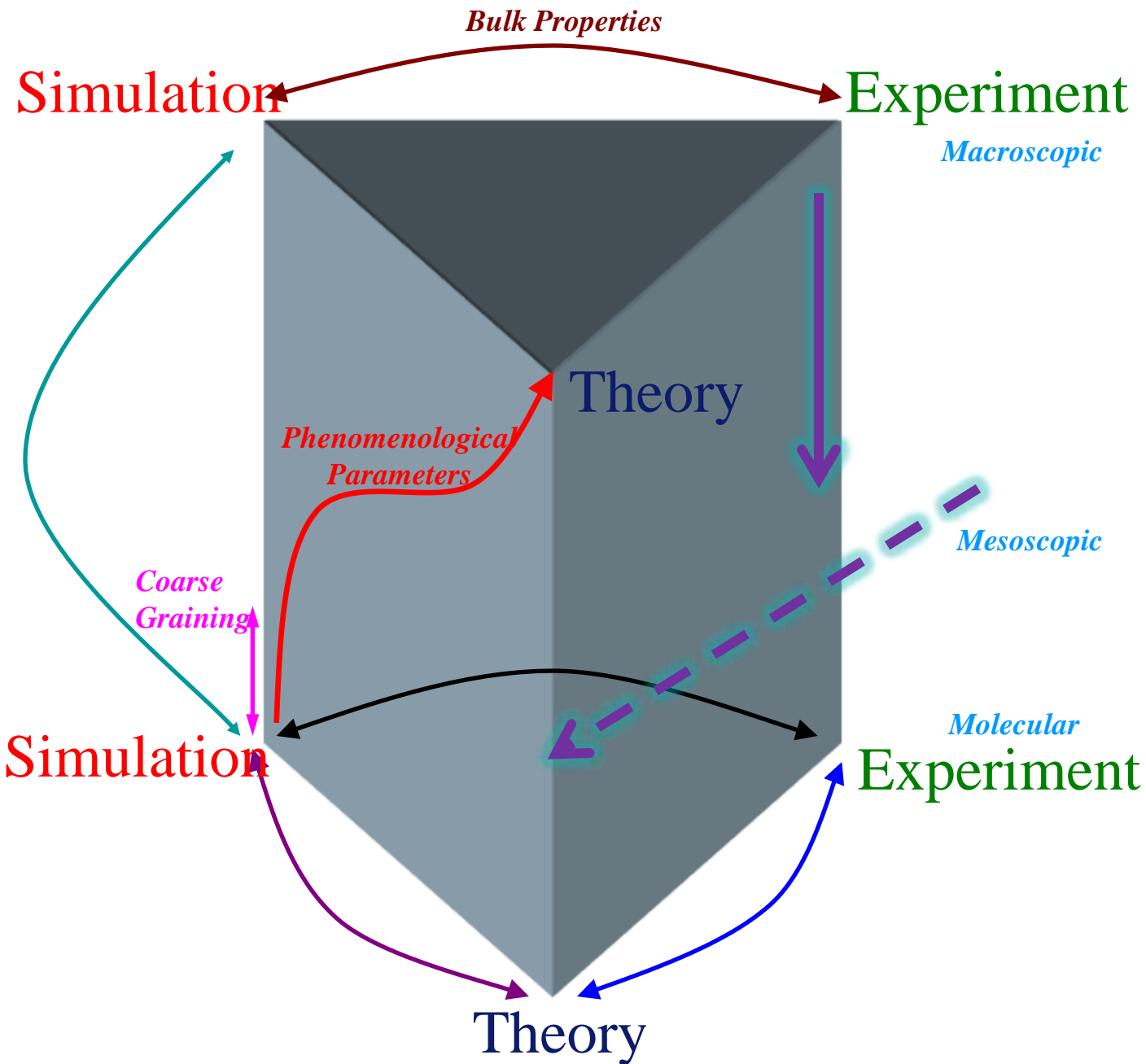
Buining et al., "Preparation of Colloidal Boehmite Needles by Hydrothermal Treatment of Aluminum Alkoxide Precursors", J. Amer. Ceram. Soc., vol. 74, No. 6, 1991, pp. 1303-1307.
Philippe et al., "Isotropic and Birefringent Dispersions of Surface Modified Silica Rods With a Boehmite-Needle Core", Langmuir, vol. 10, 1994, pp. 4451-4458.
van der Kooij et al., "Formation of Nematic Liquid Crystals in Suspensions of Hard Colloidal Platelets", J. Phys. Chem. B, vol. 102, 1998, pp. 7829-7832.
Wierenga et al., "Aqueous Dispersions of Colloidal Gibbsite Platelets: Synthesis, Characterisation and Intrinsic Viscosity Measurements", Colloids and Surfaces A, vol. 134, 1998, pp. 359-371.

Gelation of mixed colloid drilling fluids on cessation of flow

Concept: Designer Gels or Dial-a-Yield Stress



Type of Study



Shaplex: Objectives of Study

- To determine the rheology over a wide range of stress/strain-rates (using oscillatory, transient and continuous shear) of well-characterised gelling suspensions of colloids of varying shape:
rods (boehmite), laths (hectorite), plates (gibbsite)
- To explore the rheological synergies in mixed-shape colloidal suspensions:
2.5% w/w laths (hectorite)
+ 0.25% w/w rods (boehmite)
or plates (gibbsite)
or spheres (alumina-coated silica)

Acknowledgements

Thanks to

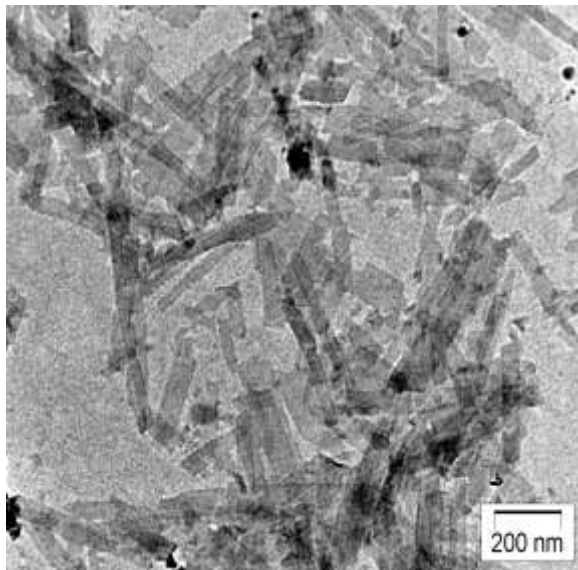
- Henk, Annemieke, Marcel and Louise for many years of fruitful collaboration
- Nederlandse Organisatie voor Wetenschappelijk Onderzoek (NWO) and
- Schlumberger Cambridge Research, for financial support to Annemieke ten Brinke
- SoftComp EU 6th Framework Network of Excellence
- Edo Boek of Imperial College London (formerly Schlumberger Cambridge Research) for helpful discussions
- Dzina Kleshchanok, University of Utrecht, for producing the TEM images

Key messages

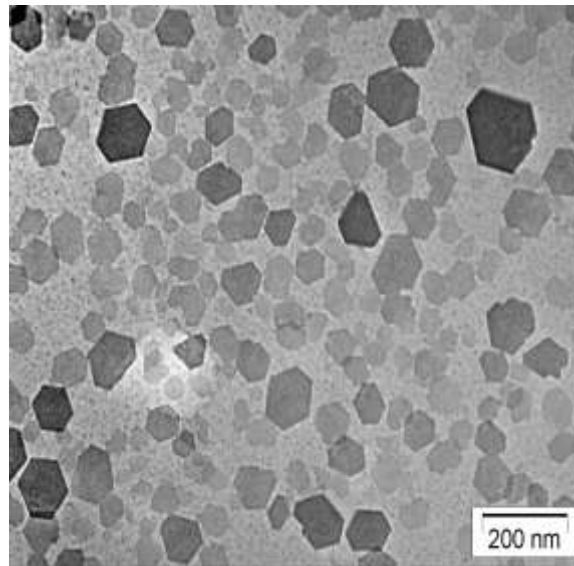
- General complex rheological behaviour of clay and clay-colloid mixtures as they transform from gels (elastoviscous solids) to weakly elastic shear-thinning liquids
- The significant enhancements to gel rheological properties caused by minor ($\sim 1:10$ w/w) additions of a second colloidal component of varying shape
- Contrasts between hectorite and montmorillonite as the base clay
- The contrasting effect of one particular additive (silica spheres) depending on charge and clay concentration

Tuning gel behaviour by shape and charge

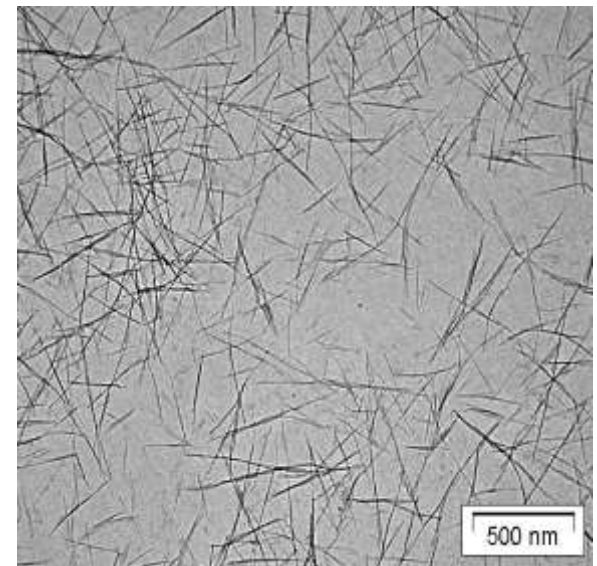
- Understand structure/performance relationships in mixed systems using **model colloids**



Hectorite



Gibbsite



Boehmite

*Henk Lekkerkerker, Annemieke ten Brinke, Marcel Vogel (Utrecht),
Louise Bailey Schlumberger*

Characteristics of Particles

Property	Particle			
	Hectorite	Gibbsite	Boehmite	Ludox CL
Shape	Lath	Plate	Rod	Sphere
L_1 [nm]	288	81	200	12
L_2 [nm]	43	81	10	12
d [nm]	6	6	10	12
Density [g/cm ³]	2.39	1.96	2.06	2.2
α	160	6.8	200	1.0
C^* [g/100 cm ³]	1.5	28.8	1.1	220
pH	8.9	7.8	6.2	4.5
Sign of face charge	–	+	+	+
Conductivity [μ S/cm]	38.1	80.2	46.0	
	@ 1336 ppm	@ 1154 ppm	@ 1045 ppm	
Mobility [10^{-8} m ² /Vs]	-1.2	2.8	3.9	
Zeta potential mV	-9.8	+24.0	+44.2	+42

α is the ratio of hydrodynamic volume V_h ($4\pi (L_1/2)^3/3$) to real particle volume ($\sim L_1 L_2 d$)

C^* is the ‘overlap concentration’ at which the hydrodynamic volumes swept out by the particle’s largest dimension start to overlap = $(100 L_1 L_2 24d \rho)/4\pi L_1^3$

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Characteristics of Particles

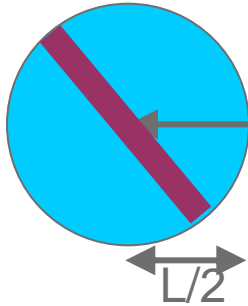
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	Hectorite	Gibbsite	Boehmite	Ludox CL
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Concentration Regimes

Dilute



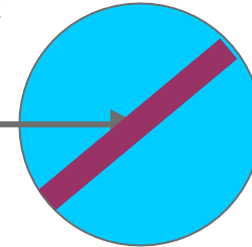
$$\text{Concentration } C = nM_p / V$$

$$\text{Volume per molecule} = V/n = M_p/C$$

$$\text{Hydrodynamic volume } V_h = \pi L^3/6$$

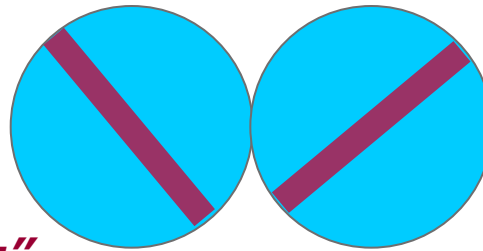
$$R \gg L$$

$$V/n = M/C \gg V_h$$



Semi-Dilute

Critical Overlap Concentration
 $C^* = M_p / V_h$



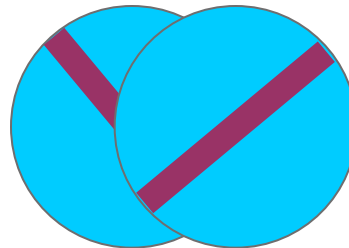
$$R = L$$

$$V/n = M/C = V_h$$

$$C = C^*$$

"Hydrodynamic close-packing"

Concentrated



$$R \ll L$$

$$V/n = M/C \ll V_h$$

$$C \gg C^*$$

Multi-technique study

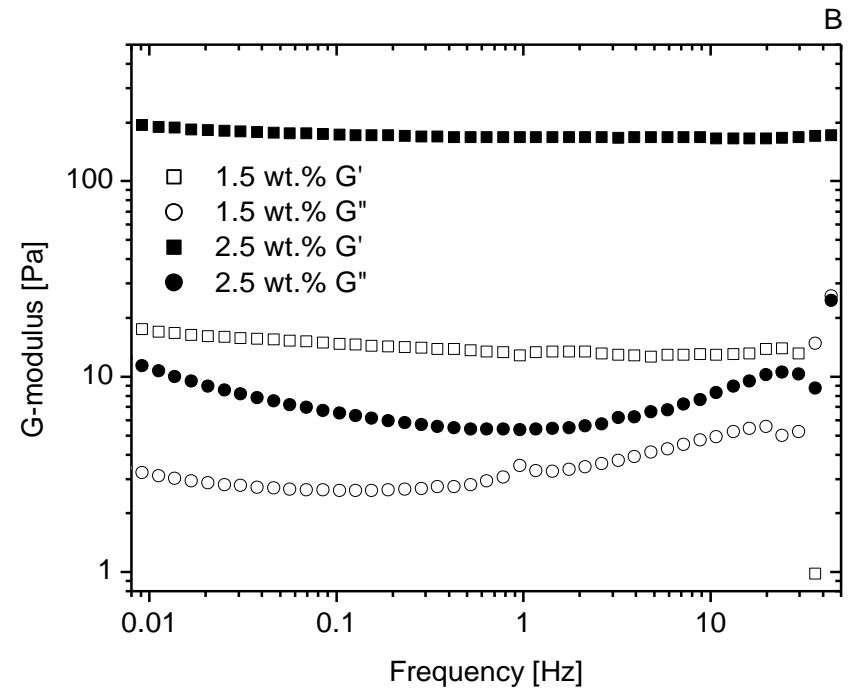
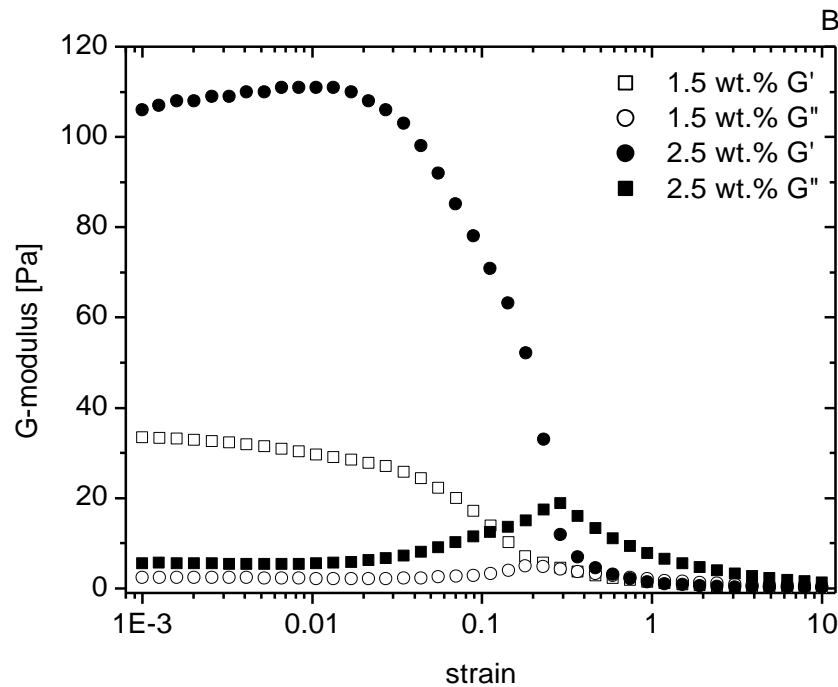
- *Oscillatory Shear*
 - *Creep*
 - *Steady Shear*
 - *Controlled Stress*
 - *Controlled Shear Rate*
-
- *Measurement Systems*
 - *1°, 2° and 4° cone & plate*
 - *Micro-roughened and smooth*
-
- *Controlled sample pre-shearing preparation protocols*

Pure Components

A few remarks...

Hectorite – Oscillatory Shear Flow

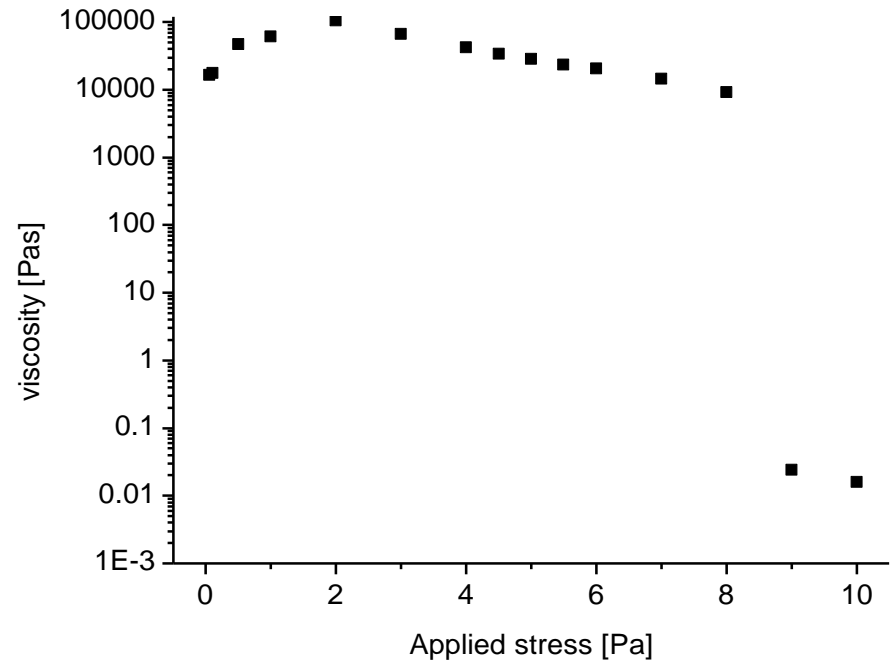
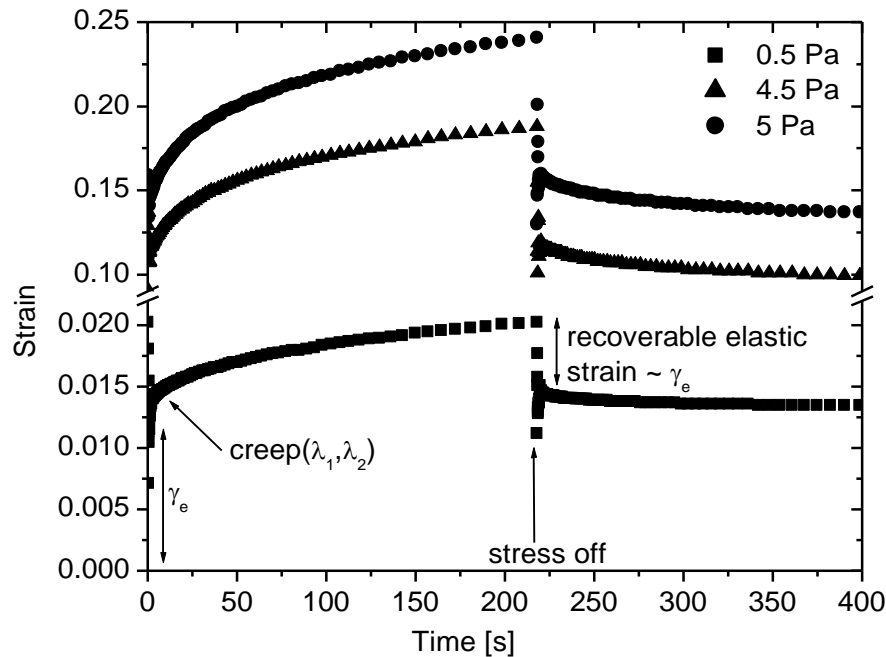
$C^* \sim 1.5 \text{ wt}\%$



Hectorite – Gel State

Hectorite – Creep

C = 2.5 wt% = 1.7C*

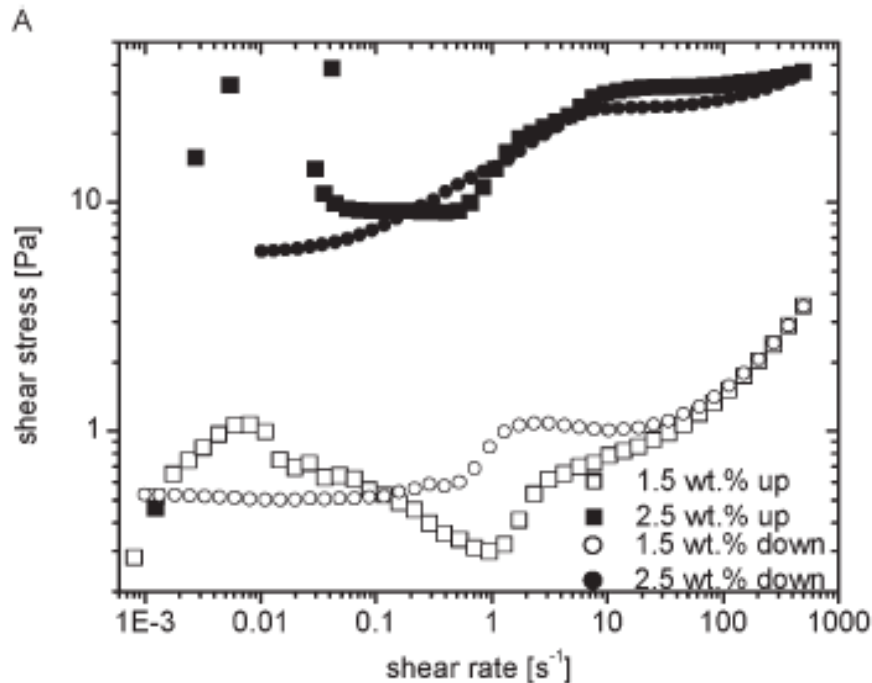


Hectorite – Transition from Gel to Sol

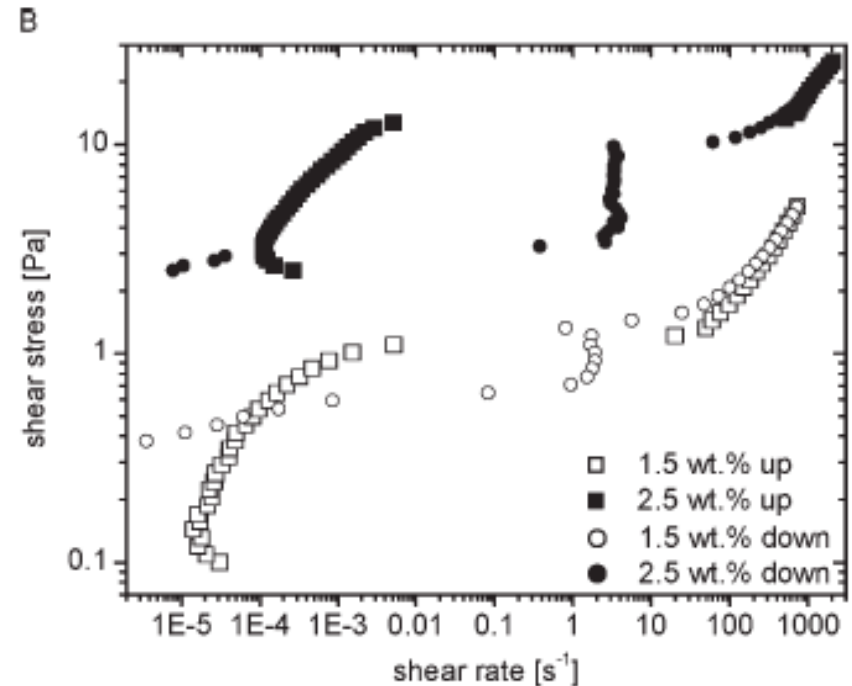
Hectorite – Continuous Shear

Recovered Gel

$C^* \sim 1.5 \text{ wt}\%$



Controlled Shear Rate



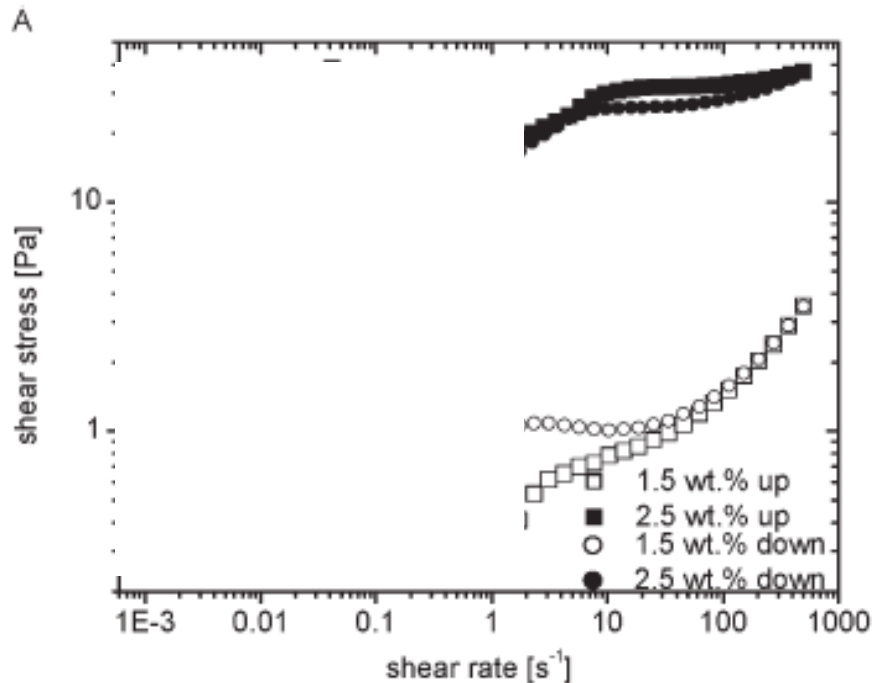
Controlled Shear Stress

Hectorite Gel – From Cradle to Grave and Back Again

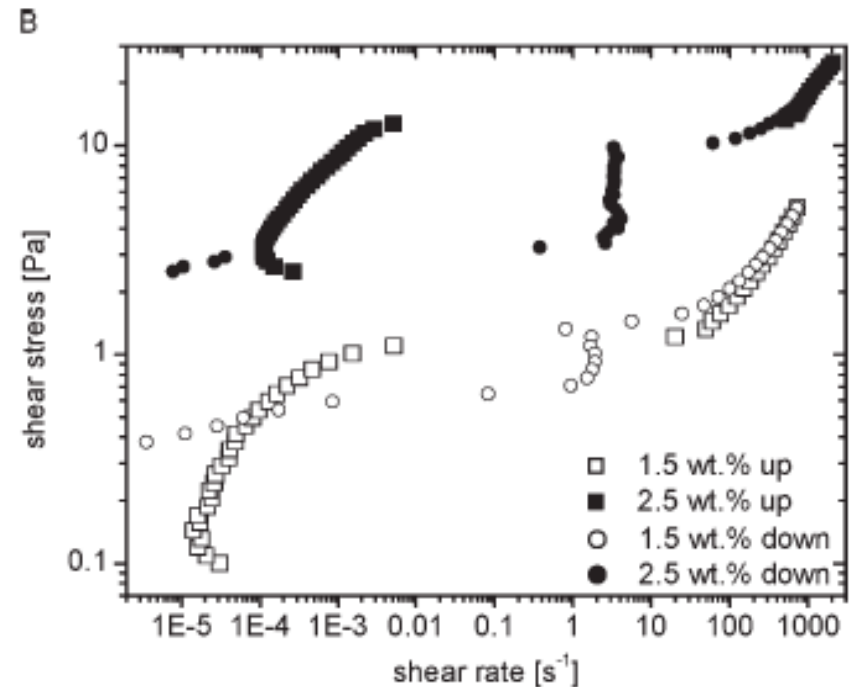
Hectorite – Continuous Shear

Recovered Gel

$C^* \sim 1.5 \text{ wt}\%$



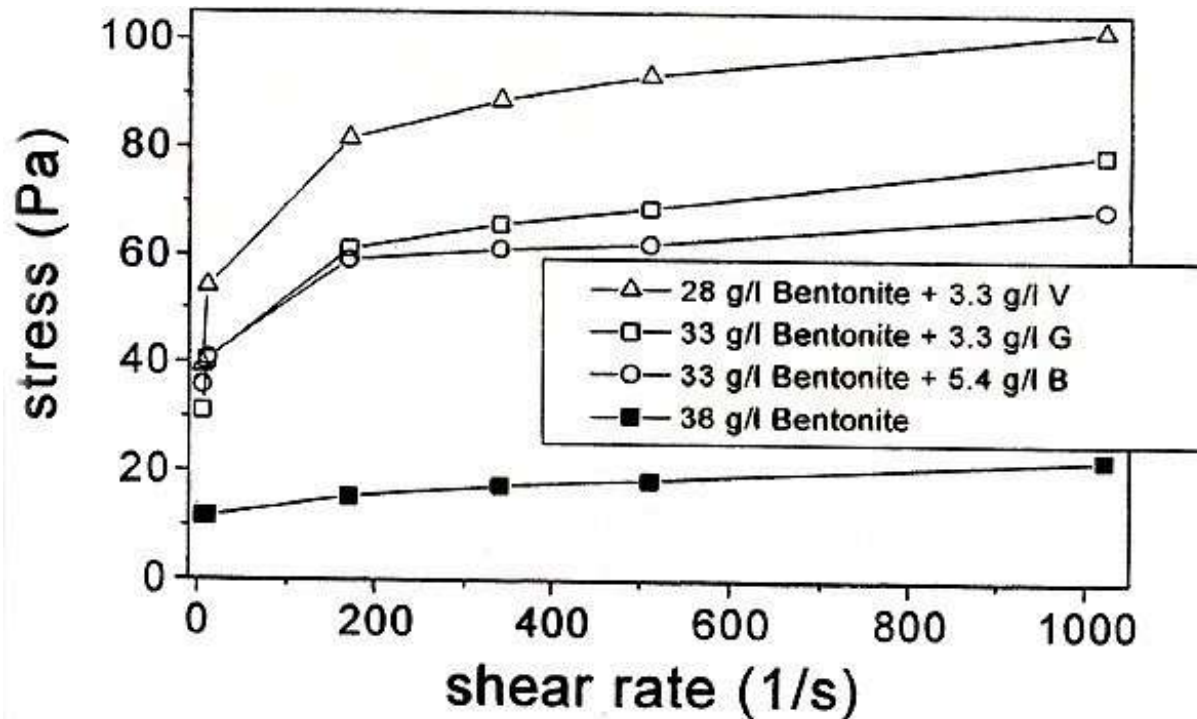
Controlled Shear Rate



Controlled Shear Stress

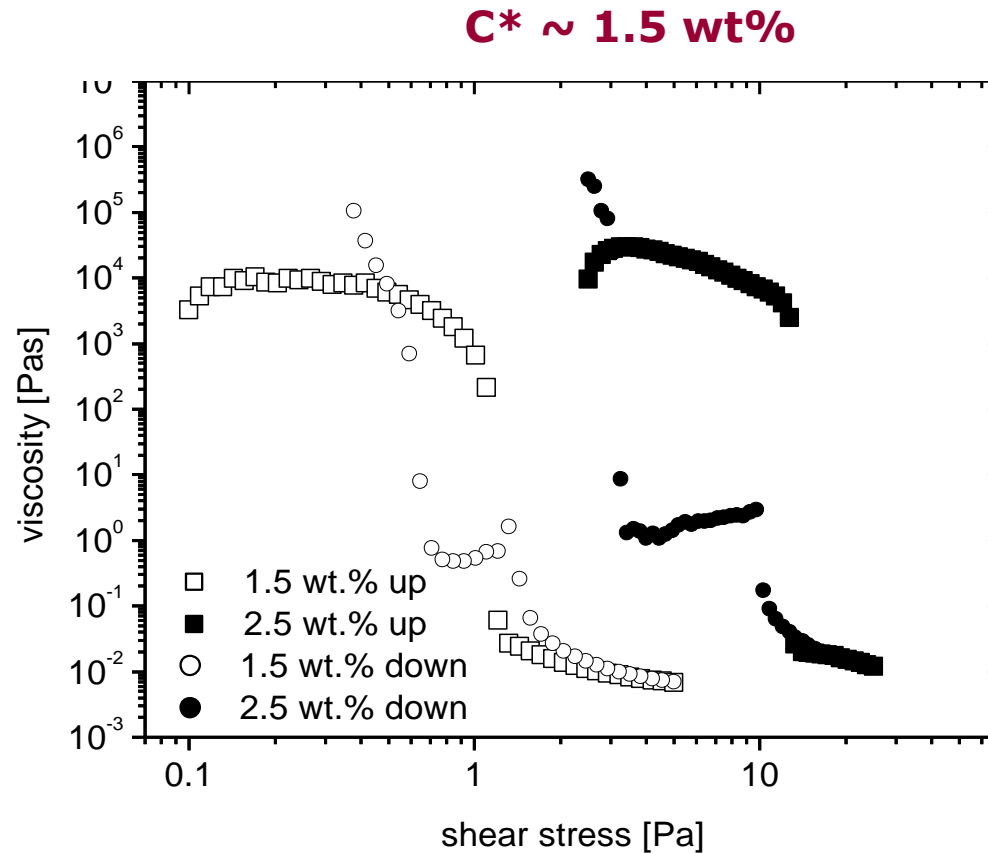
Hectorite Gel – From Cradle to Grave and Back Again

Fann Flow Curves Probe only the Liquid Region



Bingham Model $\tau = \tau_y + \eta\dot{\gamma}$
Herschel Bulkley Model $\tau = \tau_y + K\dot{\gamma}^n$
are only the tip of the iceberg!

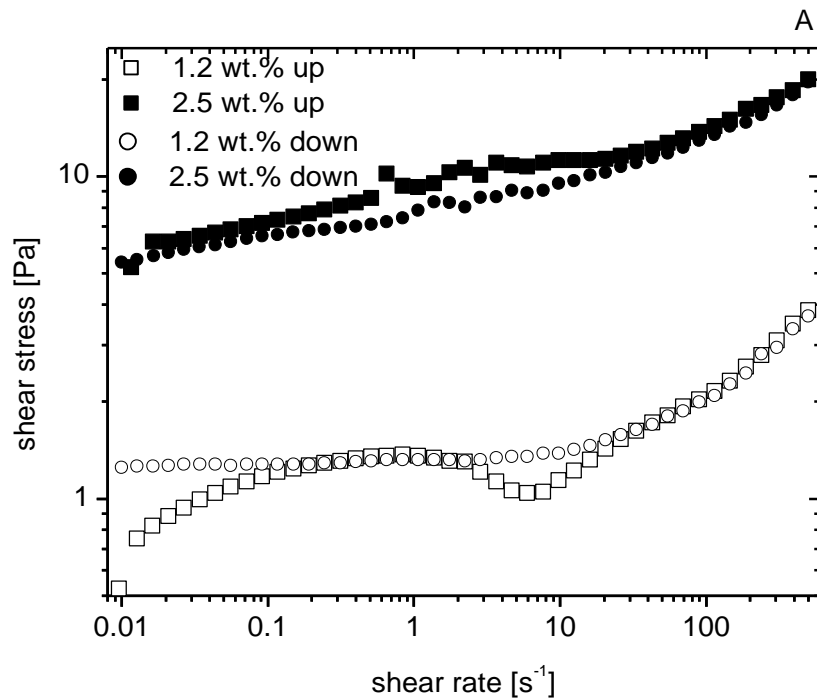
Hectorite – Continuous Shear



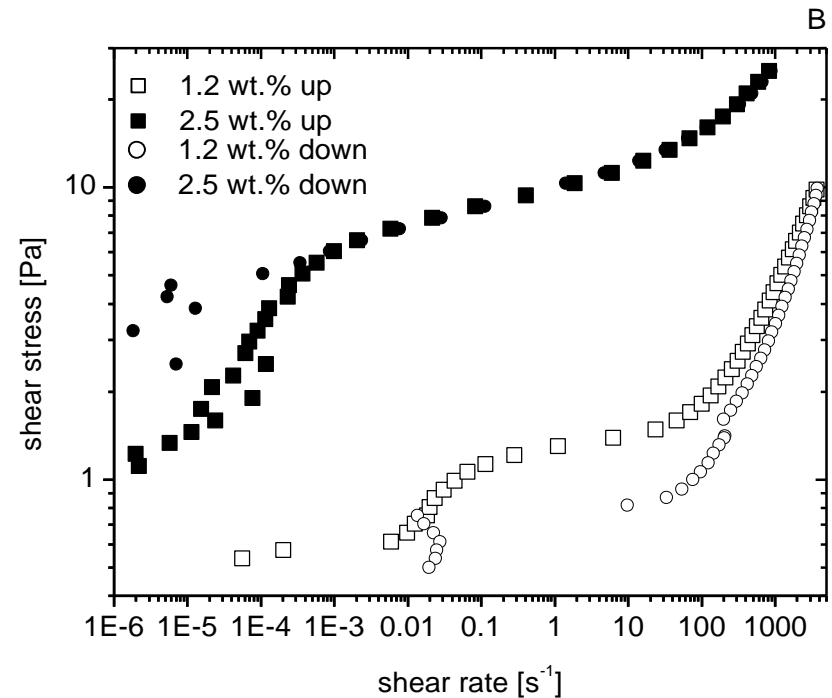
Controlled Shear Stress – Recovered Gel

Boehmite Rods – Continuous Shear

$C^* \sim 1.1 \text{ wt}\%$

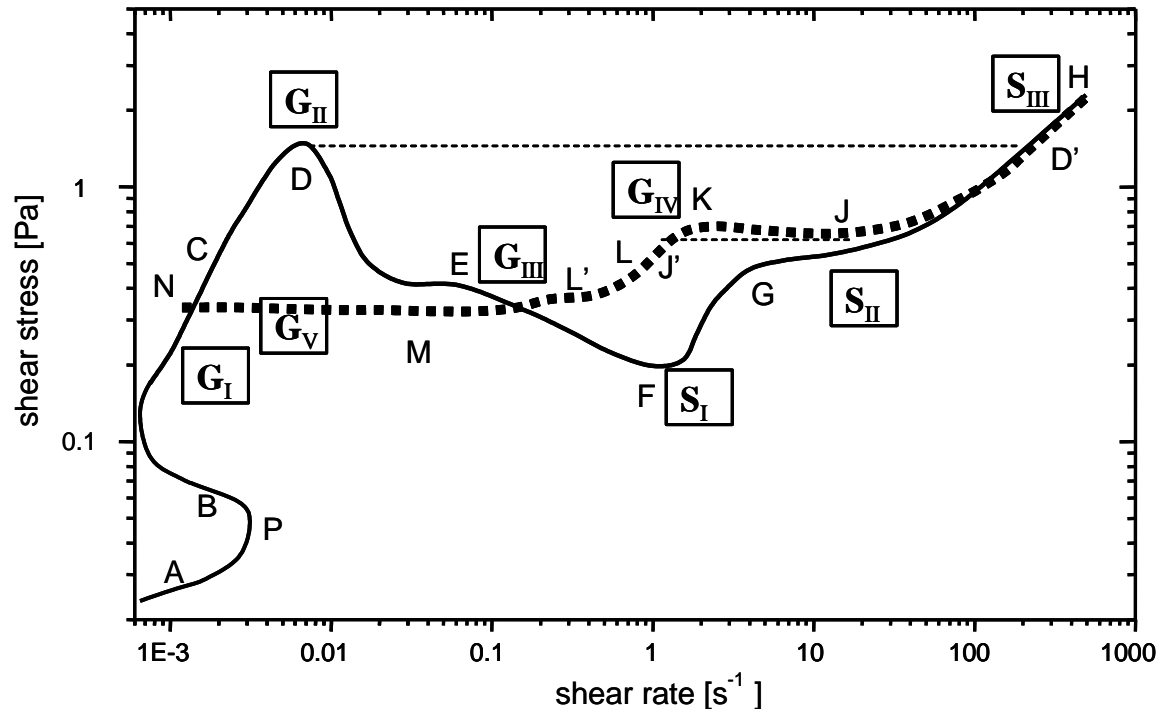


Controlled Shear Rate



Controlled Shear Stress

Continuous Shear – Generic Flow Curves



G_I = Disordered Gel

G_{II} = Ordered Gel

G_{III} = Breaking Gel

G_{IV} = Partially-ordered Gel

G_V = Ordered Gel (not same as G_{II})

S_I = Structured Sol

S_{II} = Breaking Fluid

S_{III} = Dispersed, Partially-ordered Sol

Common critical factor – yield strain

- Consistent values of G , η , ' τ_y ', γ_y etc from oscillatory, transient and continuous shear experiments
- γ_y essentially independent of concentration

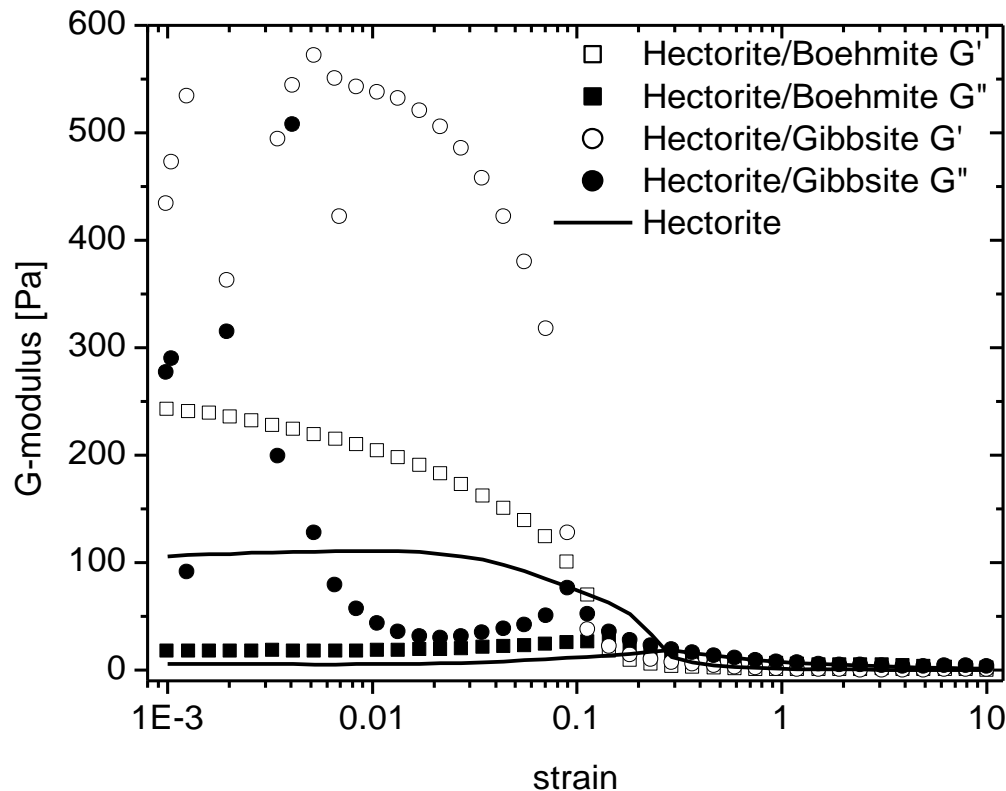
γ_y for

- Gibbsite plates 0.1 ± 0.05 ($L_1 = 81 \text{ nm}$)
- Hectorite laths 0.3 ± 0.05 ($L_1 = 200 \text{ nm}$)
- Boehmite rods 0.45 ± 0.05 ($L_1 = 288 \text{ nm}$)
- Same ordering as L_1 or parameter α

Mixed Shape Dispersions

Replacement of 10 wt% of the Hectorite
(@ 2.5 wt%) by a second component

Mixed-shape Suspensions – Oscillatory Flow



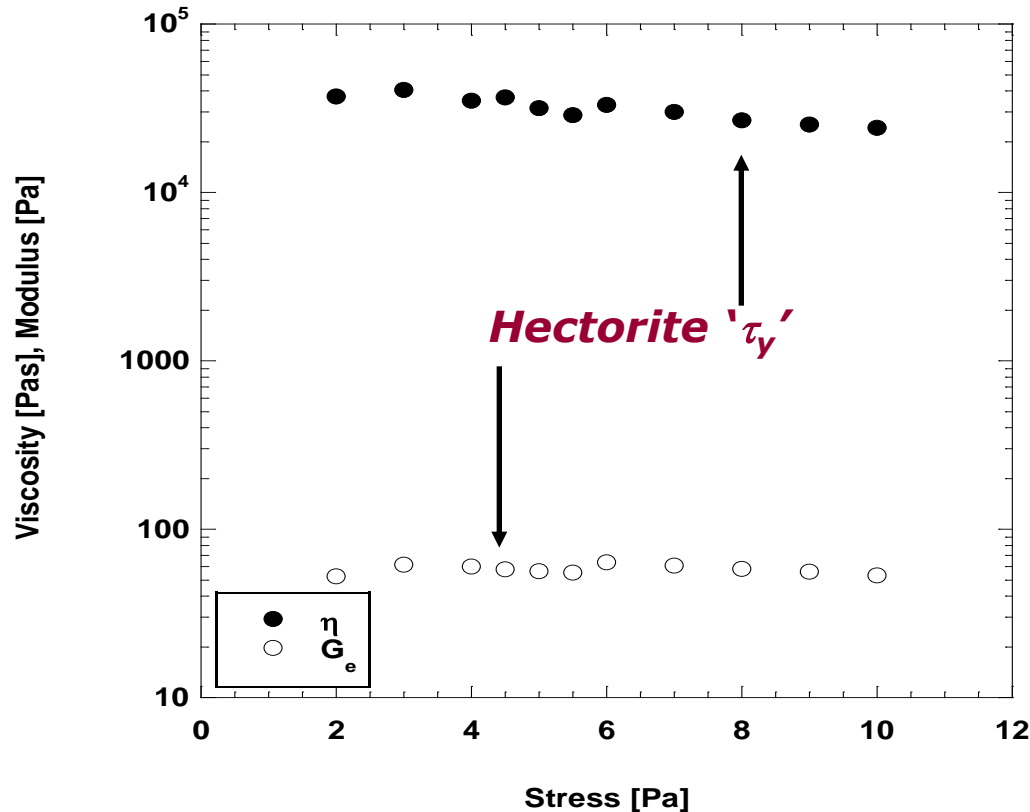
Boehmite $\alpha = 200$

Hectorite $\alpha = 160$

Gibbsite $\alpha = 6.8$

Hectorite 2.5 wt% (1.7c*), Minor Component 0.25 wt%

Creep viscosity $\eta(t)$ and plateau modulus G_e

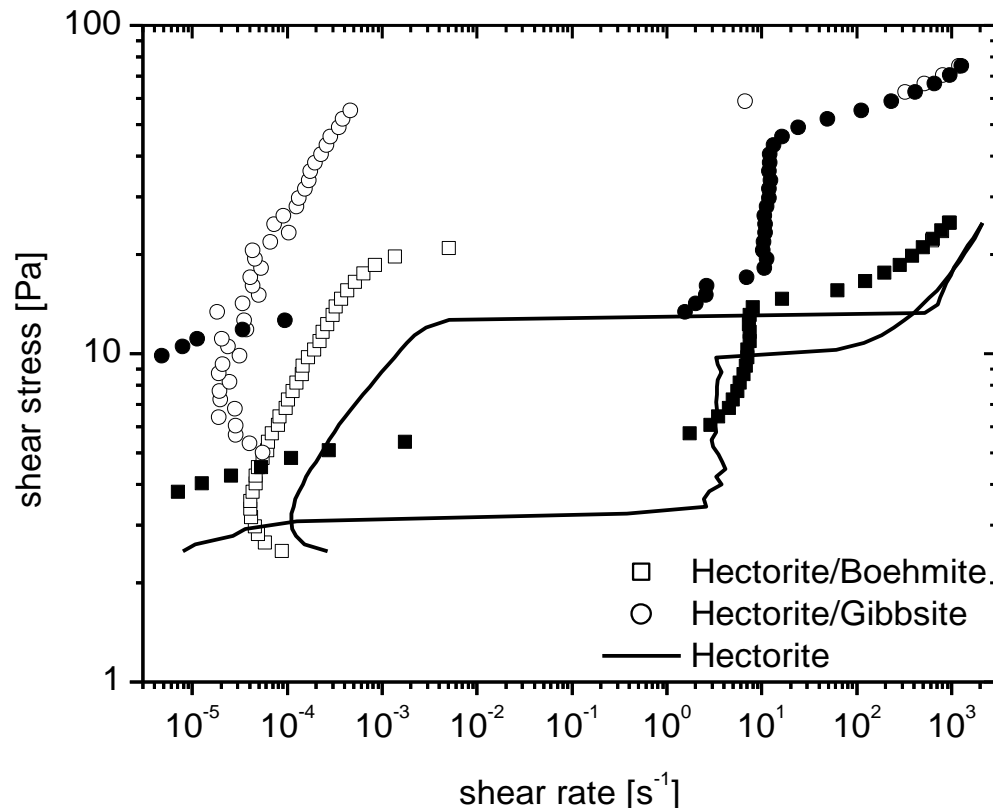


Hectorite-boehmite 10:1 mixture

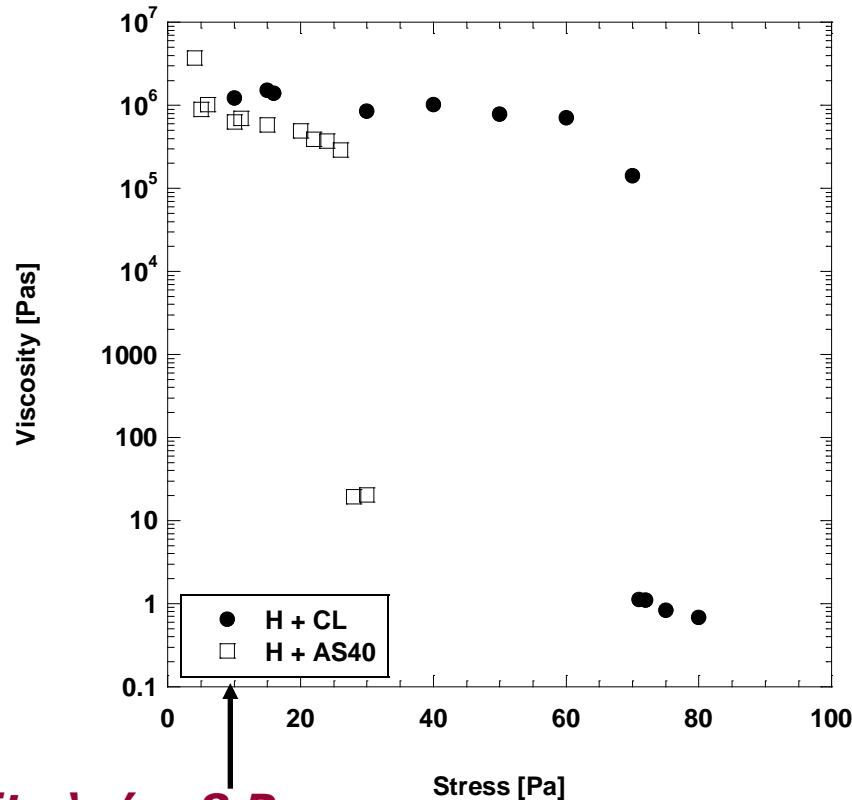
$$C_{\text{hectorite}} = 2.5 \text{ wt\%} = 1.7C^*$$

Controlled shear stress flow curves - effect of 10 wt% minor colloid

$$C_{\text{hectorite}} = 2.5 \text{ wt\%} = 1.7C^*$$



Post-creep viscosities – added silica spheres and the effect of charge

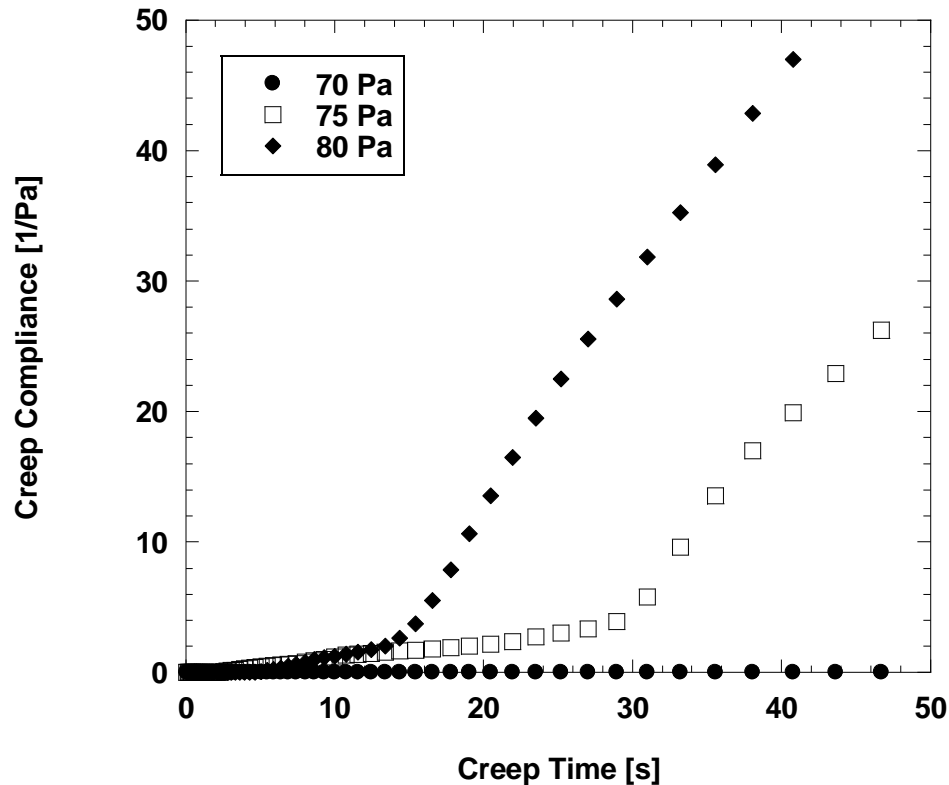


Ludox CL cationic
Ludox AS40 anionic
D = 12 nm for both

Pure Hectorite ' τ_y ' = 8 Pa

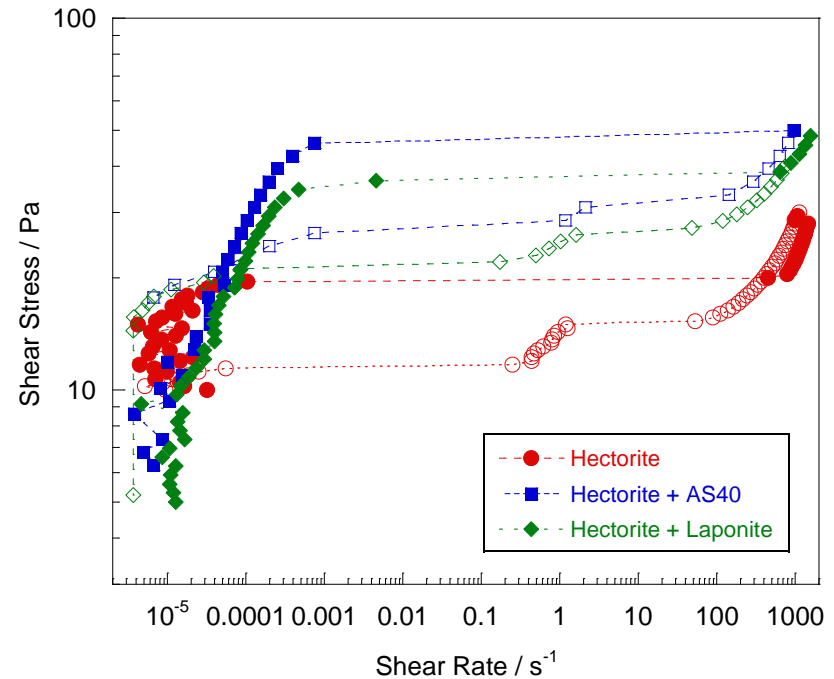
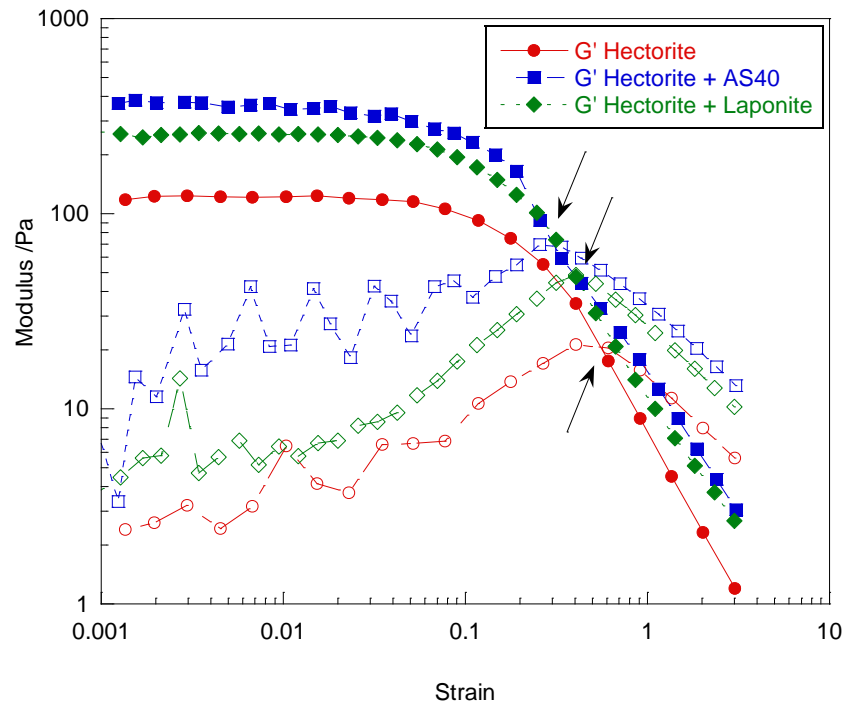
C_{hectorite} = 2.8 wt% = 1.9C*

Early-time creep behaviour near ' τ_y '



Hectorite (-ve)-Ludox CL (+ve)

Comparative anionic mixtures



Again enhancement of rheology laths + plates < spheres

Enhancement by adding minor colloid 1:10 to 2.5 wt% Hectorite

Property Colloids	Hectorite	Hectorite-Boehmite	Hectorite-Gibbsite	Hectorite-Ludox CL
G''	1	2	5	30
τ_y	1	1	2	6
G'_y	1	1	2	20
G' (1Hz)	1	1.4	4	20
G_e (peak)	1	1	-	1500
$\eta(\tau \rightarrow 0)$ (Creep)	1	0.5	-	14
τ_y (Creep)	1	>1.2	-	8
$\eta(\tau \rightarrow 0)$ (Steady Shear)	1	3	10	20
τ_y (Steady Shear)	1	1.5	4.5	6
Yield Strain (Oscillatory)	1	0.6	0.3	0.25
Yield Strain (Cont Shear)	1	0.5	0.2	0.06
Relative particle concentration, n_p		2	1	280
Packing ratio per hectorite lath		0.8	4.5	200

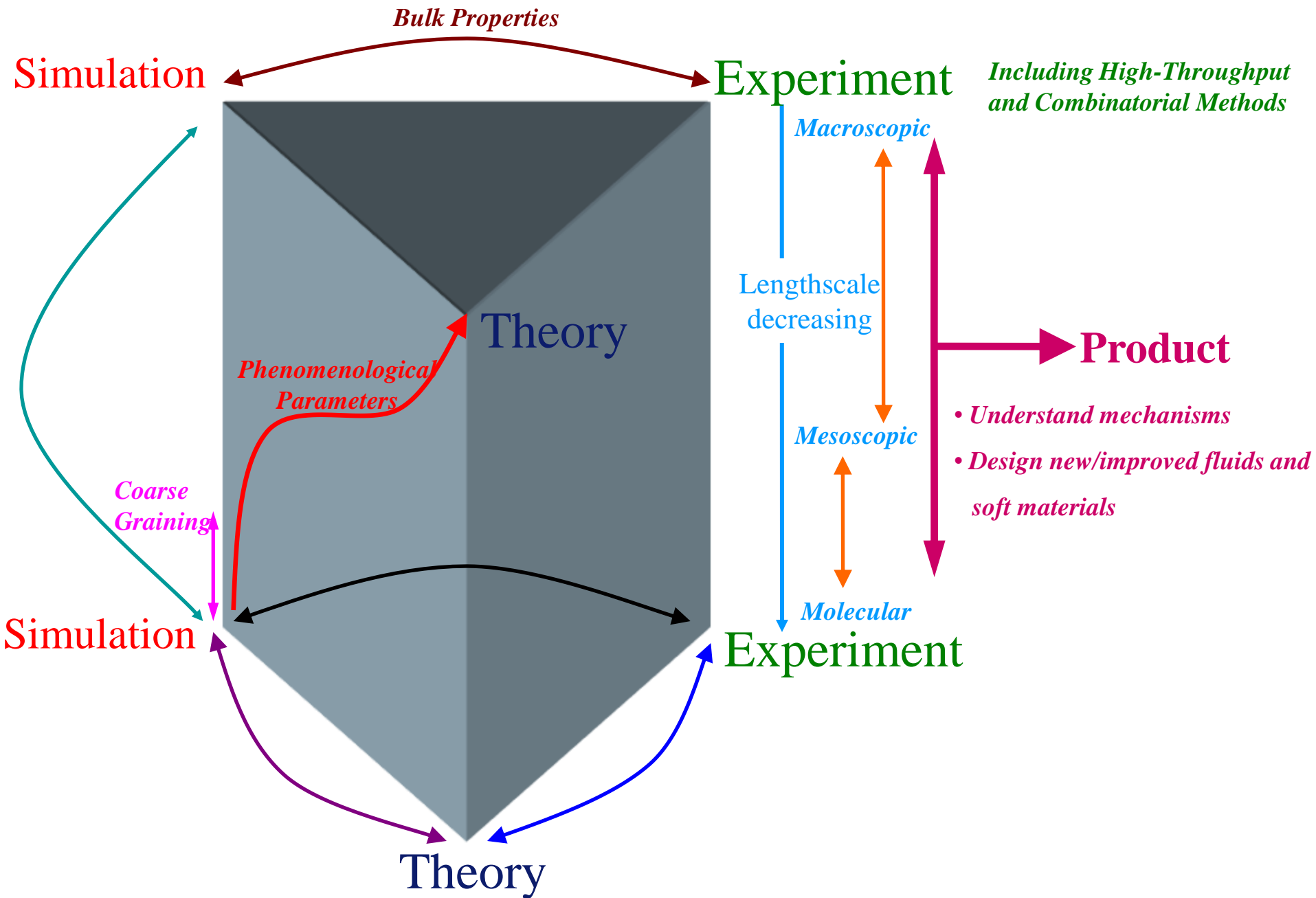
Mixed Colloid Conclusions

- Complexity of hectorite and hectorite-aluminasol gel rheology
 - Elastoviscous solid \rightarrow weakly elastic, shear-thinning liquid
 - ‘Yield Space’ rather than single Yield Stress
- Rheological behaviour and parameters by different techniques consistent if uniform sample pre-treatment used
- Major enhancements of rheology for small additions of second component ($\sim 0.1 c_{\text{initial}}$ w/w)

Mixed Colloid Conclusions

- Enhancements depend on second colloid shape, size, charge and number concentration
 - G' , η ($t \rightarrow 0$) and ' τ_{yeff} ' all increase rods < platelets < spheres,
 - Enhancements for nanospheres being typically x20 and up to x500
 - Critical parameter is γ_y , determined by size of minor component
- For a given shape, size and charge have a significant effect
- Most dramatic effects are with silica, a relative cheap and widely available material
 - So **cost-effective** rheology enhancement and tuning of gelation characteristics looks feasible
- Qualitative physicochemical models can rationalise the observed behaviour – heteroflocculation
 - depletion or dispersion effects
- More microstructural flow studies and quantitative models are needed

Transforming Soft Materials Formulation



Thank you all for your attention,
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Schlumberger, other companies,
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