



Leibniz
Universität
Hannover



“Enabling Technologies in Organic Chemistry – From Minireactors to New Heating Techniques”

Andreas Kirschning

**1st RSC/SCI Symposium on Continuous Processing and Flow
Chemistry, 3rd – 4th November 2010**



Institut für Organische Chemie



The FLOW Team



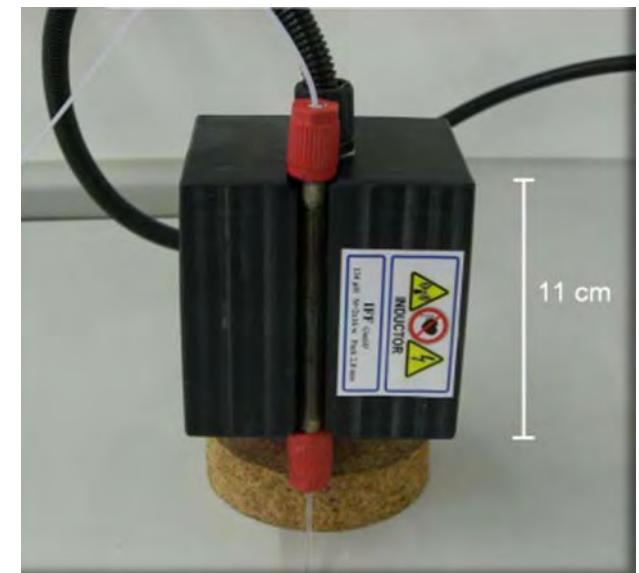
Sascha Ceylan

Jens Wegner

Dr. Ludovic Coutable

Dr. W. Solodenko

The Tools



Enabling Technologies in Organic Chemistry

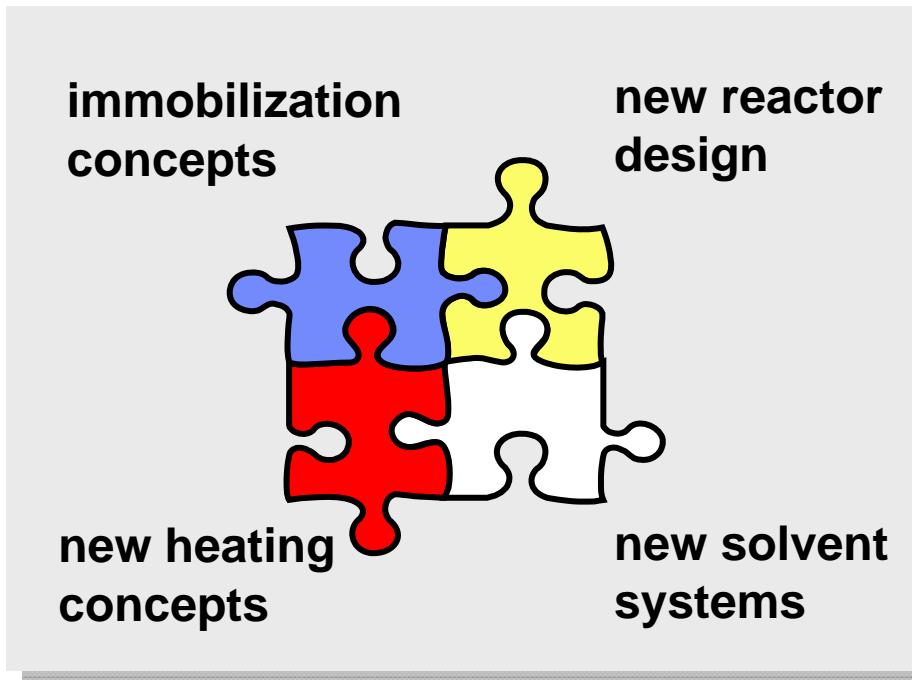
Reviews:

A. Kirschning *et al.* *Chem. Eur. J.* **2003**, 9, 5708-5723.

Chem. Eur. J. **2006**, 12, 5972-5990.

S. Ceylan, A. Kirschning, *Organic synthesis with mini flow reactors*

using immobilised catalysts, John Wiley & Sons **2009**, 379-410.



The ideal technology platform for synthesis combines facilitating technologies in a flexible manner

1st paper on functionalized monoliths within a flow device:

A. Kirschning, U. Kunz *et al.* *Angew. Chem. Int. Ed.* **2001**, *40*, 3995-3998.

PASSflow syntheses using functionalized monolithic polymer/glass composites in flow-through microreactors

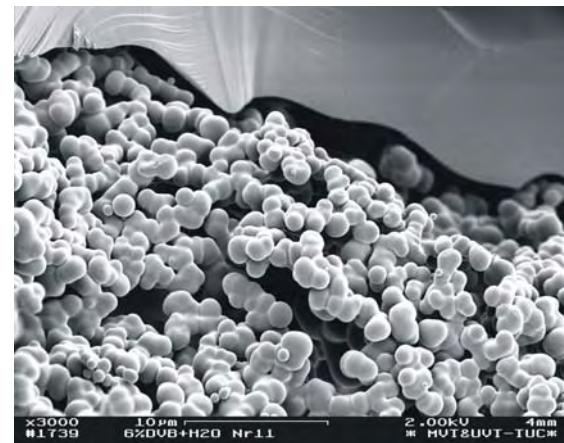
Founding of CHELONA GmbH in 2001.



**The PASSflow
Reactor**



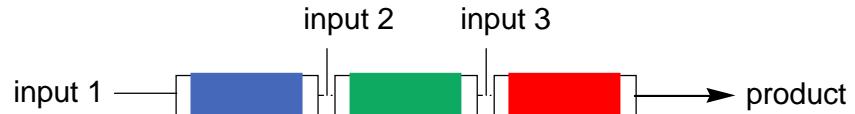
The Synthesizer



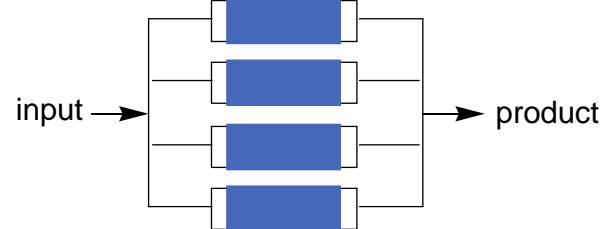
**The Monolithic
Solid Phase
(Glass/Polymer composite)**

Concepts for continuous flow syntheses

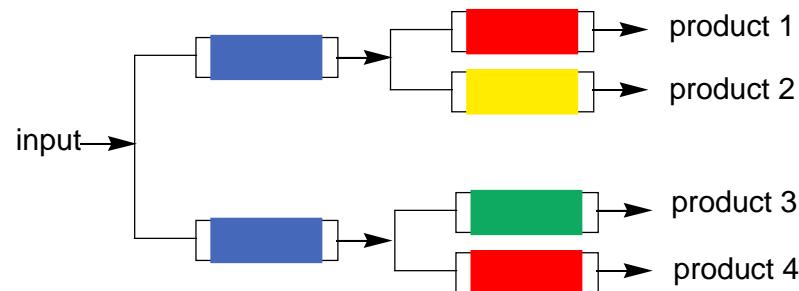
Linear series of flowthrough reactors



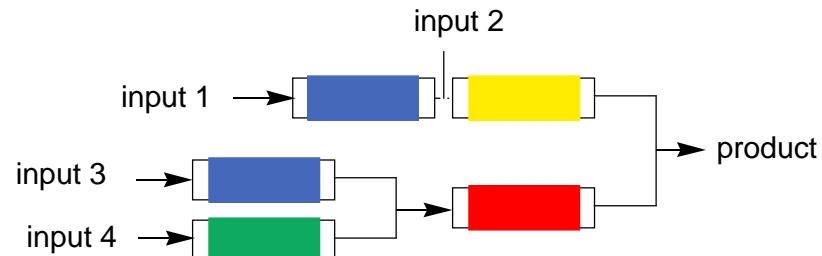
Upscale



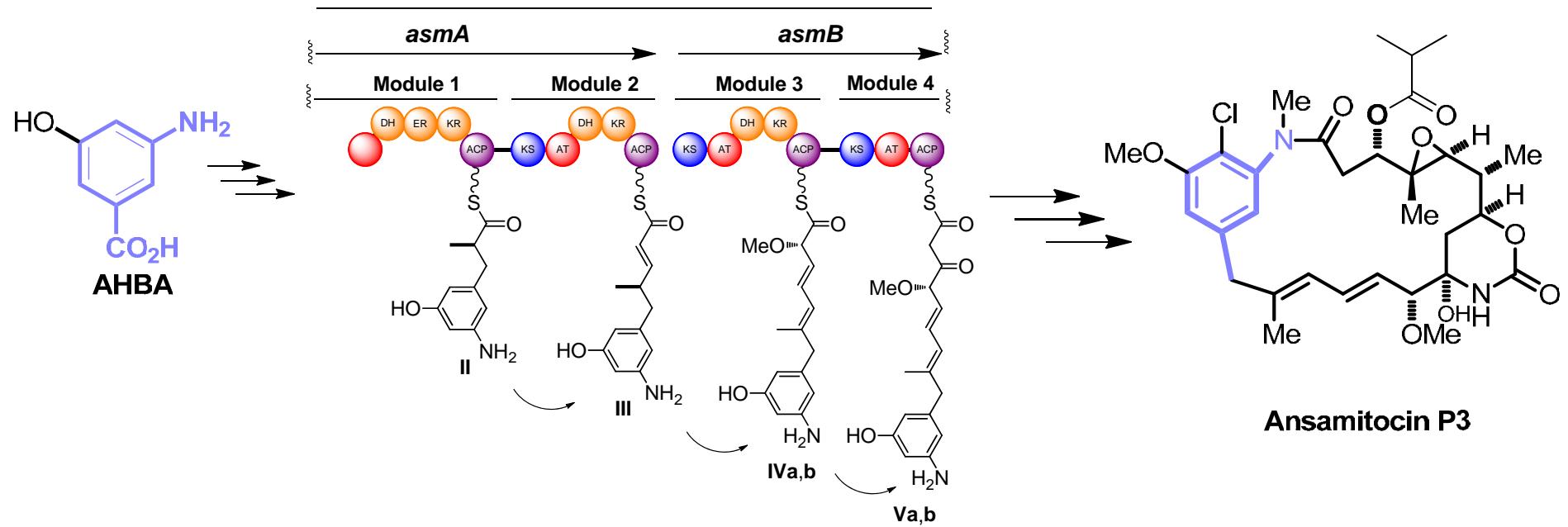
Divergent set up of flowthrough reactors



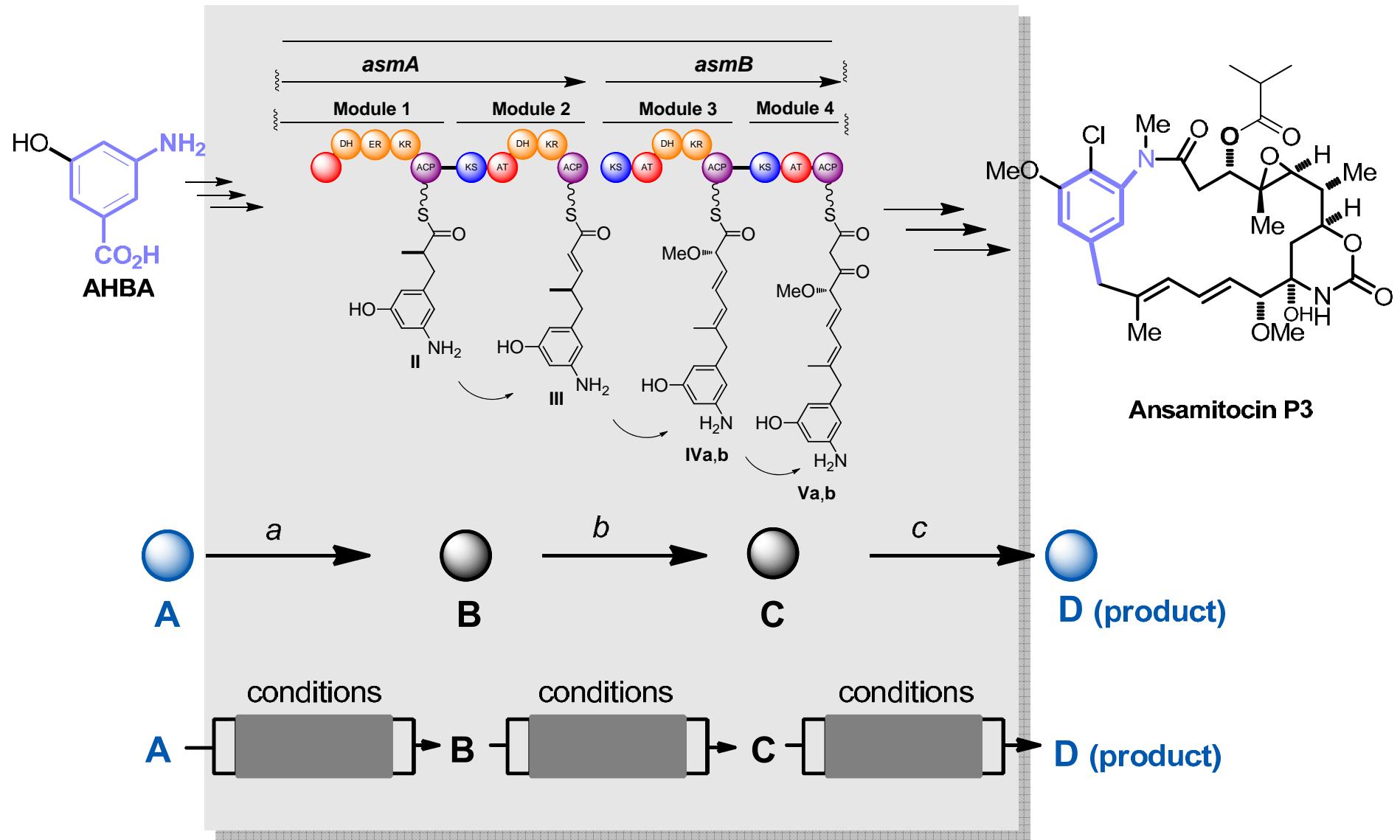
Convergent set up of flowthrough reactors



Mimicking Nature's Concept of Multistep Synthesis

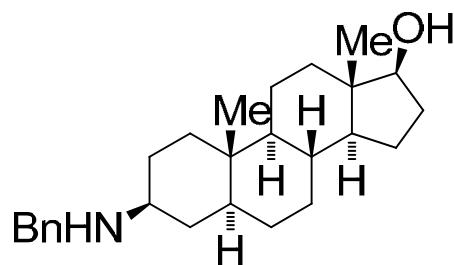
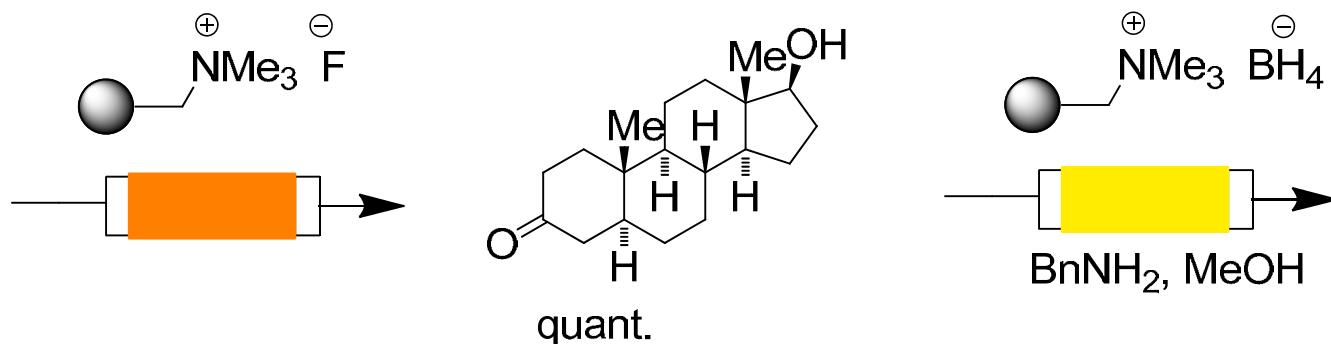
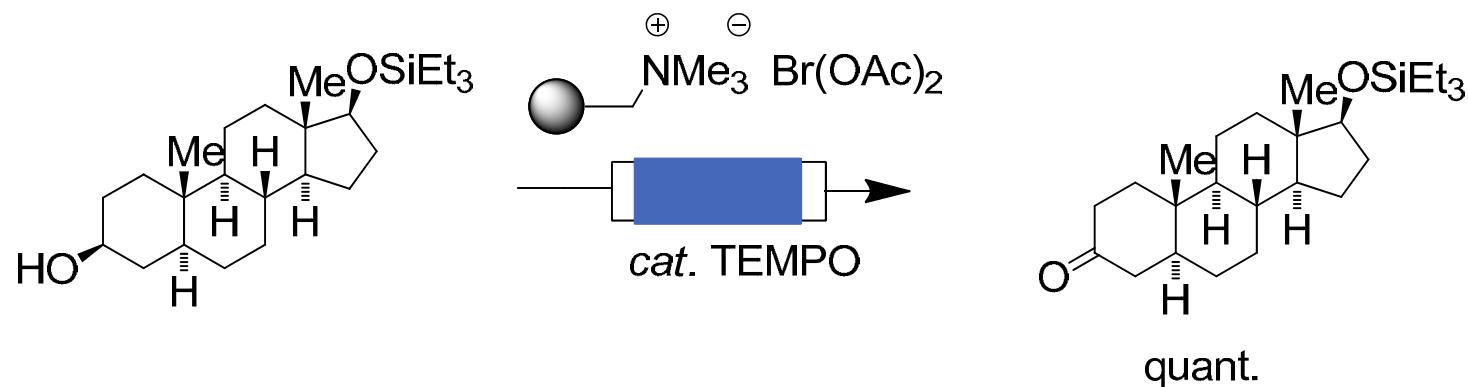


Mimicking Nature's Concept of Multistep Synthesis



a - c= enzymes; A= starting material; B and C= intermediates; D= product

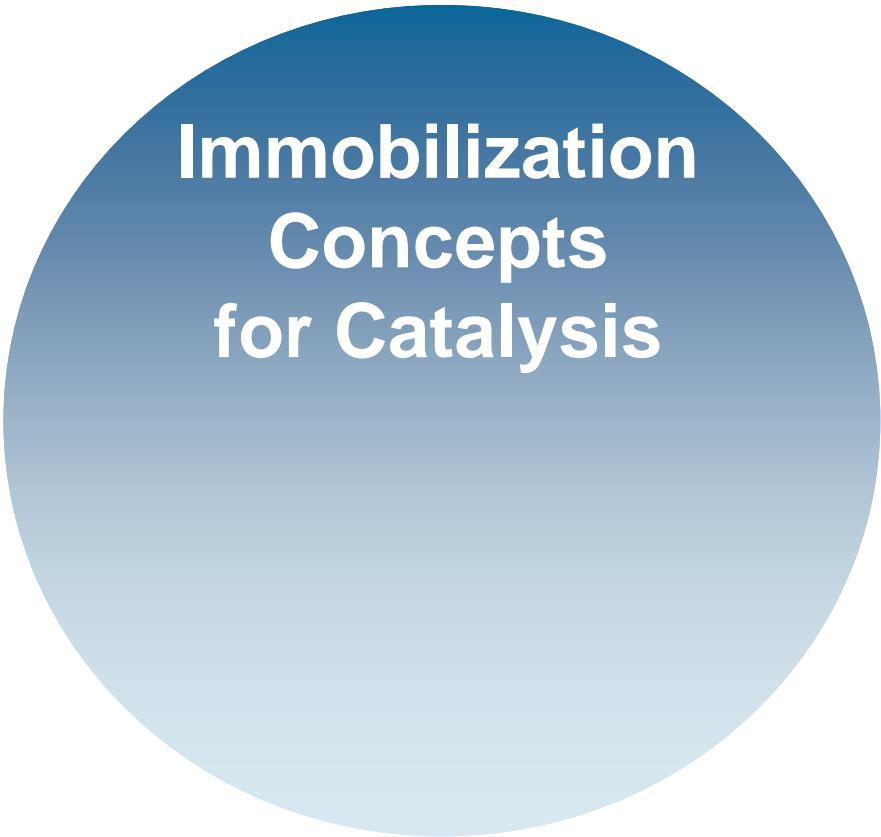
Multistep synthesis: A telling example



All reactions were carried out in a sequence mode. One reactor served for each reaction. None of the intermediates or the final product was further purified.

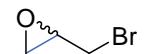
Angew. Chem. Int. Ed. **2001**, *40*, 3995-3998.

Catalysis

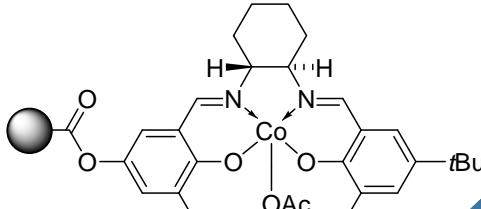
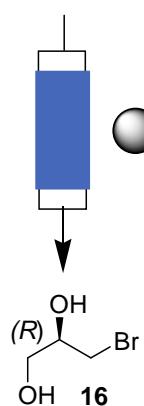


Immobilization
Concepts
for Catalysis

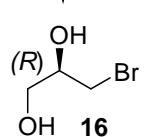
covalent



Synthesis 2007, 583-589.



H₂O (1.5 equiv.)

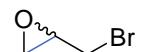


76-87% yield
91-93% ee

Immobilization Concepts for Catalysis

Covalent

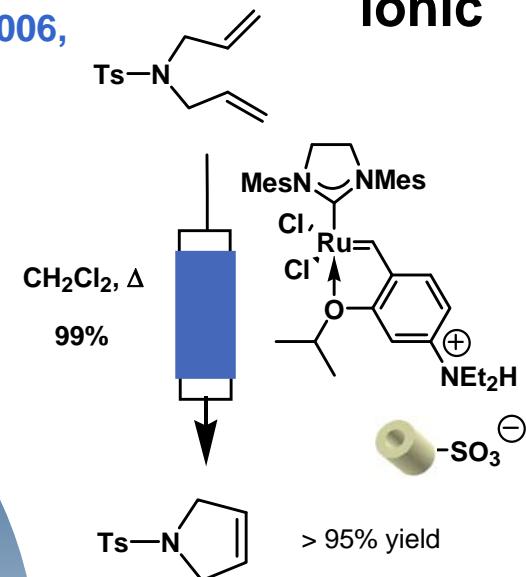
covalent



Synthesis 2007, 583-589.

J. Am. Chem. Soc. 2006,
128, 13261-13267

ionic



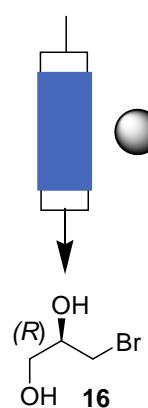
Immobilization Concepts for Catalysis

Covalent
Ionic

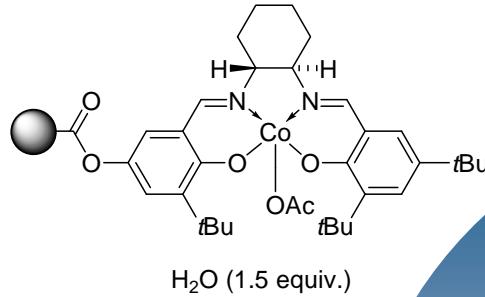
covalent



Synthesis 2007, 583-589.

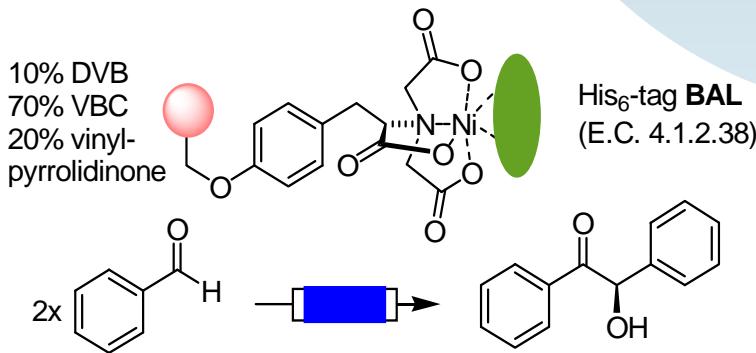


76-87% yield
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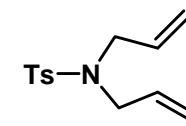
coordinative

Org. Biomol. Chem. 2007,
5, 3657-3664

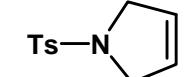


J. Am. Chem. Soc. 2006,
128, 13261-13267

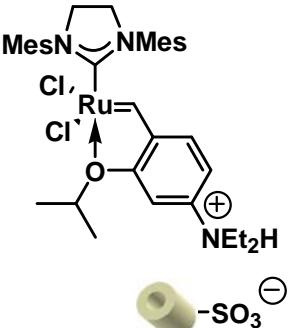
ionic



CH₂Cl₂, Δ
99%



> 95% yield



Immobilization Concepts for Catalysis

Covalent

Ionic

Coordinative

Immobilization Concepts for Catalysis

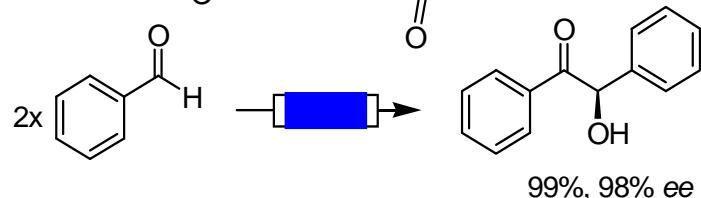
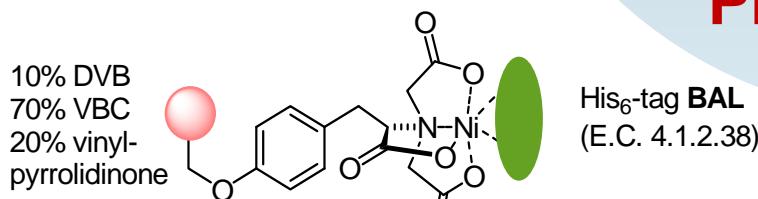
Covalent

Ionic

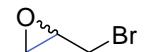
Coordinative
Physisorption

coordinative

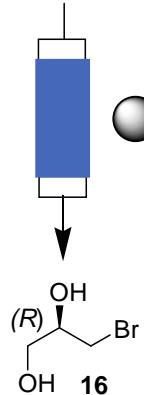
Org. Biomol. Chem. 2007,
5, 3657-3664



covalent

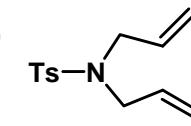


Synthesis 2007, 583-589.



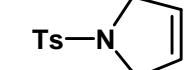
J. Am. Chem. Soc. 2006,
128, 13261-13267

ionic



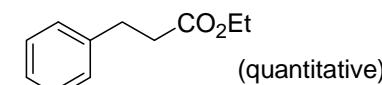
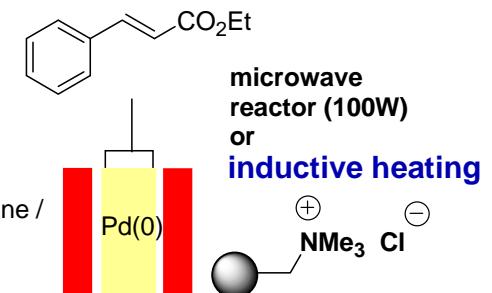
CH₂Cl₂, Δ

99%



> 95% yield

nanoparticles



Adv. Synth. Catal.
2008, 350, 717-730.

Angew. Chem.
2008, 47, 8950-8953.

Combination of three enabling techniques

Adv. Synth. Catal. **2008**, *350*, 717-730.

The diagram illustrates the combination of three enabling techniques:

- immobilization concepts
- new heating concepts
- new reactor design

These techniques are represented by four puzzle pieces (blue, yellow, red, grey) that fit together. The grey piece is labeled "new solvent systems".

The "new reactor design" section shows a schematic of a transfer hydrogenation reaction:

Transfer hydrogenation

Reaction scheme:

Starting material: c1ccccc1C=CC(=O)[O]2 (Styrene derivative)

Reactor setup:

- Pd(0) (Palladium(0))
- microwave reactor (100W) or inductive heating
- Catalyst: [NMe3]+Cl-

Product: c1ccccc1CC(=O)[O]2 (Ethylbenzene derivative)

(quantitative)

Thermal heating – a classical enabling technology



It all started with the invention of **FIRE**



A new technology – the Bunsen burner

The latest trend – microwave irradiation

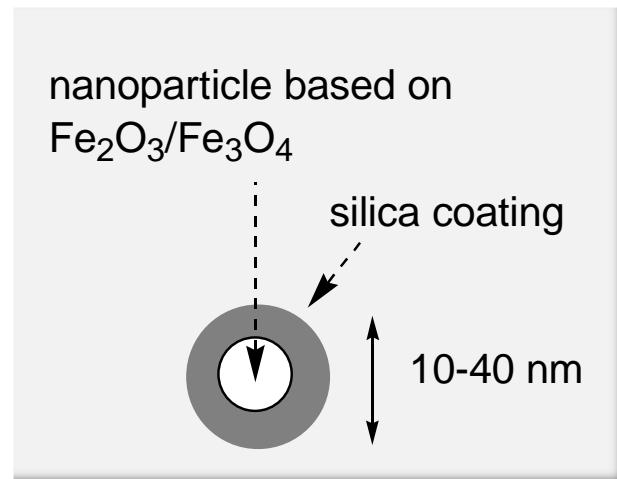


Magnetic nanoparticles

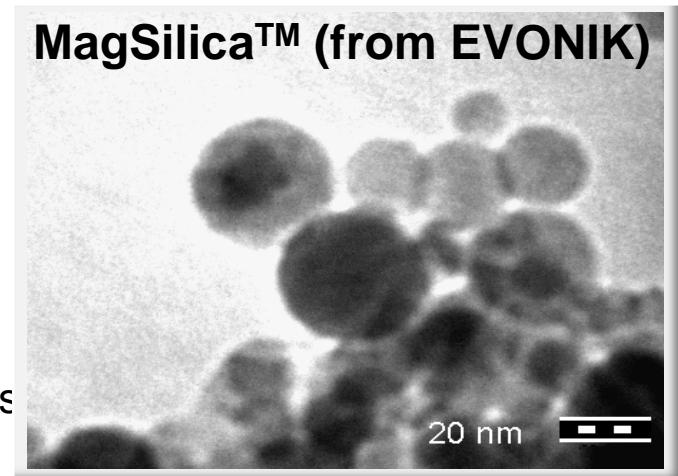
Common use

- magnetic liquids
- biomedicine
- magnetic resonance

Silica coated maghemite/magnetite particles

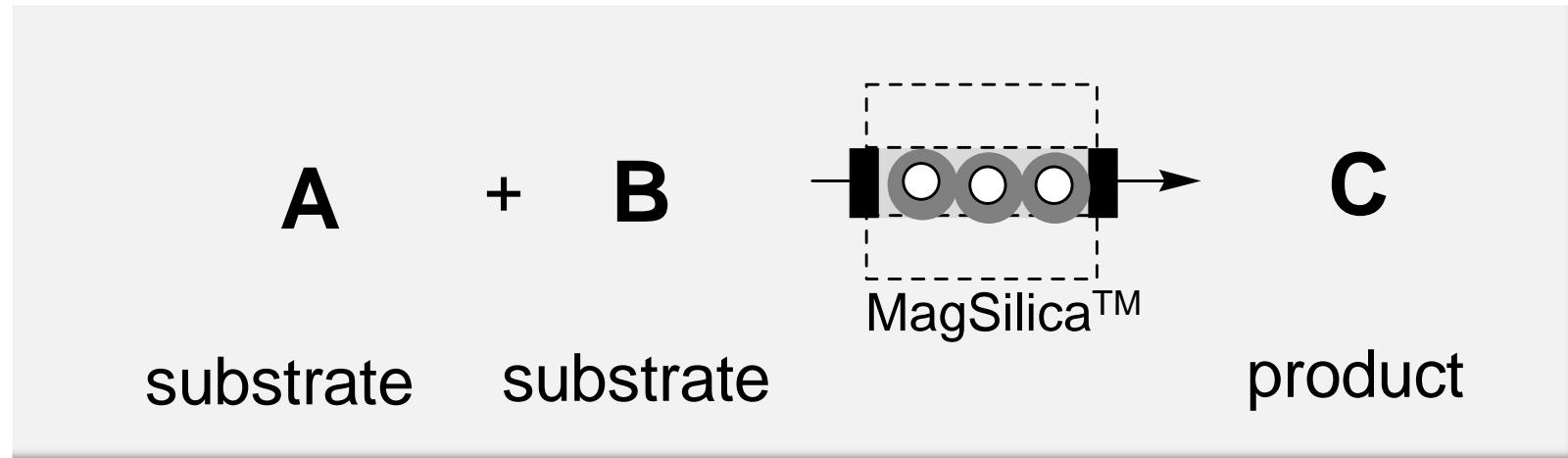


TEM micrographs of unfunctionalized magnetic nanoparticles before heating



Review: F. Schüth et al., *Angew. Chem.* **2007**, 119, 1242-1266; *Angew. Chem. Int. Ed.* **2007**, 46, 1222-1244

Inductive Heating: A new heating technology for synthesis



MagSilica™ (from EVONIK)

- application in adhesive technologies
- magnetite (Fe_2O_3) / maghemite (Fe_3O_4) core
- silica shell
- stable against most chemicals
- high surface due to nano-sized dimensions

Inductive Heating with Functionalized Magnetic Nanoparticles inside Flowreactors

Magnetic nanoparticles (1-10 nm) show superparamagnetism.

- No remanent magnetization
- Energy to alter direction of magnetic moment equals thermal energy

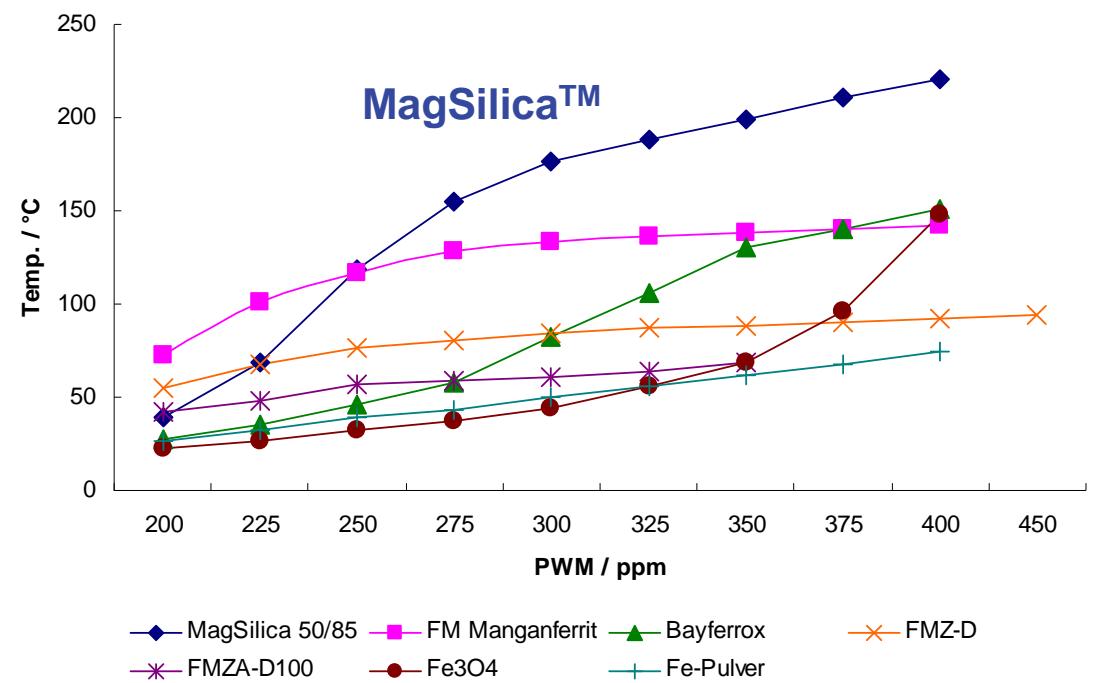
Inductive Heating with Functionalized Magnetic Nanoparticles inside Flowreactors

Magnetic nanoparticles (1-10 nm) show superparamagnetism.

- No remanent magnetization
- Energy to alter direction of magnetic moment equals thermal energy

High frequency electromagnetic field (25 KHz to > 100 KHz) leads to dramatic heating.

For **100 KHz** inductors temperatures well above **500 °C** are possible.



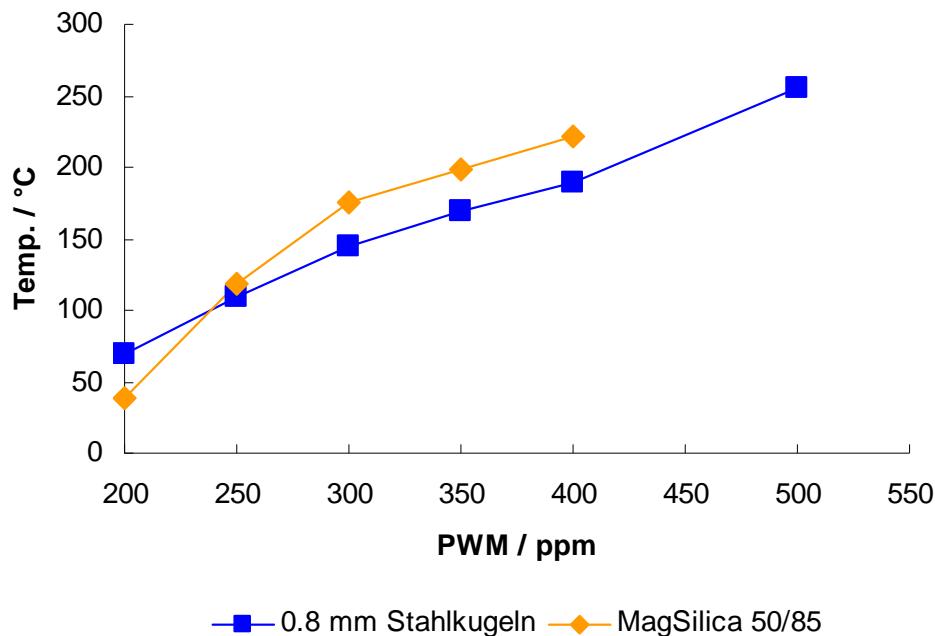
for 25 KHz inductor

Heating media

Alloys (steel)

Ferrites (Fe_3O_4 , CoFe_2O_4)

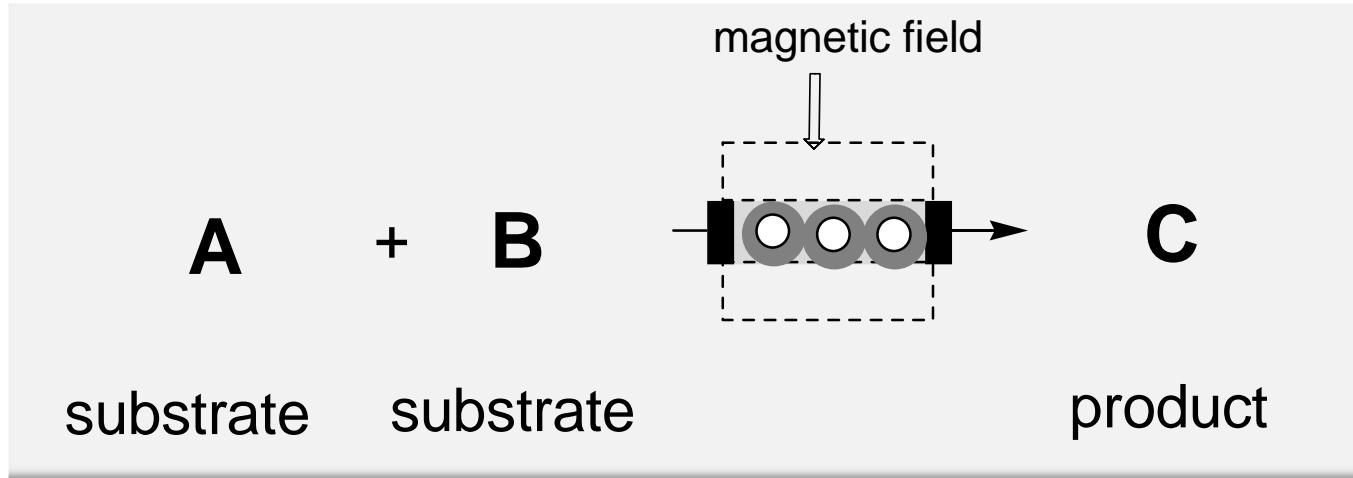
Metals (Cu, Fe etc.)



MagSilica™ superior

Steel beads (0.8 mm diameter)
competitive

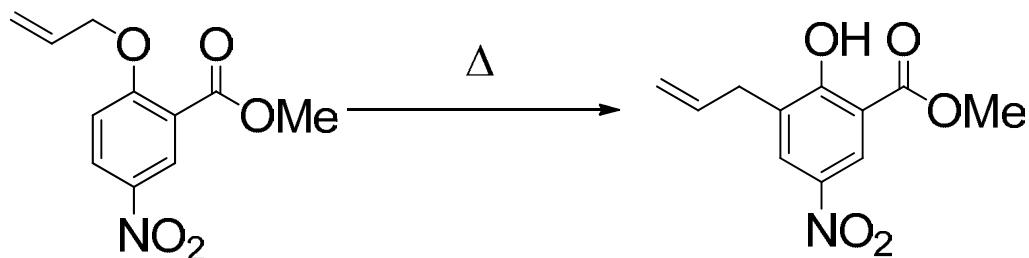
Magnetic heat induction



- heat by magnetic induction inside conductive materials → iron, copper, alloys etc.
 - superparamagnetic nanoparticles can be easily heated up to 250 °C at 25 KHz within seconds
- direct heat formation at reaction center
→ no safety risks
- hot-spot effects ?



A comparison study in batch: oil bath vs. MW vs. induction



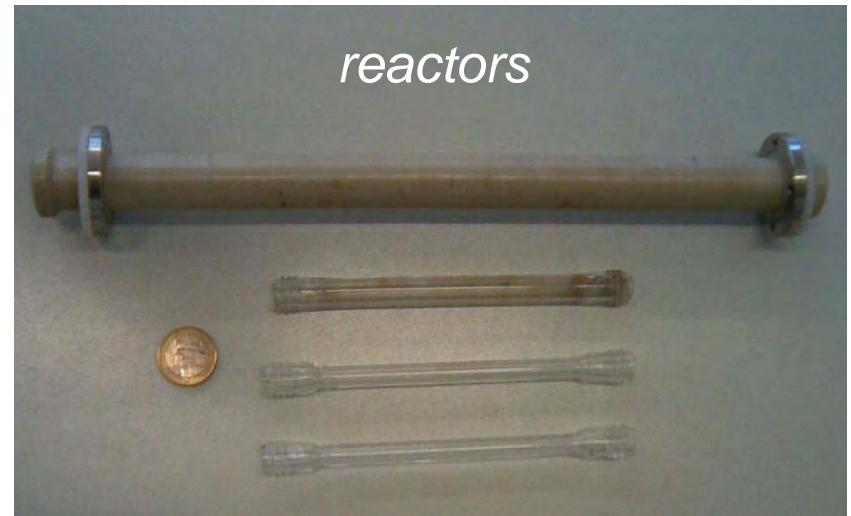
<i>entry^a</i>	<i>heating</i>	<i>time</i>	<i>temp.</i>	<i>solvent</i>	<i>yield^b</i>
1	oil bath	2 h	200 °C	toluene	17 %
2	oil bath	5 h	150 °C	DMF	0 %
3	MW, SiC	2 h	200 °C	toluene	38 %
4	MW, SiC	1 h	250 °C	solvent free	40 %
5	induction	2 h	200 °C	toluene	39 %
6	induction	0.5 h	200 °C	solvent free	25 %
7	Induction	1.5 h	200 °C	solvent free	40 %

^a MW vial, sealed, MagSilica™, 25 kHz.; ^b isolated yield.

Inductive Heating: equipment

Glass reactors:

- easy to produce and versatile
- stable up to 3 bar and 200 °C



PEEK reactors:

- stable up to 20 bar and 200 °C
- directly connectable to HPLC fittings
- expensive

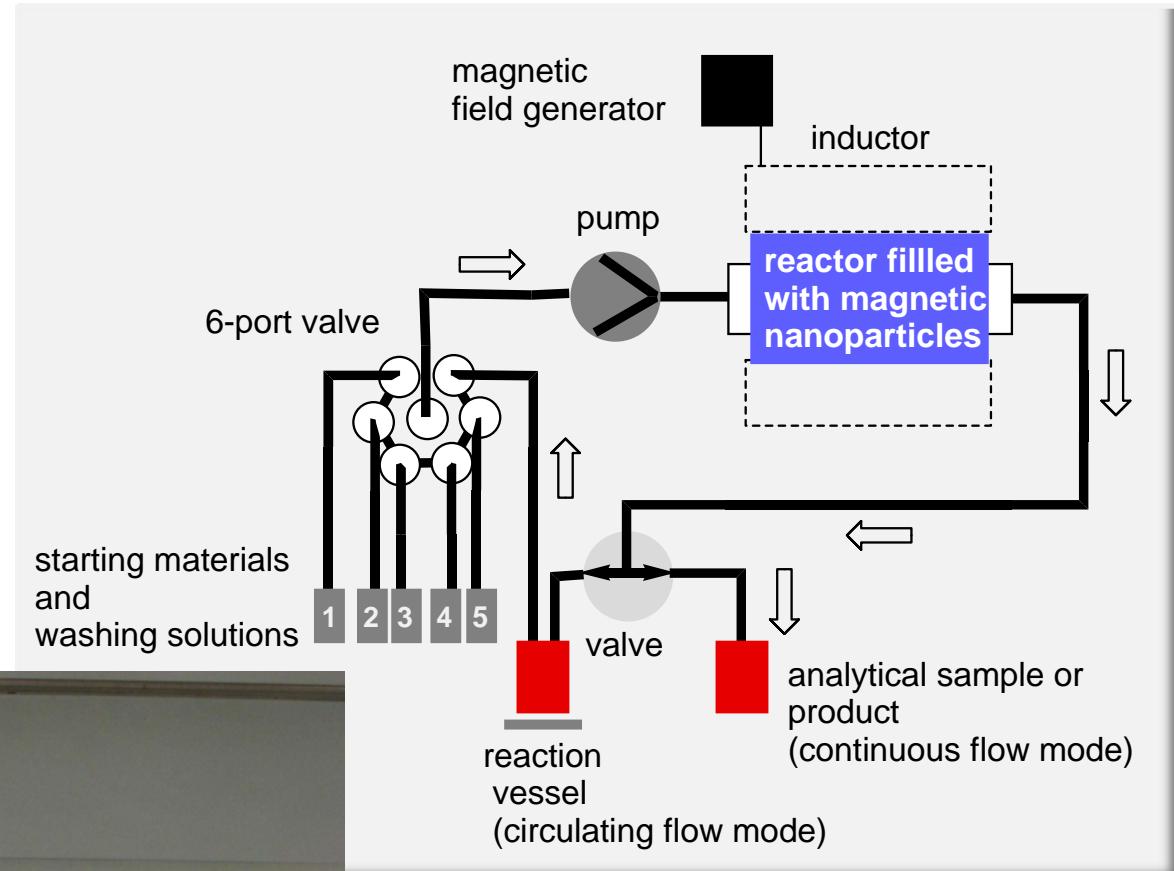
- possibility of back-pressure application
- all common solvents/reagents usable
- tailor-made inductors for individual reactors
- differ in slit diameter



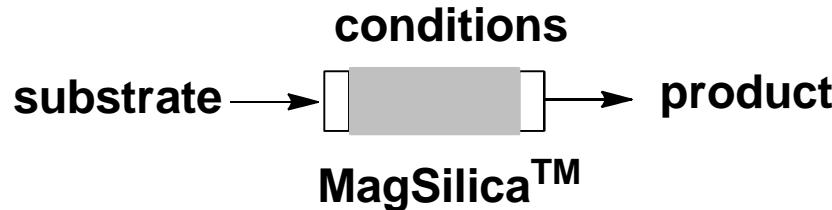
inductors

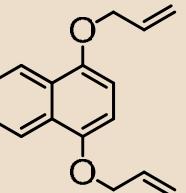
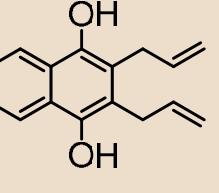


The setup – the inductor – the reactor

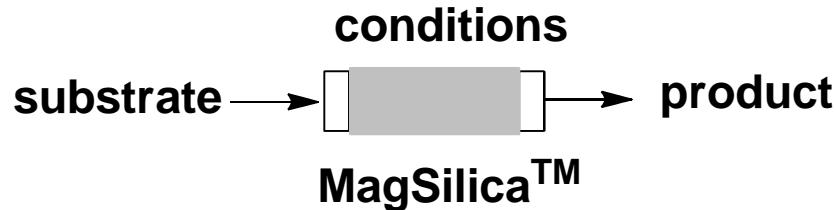


Selected inductively heated flow reactions



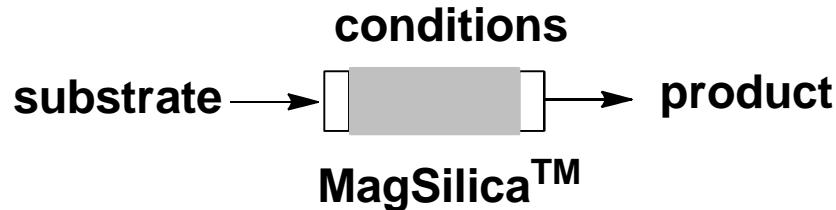
<i>entry^a</i>	<i>substrate</i>	<i>product</i>	<i>conditions</i>	<i>result^b</i>
Claisen			170 °C, dodecane, 0.5 mL/min	85 %

Selected inductively heated flow reactions



entry ^a	substrate	product	conditions	result ^b
Claisen			170 °C, dodecane, 0.5 mL/min	85 %
Cond.			70 °C, EtOH, 0.5 mL/min,	85 %
^a conditions: MagSilica™, glass reactor (12 cm x 8.5 mm, 4 mL void volume), induction frequency 25 kHz. ^b isolated yield.				

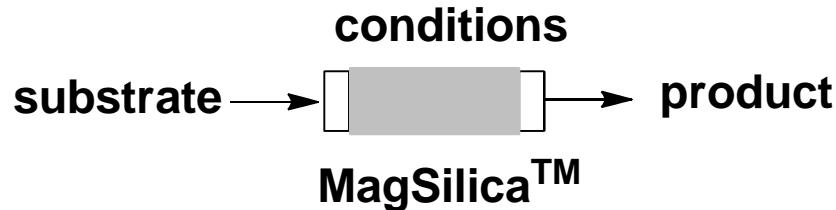
Selected inductively heated flow reactions



entry ^a	substrate	product	conditions	result ^b
Claisen			170 °C, dodecane, 0.5 mL/min	85 %
Cond.			70 °C, EtOH, 0.5 mL/min,	85 %
Trans-esterif.			60 °C, NaOMe, MeOH, 0.5 mL/min	88 %

^a conditions: MagSilica™, glass reactor (12 cm x 8.5 mm, 4 mL void volume), induction frequency 25 kHz. ^b isolated yield.

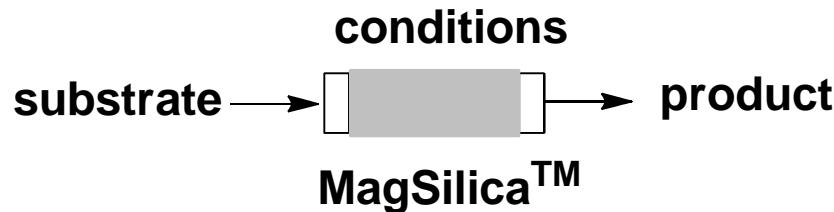
Selected inductively heated flow reactions



entry ^a	substrate	product	conditions	result ^b
Claisen			170 °C, dodecane, 0.5 mL/min	85 %
Cond.			70 °C, EtOH, 0.5 mL/min,	85 %
Trans-esterif.			60 °C, NaOMe, MeOH, 0.5 mL/min	88 %
Wittig			100 °C, toluene, 0.5 mL/min	> 99 %

^a conditions: MagSilica™, glass reactor (12 cm x 8.5 mm, 4 mL void volume), induction frequency 25 kHz. ^b isolated yield.

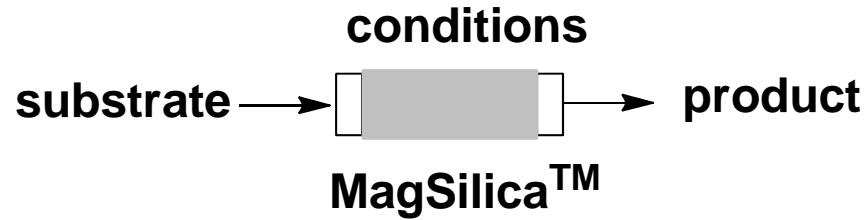
Selected inductively heated flow reactions



<i>entry^a</i>	<i>substrate</i>	<i>product</i>	<i>conditions</i>	<i>result^b</i>
Claisen			170 °C , dodecane, 0.5 mL/min	85 %
Cond.			70 °C , EtOH, 0.5 mL/min,	85 %
Trans-esterif.			60 °C , NaOMe, MeOH, 0.5 mL/min	88 %
Wittig			100 °C , toluene, 0.5 mL/min	> 99 %
Decarb.			140 °C , DMF, 0.2 mL/min	76 %

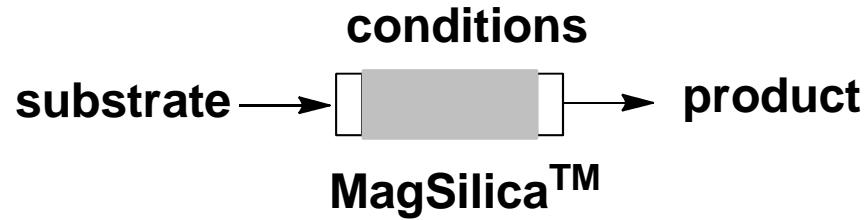
^a conditions: MagSilica™, glass reactor (12 cm x 8.5 mm, 4 mL void volume), induction frequency 25 kHz. ^b isolated yield.

Selected Inductively heated flow reactions



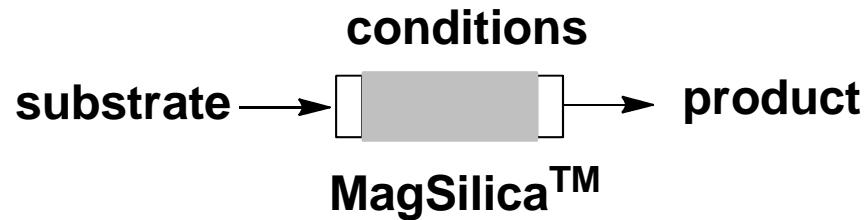
entry ^a	substrate	product	conditions	result ^b
Domino Friedländer quinoline			70°C, EtOH, KOH, 0.05 mL/min	67 %

Selected Inductively heated flow reactions



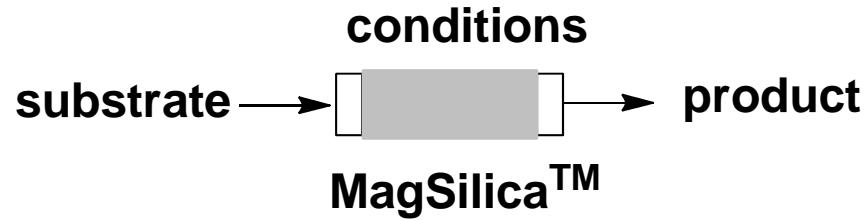
entry ^a	substrate	product	conditions	result ^b
Domino Friedländer quinoline	 		70°C, EtOH, KOH, 0.05 mL/min	67 %
Domino benzoxazine	 		135 °C, DBU (2 eq.), DMF, 0.2 mL/min	82 %

Selected Inductively heated flow reactions



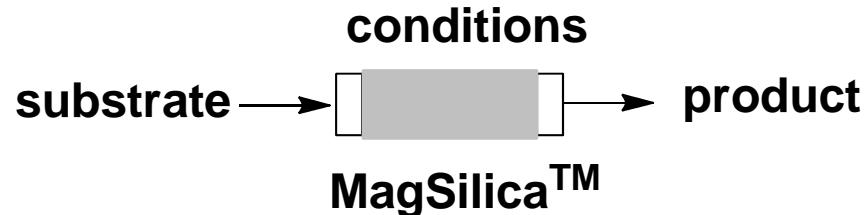
entry ^a	substrate	product	conditions	result ^b
Domino Friedländer quinoline	 		70 °C, EtOH, KOH, 0.05 mL/min	67 %
Domino benzoxazine	 		135 °C, DBU (2 eq.), DMF, 0.2 mL/min	82 %
Organometallic	 		60 °C, Zn (30 eq.), THF, 0.1 mL/min (d.r. 4:1)	70% (batch 35%)

Selected Inductively heated flow reactions



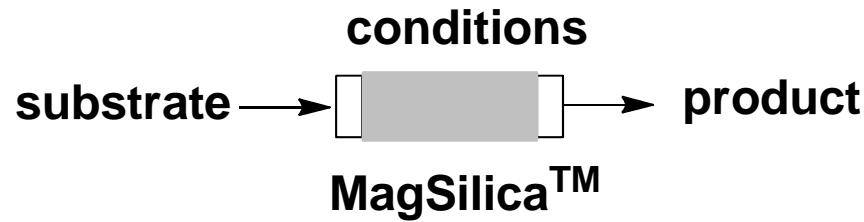
entry ^a	substrate	product	conditions	result ^b
Hartwig Buchwald			120°C , 4 mol% PEPPSI™ <i>n</i> -Bu ₃ N, DME, 25 kHz, 0.5 mL/min	87 %

Selected Inductively heated flow reactions



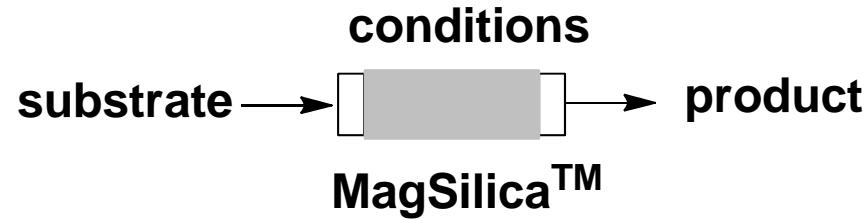
entry ^a	substrate	product	conditions	result ^b
Hartwig Buchwald			120°C , 4 mol% PEPPSI™ <i>n</i> -Bu ₃ N, DME, 25 kHz, 0.5 mL/min	87 %
Catalysis, hydro-amination			80°C , (MeCN) ₄ Pd(BF ₄) ₂ , FeCl ₃ .6H ₂ O (CICH ₂) ₂ /DMF (5:1) 0.1 mL/min	70 %

Selected Inductively heated flow reactions



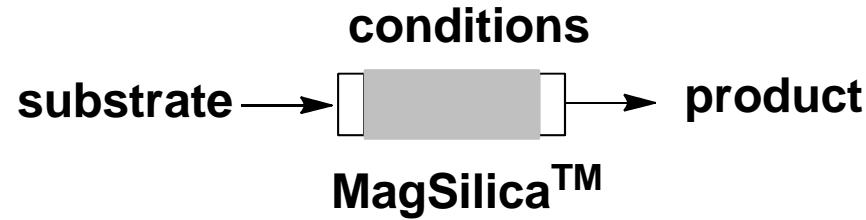
entry ^a	substrate	product	conditions	result ^b
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Catalysis, domino Sonogashira			110 °C , PdCl ₂ , TBAA, NMP, 0.15 mL/min Steel beads	82 %

Selected Inductively heated flow reactions



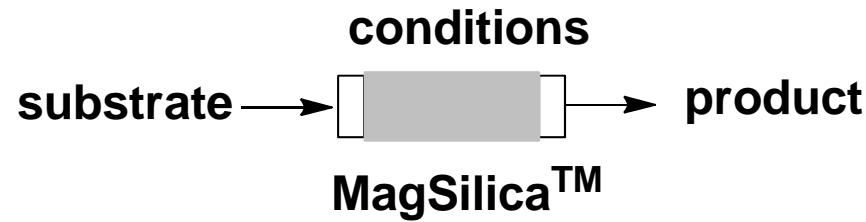
entry ^a	substrate	product	conditions	result ^b
Enyne Metathesis			90°C , 5 mol% Grubbs II toluene, 0.2 mL/min,	92 %

Selected Inductively heated flow reactions



entry ^a	substrate	product	conditions	result ^b
Enyne Metathesis			90°C , 5 mol% Grubbs II toluene, 0.2 mL/min,	92 %
Reductive cyclization			150°C , P(OEt) ₃ / DMF 3:1, 0.05 mL/min	44 %

Selected Inductively heated flow reactions

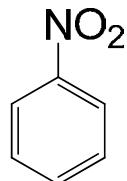


entry ^a	substrate	product	conditions	result ^b
Enyne Metathesis			90°C , 5 mol% Grubbs II toluene, 0.2 mL/min,	92 %
Reductive cyclization			150°C , P(OEt) ₃ / DMF 3:1, 0.05 mL/min	44 %
Catalysis, Domino dihydrobenz -oxazine			150 °C , P(OEt) ₃ / toluene 3:1, 0.05 mL/min Superheated	52 %

Inductively heated flow reactions

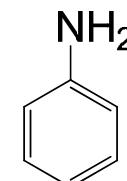
Catalytic transfer
Hydrogenations
(isolated yields)

cyclohexene/Et₂O, H₂,



Pd/C

Fe₃O₄



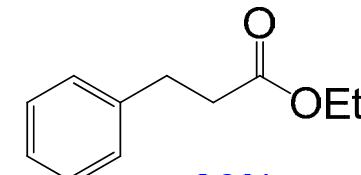
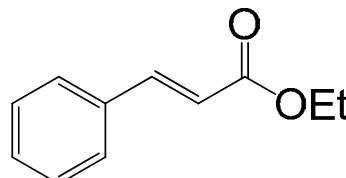
25 kHz,
70 °C, 0.2 mL/min

93%

cyclohexene/Et₂O, H₂,

Pd/C

Fe₃O₄



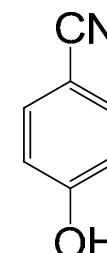
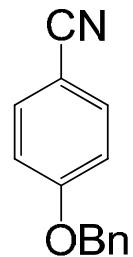
90%

25 kHz,
70 °C, 0.5 mL/min

cyclohexene/Et₂O, H₂,

Pd/C

Fe₃O₄



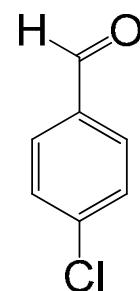
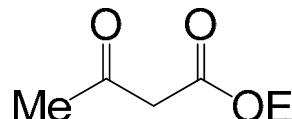
25 kHz,
70 °C, 0.2 mL/min

89%

Multicomponent reactions

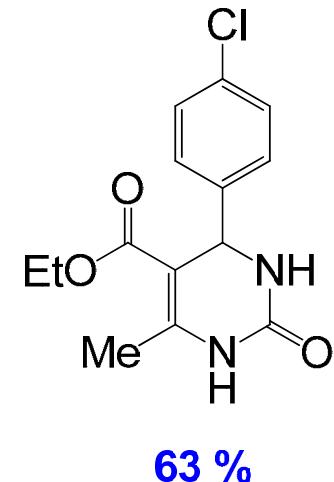
(isolated yields)

Biginelli reaction

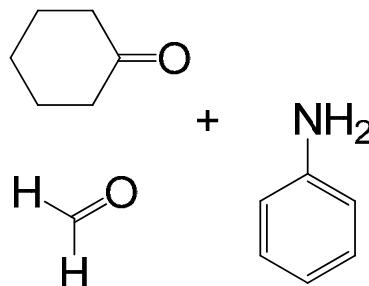


PTSA (0.25 eq.),
PEG-200/DMF (1:1)

—  →
20 KHz, 130 °C,
0.05 mL/min

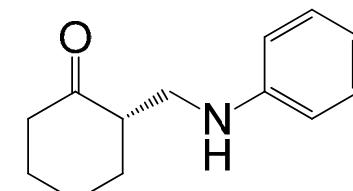


Mannich reaction (organocatalyzed)



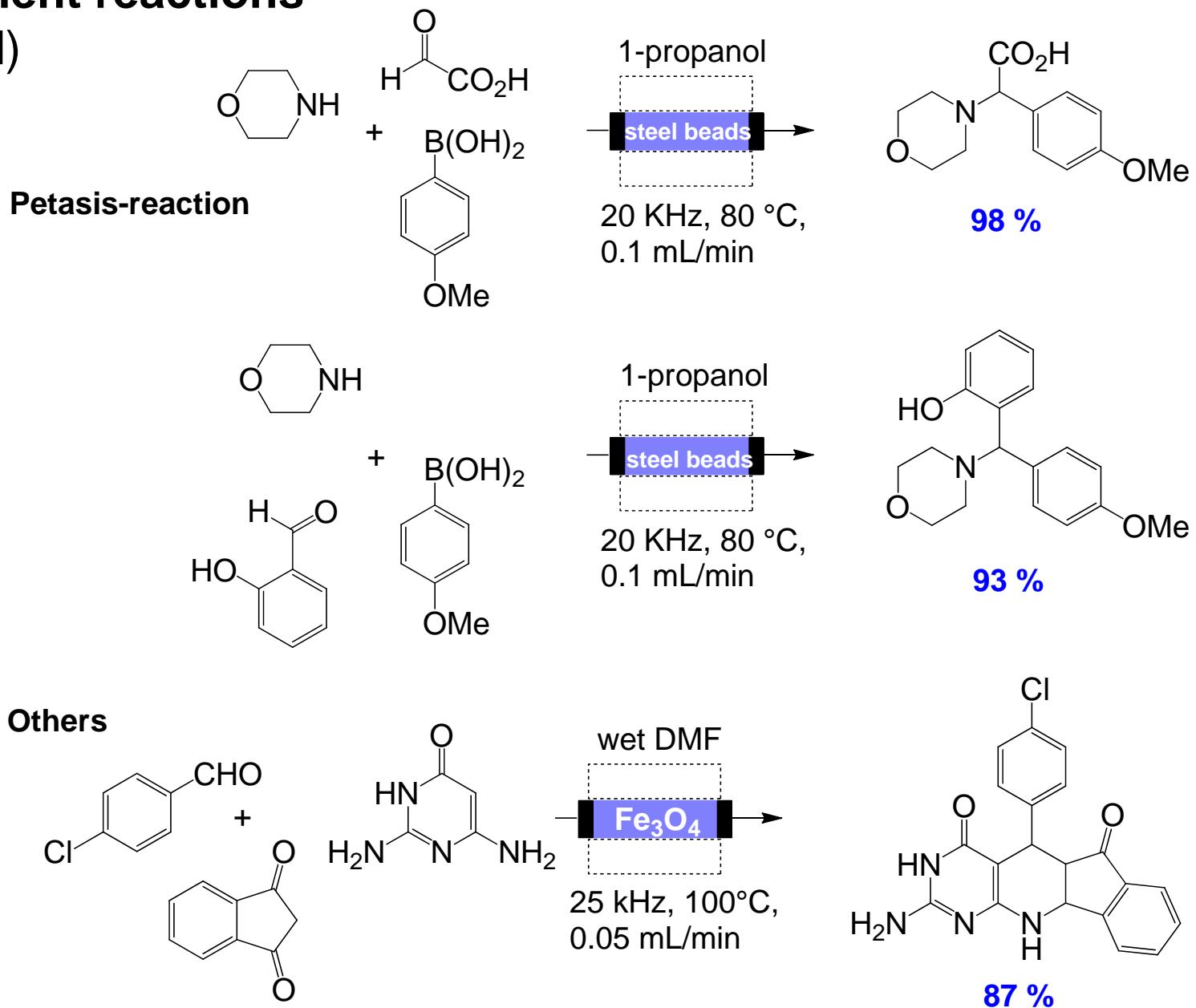
(S)-proline (0.1 eq.)

DMSO
—  →
20 KHz, 65 °C,
0.07 mL/min

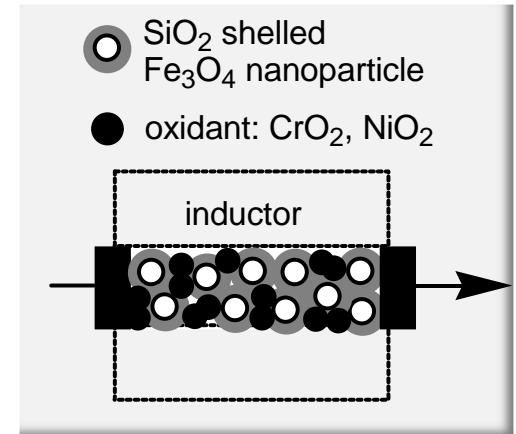
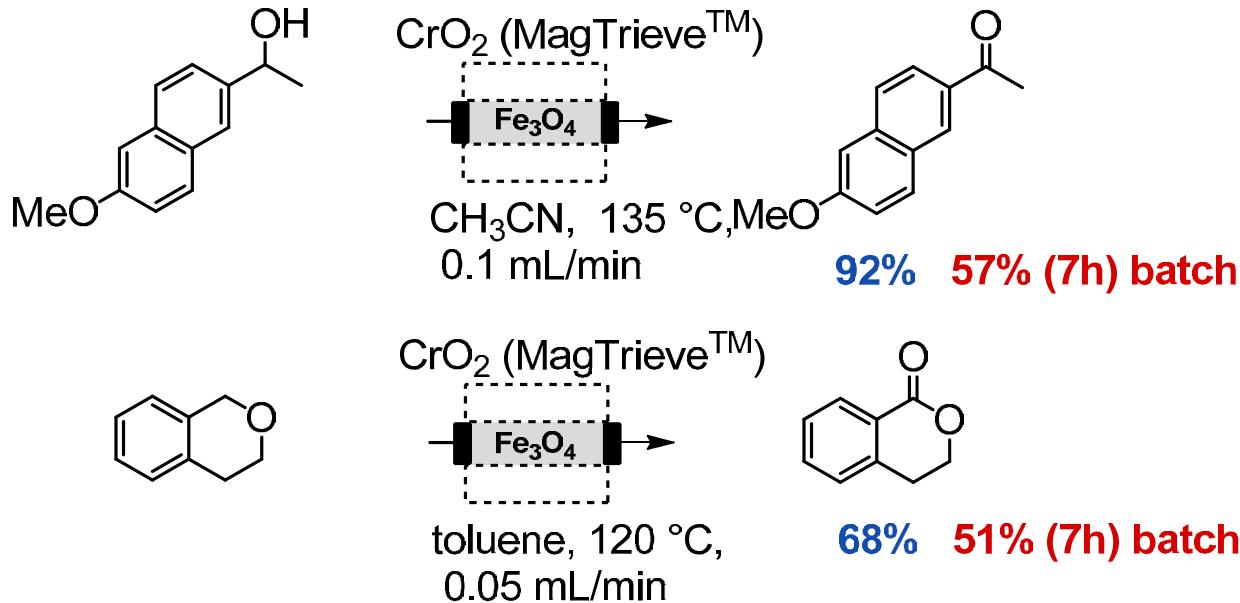


85 %, 88 % ee

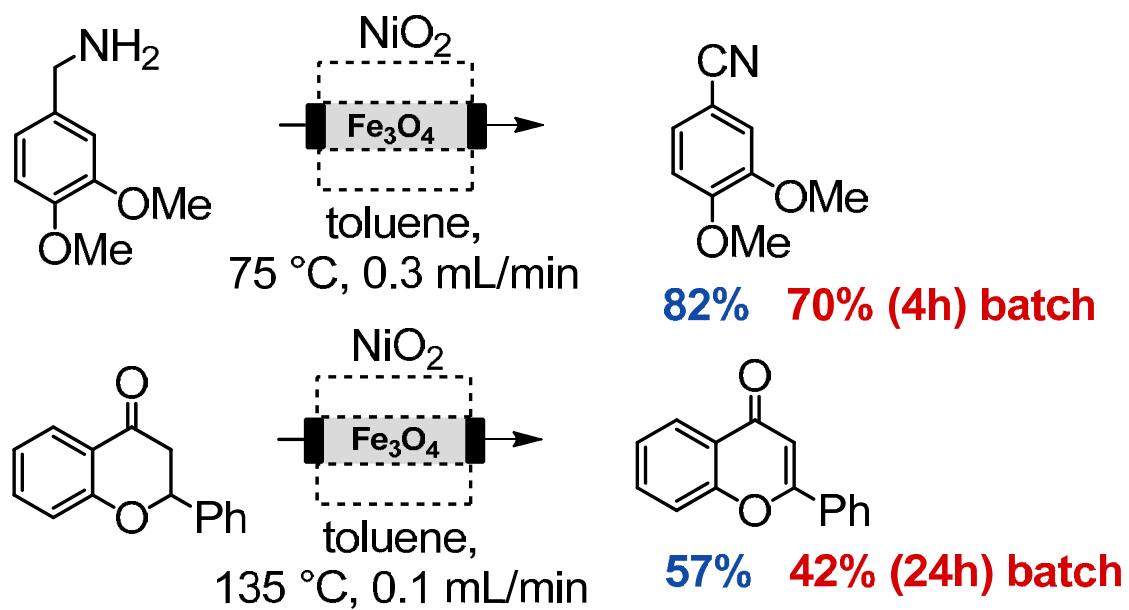
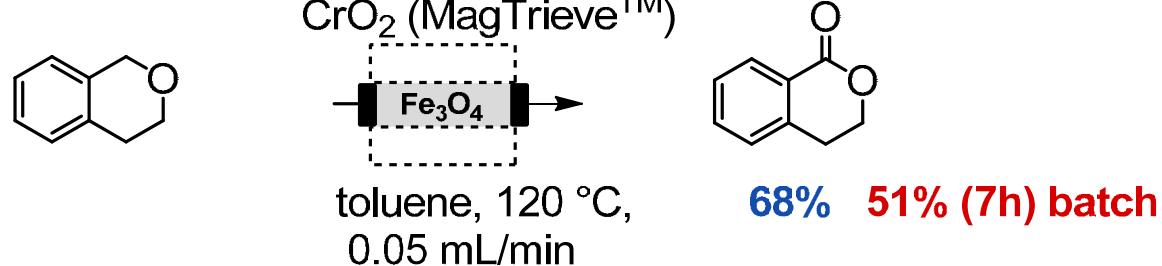
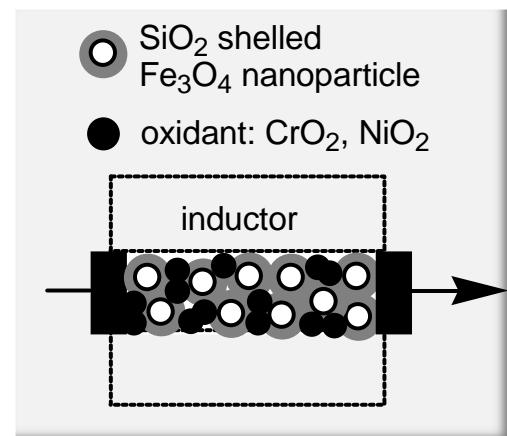
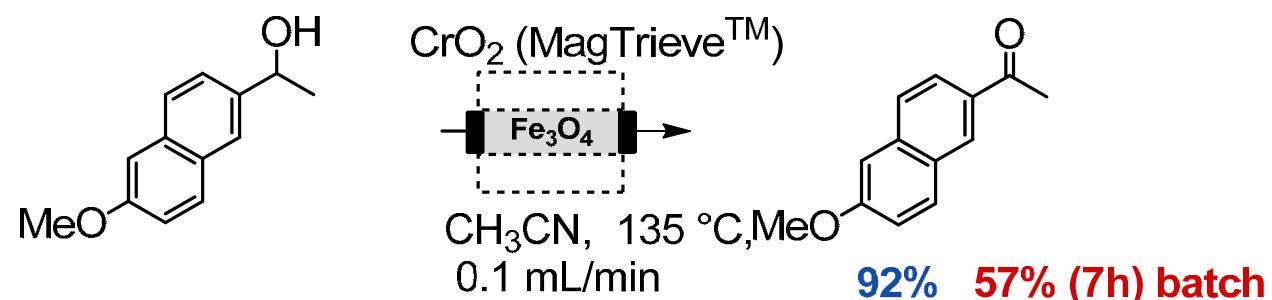
Multicomponent reactions (isolated yield)



High pressure, high temperature oxidations in flow

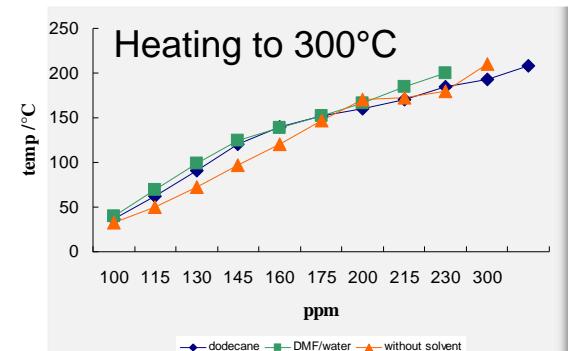


High pressure, high temperature oxidations in flow



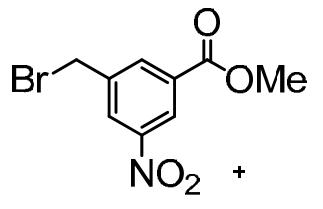
A. Kirschning, C. Friese,
S. Ceylan, J. Wegner,
Eur. J. Org. Chem.
2010, 4372-4375.

Chemical synthesis with inductively heated copper flow reactors

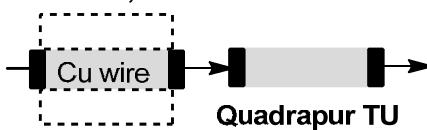


Residence time: 0.5 h

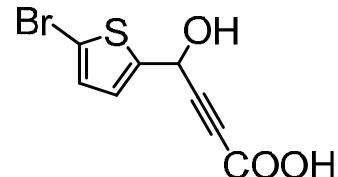
Chemical synthesis with inductively heated copper flow reactors



NaN_3 , DMF, 100°C,
0.2 mL/min, 15 kHz

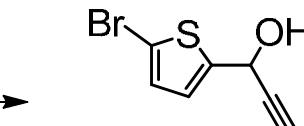


no conversion (batch)
99% (flow)

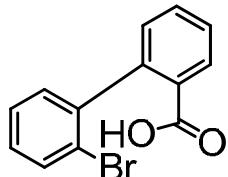


MeCN, 0.1 mL/min,
60°C, 15 kHz

glass reactor

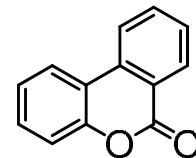


3h, 92% (batch)
90%

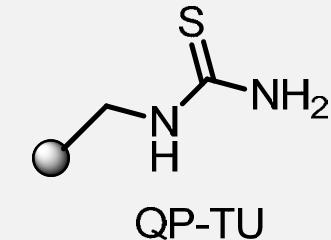


DMF, 0.1 mL/min,
200°C, 15 kHz

PEEK reactor



2.5h, 77% batch
95%



Residence time: 0.5 h

Leaching experiments

- Determination of metal residues
- ICP-OES measurements

thermal reactions

solvent ^a	Fe content ^b
dodecane	0.46 ppm
toluene	0.11 ppm
DMF	0.34 ppm
PEG	2.65 ppm
EtOH	0.25 ppm

^a taken at 120 °C, flow rate 0.1 mL/min,
MagSilica™

^b average of three runs

oxidations

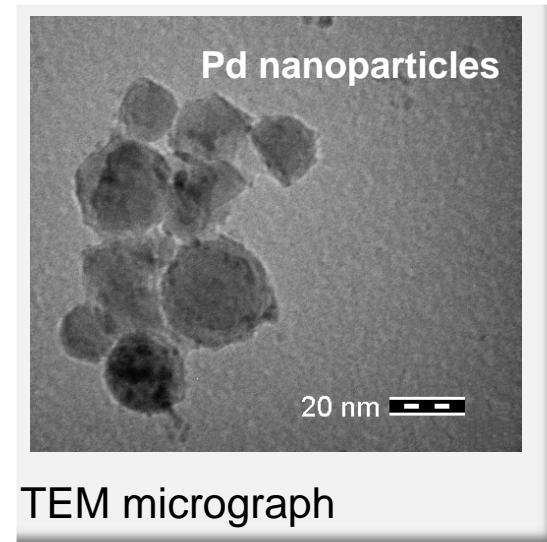
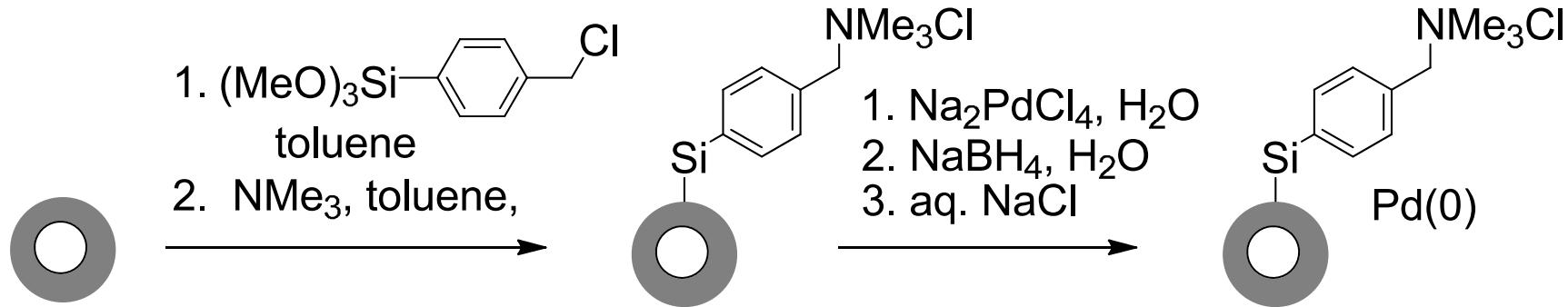
metal	metal content ^a
Fe	4.15 ppm
Ni	0.15 ppm
Cr	1.75 ppm

Cu catalysis

reaction	Cu content
„click“	3.52 ppm
decarboxylation	> 0.01 ppm
C-O-coupling	12.65 ppm

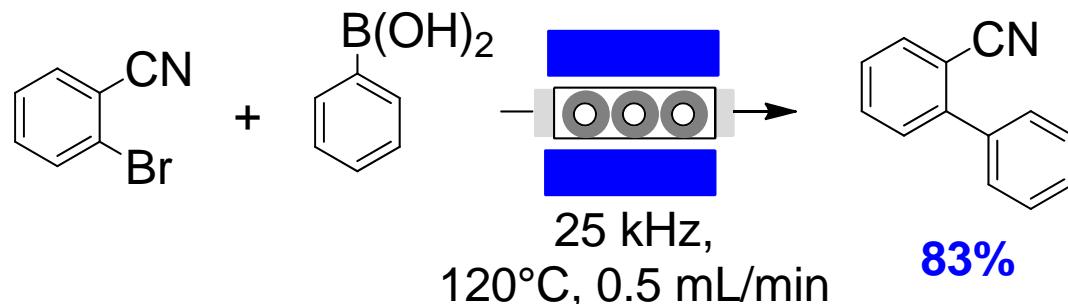
^a average of three runs

Immobilisation of Pd nanoparticles on magnetic nanoparticles

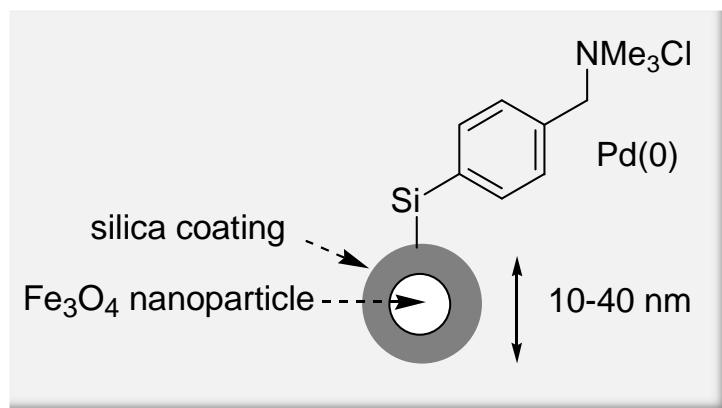
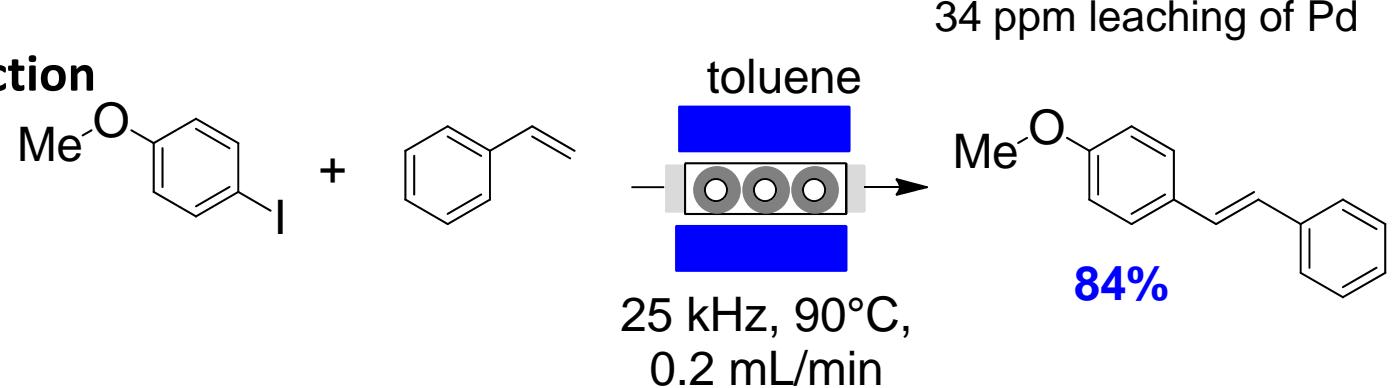


Pd nanoparticles on core-shell magnetic nanoparticles

Suzuki-Miyaura reaction



Heck-Mizoroki reaction

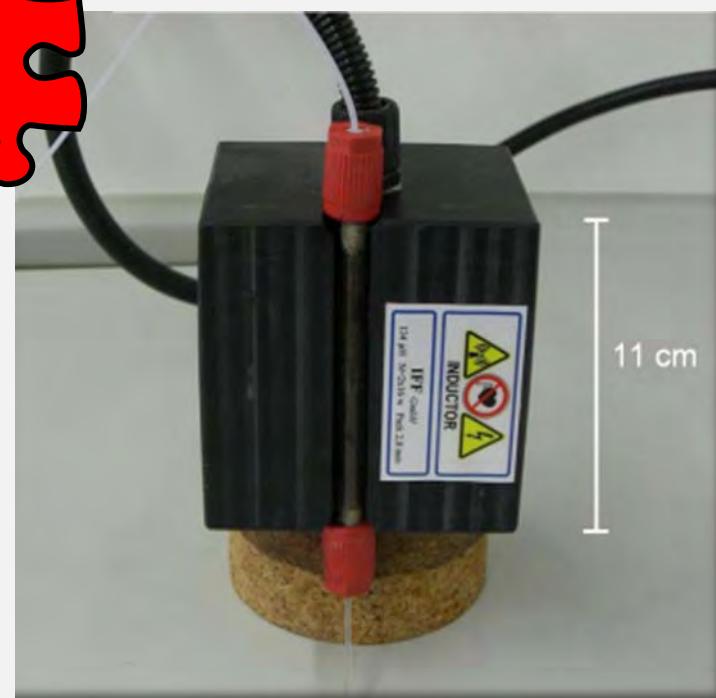
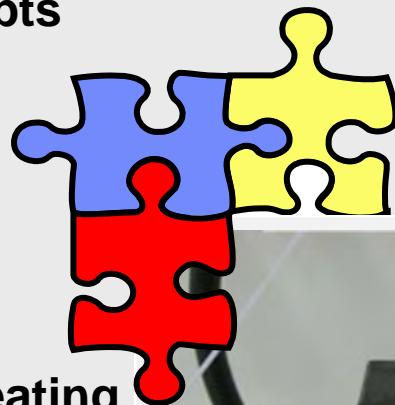


Angew. Chem. 2008, 47, 8950-8953.

immobilization
concepts

new reactor
design

new heating
concepts



Inductive heating – a new enabling technology for organic synthesis ?

a third, new heating technology

new tailor-made reactors and
inductors

many reactions under
flow conditions achieved
(continuous processes)

synthesis under hypercritical
conditions possible

successful immobilization
of catalysts on MagSilica™



Leibniz
Universität
Hannover



The Key Pioneers



Dr. G. Dräger



Dr. W. Solodenko



Dr. E. Kunst



Dr. K. Mennecke

Funding

Fonds der Chemischen Industrie

DFG

EU

Henkel KGaA, Düsseldorf

SOLVAY Pharmaceuticals, Hannover

PLASMATREAT, Steinhagen

Collaborations

U. Kunz (Clausthal)
IFF (München)

C. O. Kappe (Graz)
K. Grela (Warsaw)
EVONIK/ Degussa
(Frankfurt/Hanau)